# Formation of micropollutant decomposition by-products during oxidation processes supported by natural sunlight

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#### ABSTRACT

The paper presents the comparison of micropollutant removal degrees after the  $O_3$  and  $O_4/$ H<sub>2</sub>O<sub>2</sub> processes supported by sunlight radiation. These tests were conducted on selected organic micropollutant water solutions prepared on the base of deionized water. The examined compounds belong to the group of pharmaceuticals (benzocaine, caffeine, carbamazepine (CBZ), diclofenac sodium salt, ibuprofen sodium salt (IBU)), hormones ( $\beta$ -estradiol,  $17\alpha$ -ethinylestradiol, mestranol, progesterone), pesticides (triallate, triclosan, oxadiazon), food additives (butylated hydroxytoluene (BHT)) and dyes (acridine). Processes were carried out at various O<sub>3</sub> doses: 1, 2, 3, 5 and 10 mg/L. The reaction vessels containing the test solutions were exposed to solar radiation for 10, 20, 30 and 60 min. The process effectiveness and the identification of the formed compound decomposition by-products were assessed by the use of gas chromatography coupled with mass detection based on the NIST v17 mass spectra database. It was noted that the presence of another type of oxidant in the form of H<sub>2</sub>O<sub>2</sub> during the O<sub>3</sub>/sun light process results in the reduction of the half-life of CBZ, IBU, BHT, and all tested hormones and pesticides. On the other hand, the presence of H<sub>2</sub>O<sub>2</sub> affected the type and the number of generated micropollutant intermediates. The highest compound removal degrees, which exceeded 92%, were noted during the implementation of sunlight supported process for micropollutants belonging to the group of hormones and pesticides. Also, it was observed that the irradiation of samples with sunlight resulted in a decrease in the number of formed decomposition by-products. The conducted toxicological analysis confirmed the reduction of the toxic nature of samples subjected to sunlight assisted by the O./H,O, process compared to samples treated by the action of O<sub>2</sub>/H<sub>2</sub>O<sub>2</sub> performed in a dark chamber.

Keywords: Organic micropollutants; Decomposition by-products; Sunlight; Toxicity

#### 1. Introduction

Pollution of the water environment with different types of contaminants in the light of the constantly decreasing availability of drinking water resources become one of the major problems of modern humanity. Micropollutants detected in surface and groundwater consists of various materials and can contain different types of metabolized or non-metabolized compounds such as pharmaceuticals, personal care products, hormones, pesticides, flame retardants, waterproofing agents, plasticizers, food and industrial additives [1–3]. Effluents from wastewater treatment plants based on activated sludge treatment methods are considered to be the main sources of several types of micropollutants that is, inorganic and organic compounds [4] and microplastic [5] in the environment. Hey [6] reported that on average 70% of pharmaceutical compounds in wastewater come from a household, 20% originates from livestock farms, only 5% comes from hospital wastewater, and 5% is introduced in the form of runoff from nanoparticular sources. Pesticides enter

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the environment with surface runoff from agricultural areas, which for example constitute about 43% of the total land area of the European Union countries [7]. The most often used classes of pesticides are herbicides, fungicides, bactericides and insecticides [8].

The implementation of advanced oxidation processes based on the action of  $O_3$  or  $H_2O_2$  allowed the removal of a large number of hardly-biodegradable compounds [9,10]. On the other had those in-depth oxidation processes lead to the generation of intermediates, which are the main reason for water quality deterioration [11]. The newly formed compounds increase the toxicity of the treated water matrix [12] and cause sublethal biological responses of organisms that stay in contact with water [13,14].

Because  $O_3$  molecules are very unstable in water media, the introduction of this oxidant to water initiates different reactions from (1) to (16), leading to the transformation of  $O_3$  to  $O_2$  and also to the formation of reactive radicals [15]. The strongest oxidation potential after fluoride, with a standard redox potential equal to 2.8 V/SHE, and a nonselective character is attributed to OH• radicals [16].

$$O_3 + H_2O \rightarrow HO_3^+ + OH^-$$
 (1)

$$HO_3^+ + OH^- \rightarrow 2HO_2 \tag{2}$$

$$O_3 + HO_2 \rightarrow HO + 2O_2 \tag{3}$$

$$HO_2 + HO \rightarrow H_2O + 2O_2 \tag{4}$$

$$O_3 + OH^- \rightarrow HO_2^{\bullet} + O_2^{\bullet}$$
(5)

$$O_3 + OH^- \rightarrow HO_4^- \tag{6}$$

 $\mathrm{HO}_{2}^{\bullet} \leftrightarrow \mathrm{O}_{2}^{-\bullet} + \mathrm{H}^{+} \tag{7}$ 

 $O_3 + O_2^{\bullet} \to O_3^{\bullet} + O_2 \tag{8}$ 

$$O_2^{-\bullet} + H^+ \to HO_3^{-\bullet} \tag{9}$$

$$\mathrm{HO}_{3}^{-\bullet} \to \mathrm{HO}^{\bullet} + \mathrm{O}_{2} \tag{10}$$

 $O_3 + OH^{\bullet} \rightarrow HO_2^{\bullet} + OH^{-}$ (11)

 $O_3 + OH^{\bullet} \rightarrow HO_4^{\bullet}$ 

 $OH^- + OH^{\bullet} \leftrightarrow H_2O + O^{\bullet^-}$  (13)

 $\mathrm{HO}_{4}^{\bullet} \to \mathrm{HO}_{2}^{\bullet} + \mathrm{O}_{2}^{-\bullet} \tag{14}$ 

$$HO_4^{\bullet} + HO_4^{\bullet} \rightarrow H_2O_2 + 2O_3 \tag{15}$$

$$HO_4^{\bullet} + HO_3^{\bullet} \rightarrow H_2O_2 + 2O_3 + O_2$$
(16)

The process of ozonation can be carried out as an effective single method or combined with other oxidizing agents or UV radiation in order to increase its efficiency and reduce process times. O<sub>2</sub> based processes can be used for the treatment of industrial wastewater, for example, Lucas et al. [17] showed that O<sub>2</sub>/UV and O<sub>2</sub>/UV/H<sub>2</sub>O<sub>2</sub> processes can treat winery wastewaters. Kim and Tanaka [18] reported that the comparison of  $O_2/H_2O_2$  and  $O_2/UV$  by an  $O_2$  dose equal to 6 mg/L and a 15 min contact time, can reduce the concentration of caffeine (CAF), N,N-diethyl-meta-toluamide and cyclophosphamide by 84%, 89%, and 46%, respectively, Chávez et al. [19] tested the process of UVA-LED photocatalytic ozonation and also achieve a nearly 90% removal of micropollutants occurring in municipal wastewater secondary effluent. Also, the process of heterogeneous catalysis can be applied in various branches of environmental chemistry because it allows for obtaining a different kind of species using various types of catalysts [20]. For example, the use of TiO<sub>2</sub> in the process of heterogeneous photocatalysis is one of the best-known processes for the decomposition of many types of contaminants [21,22]. However, it should be noted that the combination of some well-known processes in water treatment technologies like chlorination with other advanced processes can lead to the formation of intermediates with a larger number of Cl- atoms in their structure than in the structure of the parent organic pollutant [23]. Newly formed compounds can have high biological activity and can be considered very toxic to the environment.

Some researchers classify micropollutants of anthropogenic origin to the group of compounds of emerging concern, which can have a possible harmful effect on water organisms and human health. Therefore it is necessary not only to develop methods for their removal but also methods, which guarantee the mineralization of the risk to form biological active decomposition by-products. There is a need to evaluate the removal degrees of each type of compound in different conditions with special attention to toxicological assessment (acute and chronic toxicity) of post-processed waters carried out by the use of toxicity tests using different indicator organisms.

The paper presents the comparison of removal degrees of selected organic micropollutants most commonly occurring in the water environment, subjected to the  $O_3$  and  $O_3/H_2O_2$  process supported by sunlight. The obtained results were compared to the  $O_3/H_2O_2$  conducted in a dark chamber. The influence of the  $O_3$  dose and the time of sunlight exposure on the generation of possible compound decomposition by-products were assessed. Also, toxicological analyzes of post-process water solutions were carried out using three biotests: Microtox<sup>®</sup>, DAPHTOXKIT F *magna*, and *Lemna* sp. Growth Inhibition Test (GIT).

## 2. Material and methods

(12)

### 2.1. Material and reagents

The analytical standards of all tested compounds that is, pharmaceuticals: benzocaine (BE), CAF, carbamazepine (CBZ), diclofenac sodium salt (DCF) and ibuprofen sodium salt (IBU); hormones:  $\beta$ -estradiol (E2), 17 $\alpha$ -ethinylestradiol (EE2), mestranol (EEME) and progesterone (P4); pesticides: triallate (TRI), triclosan (TCS) and oxadiazon (ODZ); food additives: butylated hydroxytoluene (BHT); and dyes: acridine(ACR) of a purity grade >97% were supplied by Sigma-Aldrich (Poznań, Poland). Table 1 summarizes the chemical characteristic of the tested micropollutants. Organic solvents in the form of methanol (MeOH), dichloromethane (DCM) and acetonitrile (ACN) with a purity over 99.5% were used during the preparation of compound standard solutions and the process of solid-phase extraction (SPE) were obtained from Avantor Performance Materials Poland S.A. (Gliwice, Poland).SPE cartridges Supelclean™ ENVI-8 and ENVI-18 equipped with a silica gel base material with  $C_8$  (octyl) and  $C_{18}$  (octadecyl) bonding respectively were supplied by Sigma-Aldrich (Poznań, Poland). The bed weight of both types of SPE cartridges was equal to 1,000 mg with a 60 Å pore size and a total surface area of  $475 \text{ m}^2/\text{g}$ .

#### 2.2. Decomposition processes

Both, O<sub>3</sub> and O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub> sunlight supported compound decomposition processes were carried out in glass batch reaction vessels with a volume of 1.0 L. The vessels were placed on a magnetic stirrer to ensure continuous mixing of the reaction mixture. In order to estimate the influence of sunlight on the course of the decomposition reactions, the O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub> process was carried out comparatively in a dark chamber. The O<sub>2</sub> used in the experiments was generated from fresh air in the Ozone FM500 generator by WRC Multiozon (Sopot, Poland). The generated O<sub>2</sub> was introduced to the reaction vessels through a ceramic diffuser, which was placed 1 cm above the bottom of the vessel. The processes were carried out at different O<sub>2</sub> doses: 1.0, 2.0, 3.0, 5.0 and 10.0 mg/L ( $O_3$  dose measured immediately after its introduction to the water matrix). The concentration of O<sub>2</sub> was measured photometrically using the Spectroquant<sup>®</sup> Ozone Test by Merck KGaA (Darmstadt, Germany) in a sample taken from the middle of the reaction mixture. The dose of H<sub>2</sub>O<sub>2</sub> was determined during preliminary studies and set on 9 mg/L. The reaction vessels containing the test solutions were exposed to sunlight radiation for 10, 20, 30 and 60 min. The experiments were conducted during the European summer period between July and August, where the average illumination intensity was 850±45 mW/cm<sup>2</sup> and the measured air temperature ranged from 22.2°C to 29.4°C. The temperature of water solutions exposed to  $O_3$  and  $O_3/$ H<sub>2</sub>O<sub>2</sub> supported by the action of sunlight ranged from 24°C to 26°C. Whereas the temperature of the solution in the dark chamber experiment was kept at a level of 24°C±1°C. The ozonation reaction was stopped by the introduction to the reaction mixture 24 mmol/L of Na<sub>2</sub>SO<sub>3</sub> by Sigma-Aldrich (Poznań, Poland).

Experiments for all tested micropollutants were carried out separately.

#### 2.3. Water samples

The tested micropollutant water solutions were prepared based on the deionized water with the addition of compound standard solutions. The standard solutions were prepared by dissolving 10 mg of each tested compound in 10 mL of MeOH. The micropollutant concentration in the prepared water solution was set on 0.5 mg/L. This high concentration allowed for the proper identification of the generated compound decomposition by-products. The pH of all water solutions was adjusted to 7.0 using 0.1 mol/L NaOH. The used volume of NaOH did not show any significant effect on the decomposition of the tested compounds before the implementation of the sunlight supported O<sub>3</sub> and O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub> processes.

## 2.4. Analytical procedure

The concentration of the tested micropollutants in the solutions before and after the implementation of selected decomposition processes as well as the identification of generated decomposition intermediates was estimated by the use of gas chromatography coupled with mass detection GC-MS(EI) performed by 7890B gas chromatograph by Agilent Technologies (Santa Clara, United States).

The chromatographic quantitative-qualitative analysis was preceded by solid-phase SPE of the micropollutants that occurred in the tested water solutions. They analyzed the volume of water solutions that were equal to 20 mL and the pH of each sample was adjusted to 7.0 by the use of 0.1 mol/L HCl (purity grade >99.8%) from Avantor Performance Materials Poland S.A. (Gliwice, Poland). The correction of pH was necessary especially in samples after the sunlight supported processes, during which an increase in pH to a value of up to 8.3 was observed. Details of the used SPE extraction for different compounds were summarized in Table 2. Recovery of the micropollutants after the implemented SPE conditions exceeded 96%.

The obtained micropollutant extracts were injected into the chromatographic capillary column SLB<sup>TM</sup> - 5 ms 30 m × 0.25 mm of 0.25 µm film thickness by Sigma-Aldrich (Poznań, Poland). The carrier gas (helium 5.0) flow rate was set on 1.1 ml/min. The injector temperature was equal to 250°C. The oven temperature program started with 80°C (held for 6 min) and then the oven was heated 5°C/min up to 260°C, 20°C/min up to 300°C (held for 2 min). The temperature of the ion trap and ion source was set at 150°C and 230°C respectively. The quantitative analysis was operated in the selected ion monitoring mode, while the qualitative analysis was performed in the total ion current (TIC) model ranged from 50 to 400 m/z.

The percentage of removal of each tested micropollutant after the application of the decomposition processes was calculated by the determining of the initial  $C_i$  and post-processed  $C_p$  compound concentrations (mg/L) according to Eq. (17):

$$\operatorname{Removal}(\%) = \frac{C_i - C_p}{C_i} \times 100 \tag{17}$$

The identification of compound decomposition by-products in the post-processed samples was made based on their mass spectra, which were compared with the United States National Institute of Standards and Technology NIST v17 Mass Spectral Library.

Table 1				
Chemical	characteristics of	of investigated	micropollutants	[24]

Compound	Structural formula	CAS No	Molecular weight (g/mol)	Solubility in water (mg/L)	pK <sub>a</sub>	logK <sub>ow</sub>
BE	O H <sub>2</sub> N	94-09-7	165.19	1,310	2.51	1.86
CAF	N N N	58-08-2	194.19	21,600	14.0	-0.07
CBZ		298-46-4	236.30	17	2.30	2.45
DCF		15307-79-6	318.13	50	4.15	0.57
IBU	CH <sub>3</sub> ONa	31121-93-4	228.26	100	4.91	3.30
E2	HO H H	50-28-2	272.38	3.6	10.33	4.01
EE2	H H H	57-63-6	296.40	11.3	10.33	3.67
EEME	H <sub>3</sub> C OH H <sub>3</sub> C OH H <sub>3</sub> C OH H <sub>1</sub> C≡CH	72-33-3	310.43	1.13	17.59	4.61
P4	H <sub>3</sub> C H H <sub>1</sub> C H H H	57-83-0	314.46	8.81	18.92	3.87
TRI	$CH_3 O CI$ $H_3C N S CI$ $H_4C CH_3 CI$	2303-17-5	304.66	2.00	a	4.60
TCS		3380-34-5	289.54	10.00	7.9	4.76
ODZ	$CI \rightarrow CH_{3}C$ $H_{3}C \rightarrow CH_{3}$ $H_{3}C \rightarrow CH_{$	19666-30-9	345.22	0.70	b	4,80
BHT	H <sub>9</sub> C H <sub>9</sub> C CH <sub>9</sub> C CH <sub>9</sub> C	128-37-0	220.35	0.6	12.23	5.10
ACR		260-94-6	179.22	38.4	5.6	3.40

<sup>a</sup>no data; <sup>b</sup>non-ionizable;

Table 2 SPE details for tested organic micropollutants

Compound	BE, CBZ, DCF, IBU,BHT	CAF, ACR, TRI, TCS, ODZ	E2, EE2, EEME, P4
Cartridge type	Supelclean™ ENVI-8	Supelclean <sup>™</sup> ENVI-18	
Bed conditioning	5.0 mL of MeOH	5.0 mL of ACN; 5.0 mL of MeOH	3.0 mL of DCM;
			3.0 mL of ACN;
			3.0 mL of MeOH
Volume of deionized water used	5.0		
for bed washing (mL)			
Sample flow (mL/min)	1.0		
Vacuum drying time after	5.0		
sample filtration (min)			
Extract elution	3.0 mL of MeOH	1.5 mL of MeOH; 1.5 mL of ACN	2.0 mL of DCM;
			1.5 mL of ACN;
			1.5 mL of MeOH

The results with the marked error bars presented in all figures are the arithmetic average of three replicates of each experiment. The error bars' ranges were estimated based on the standard deviation and did not exceed 4%.

#### 2.5. Toxicity tests

The toxicity of the post-process micropollutants water solution was estimated by three different biotests, that is, Microtox<sup>®</sup> test, DAPHTOXKIT F<sup>®</sup> test, and *Lemna* sp. GIT.

The Microtox<sup>®</sup>bioassay measured the changes in the behavior of bioluminescent saltwater bacteria *Aliivibrio fischeri*. The test was carried out by the use of the Microtox analyzer Model 500 by Modern Water (London, United Kingdom) according to the Screening Test procedure of MicrotoxOmni system. The Daphtoxkit F<sup>®</sup> test measures the immobility or mortality of freshwater crustaceans *Daphnia magna* after a 24 h exposition to the tested water samples. Whereas the *Lemna* sp. GIT base on the measurement of the number of plant fronds of freshwater vascular plants *Lemna minor*, which grows for 7 d in the tested water solution. The toxicity effect for both the Daphtoxkit F<sup>®</sup> test and the *Lemna* sp. Growth Inhibition Test was calculated by Eq. (18). Details of the conducted test were given in [24].

$$E = \frac{\left(N_c - N_T\right)}{N_c} \times 100 \tag{18}$$

where *E* – toxicity effect (%);  $N_c$  – number of lively organisms (plant fronds) in the control sample;  $N_T$  – number of lively organisms (plant fronds) in the test sample.

The obtained toxicity results were interpreted based on the toxicity classification system presented in Table 3 [25,26].

## 3. Results and discussion

## 3.1. $O_3$ and $O_3/H_2O_2$ decomposition process supported by sunlight

Fig. 1 presents the results of the first stage of the study that focused on the determination of the optimum  $O_3$  concentration during the  $O_3$ /sunlight process. Five different

O<sub>3</sub> doses (1.0, 2.0, 3.0, 5.0 and 10.0 mg/L) were tested. The micropollutant water solutions were exposed to 10 min of sun lightening after the introduction of the chosen dosage of O<sub>2</sub>. It was noted, that the removal degree of all tested micropollutants increased with the increase of the O<sub>2</sub> dose. The highest differences in compound decomposition were noted between the O<sub>3</sub> concentration of 5.0 and 10.0 mg/L. For example, the removal of IBU after the implementation of the process with a dose of 5.0 mg/L of O<sub>2</sub> was equal to 26% and increased to 52% by doubling the O<sub>2</sub> dose. In general, compounds from the group of pharmaceuticals were characterized by a low ozone caused removal degree compared to other tested micropollutants. The lower decomposition was noted for DCF solutions and ranged from 2% for the 1 mg/L O<sub>3</sub> dose to 17% for 10 mgO<sub>3</sub>/L. Coelho et al. [27] noted that the mineralization of DCF and IBU during the O<sub>2</sub> and O<sub>2</sub>/UV-VIS processes did not exceed 30%.

It should be noted that exposure to sun lightening had a beneficial impact on the  $O_3$  decomposition of compounds. Previous studies [24] dedicated to the dark chamber  $O_3$ decomposition of micropollutants indicated only a slightly decrease in their concentrations. For example, the removal degree of micropollutants by the dose of 1 mg/L of  $O_3$  did not exceed 10% and for the dose of 10 mg/L ranged from 2% for CAF to 52% achieved for the TCS decomposition. The sunlight radiation compared with the action of  $O_3$  and other radicals generated during the reaction from (1) to (16) mentioned above, allowed for the increase of TCS decomposition to over 81% by the use of 5 mgO<sub>3</sub>/L and 94% for the  $O_3$  dose equal to 10 mg/L. Muhamad [28] indicated that the source of

Table 3	
oxicity classification system of water samples [25,26]	

Effect (%)	Description	Toxicity class
<25.00	Non toxic	Ι
25.00-50.00	Low toxic	II
50.01-75.00	Toxic	III
75.01–100	Highly toxic	IV



Fig. 1. Influence of the O<sub>3</sub> on the micropollutant removal degree during the O<sub>3</sub>/sunlight irradiation process (10 min irradiation).

radiation plays an important role in pesticide removal and observed that pesticides occurred in water solutions exposed to UV-light decompose faster than those in samples irradiated with visible light or direct sunlight.

Due to the fact that the  $O_2$  in a concentration of 10 mg/L causes the highest removal degrees of al tested compounds this dose was used in future experiments dedicated to the estimation of the dependence of sun lightening time on the decomposition of tested micropollutants. Fig. 2 summarizes the compound removal degrees observed during the O<sub>2</sub>/ sunlight process carried out for 10, 20, 30 and 60 min. It was shown that the elongation of the sample sun exposure time leads to a decrease in compound concentration for all tested micropollutant water solutions. The increase of the compound removal with the increasing process time was especially visible in the case of DCF solutions. The removal of this pharmaceutical increases from 17% after 10 min of irradiation to 68% after 60 min of irradiation. The least influence of sunlight irradiation time was observed for CBZ. The concentration of the compound was reduced in the range from 48% to 51%. 60 min of O<sub>2</sub>/sunlight process duration allowed for an over 90% reduction in the concentration of all tested pesticides (E2, EE2, EEME, and P4), BHT, TCS, and ODZ. However, the studied process time intervals did not allow for a complete removal of none of the tested micropollutants.

To improve the particular compound decomposition degrees a second type of oxidant in the form of  $H_2O_2$  was introduced to the reaction mixtures.  $H_2O_2$  exhibits oxidant and reductant properties and can be effectively used in a wide range of temperatures and pH values [29]. The irradiation of  $H_2O_2$  with sunlight, which is a source of UV lightening, leads to its direct photolysis and the generation of HO<sup>•</sup> radicals according to reaction (19) [30] and improves the oxidative capacity of the reaction mixture.

$$H_2O_2 + hv \to 2HO^{\bullet} \tag{19}$$

The performance of the  $O_3/H_2O_2$ /sunlight allowed for the achievement of higher removal degrees of all tested compounds except of ACR, TCS and CAF (Fig. 3). The decomposition of ACR and TCS was at the same level in both  $O_3/$ 

sunlight and  $O_3/H_2O_2$ /sunlight processes, whereas the removal degrees of CAF observed in the  $H_2O_2$  supported were lower than them noted for the single  $O_3$ /sunlight.

The simultaneous action of  $O_{37}$ ,  $H_2O_2$ , and sunlight allowed for complete removal of E2 and EE2 after 60 min of process duration. High removal degrees reaching 98% and 99% were also noted for EEME and P4 respectively. Also, the removal of ODZ exceeded 95%. The highest removal of the compound from the group of pharmaceuticals was achieved for DCF and IBU. The concentration of both micropollutants decreased after 60 min of the O<sub>2</sub>/H<sub>2</sub>O<sub>2</sub>/sunlight process by over 81% and 74% respectively. It can be assumed that the introduction of different types of oxidants and/or reactive radical's precursors to micropollutant water solutions had always a positive impact on their removal regardless of their physicochemical properties. Fernandes et al. [31] demonstrated that even volatile organic compounds can be effectively decomposed by the  $TiO_2/UV/O_2/H_2O_2$  treatment system. However, some formed oxidative radicals like OH<sup>•</sup> radicals can react with O<sub>3</sub> molecules and accelerate their distribution to H<sub>2</sub>O and O<sub>2</sub> [32].

To estimate the real impact of sunlight on the decomposition process of micropollutants the O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub> process was performed in a dark chamber. The obtained results were presented in Fig. 4. The absence of the lightening source causes an explicit reduction of the decomposition effectiveness of all tested micropollutants. For example, a visible reduction in CAF concentration was noted only after 30 min of process duration and was equal to 1%. After 60 min of the dark chamber experiment, the concentration of this compound decreased by 2%. A similar low decomposition, which did not exceed 8% was noted in the case of the DCF solution. Also, low removal degrees, which did not exceed 43%, were obtained during the decomposition of hormones, which were particularly completely removed in sunlight supported processes. The highest decrease in concentration after 10 min of process duration reached 28% was noted for TCS, while the highest compound removal after 60 min was observed for the BHT solution and reached a value of 67%.

It can be assumed that sunlight supports the decomposition of a compound by the generation of highly reactive radicals, which can break the bonds occurring between the atoms of a compound molecule. A high removal degree of parent



Fig. 2. Influence of the irradiation time on the micropollutant removal degree during the  $O_3$ /sunlight irradiation process ( $O_3$  dose equal to 10 mg/L).



Fig. 3. Influence of the irradiation time on the micropollutant removal degree during the  $O_3/H_2O_2/sunlight$  irradiation process ( $O_3$  dose equal to 10 mg/L).



Fig. 4. Influence of the irradiation time on the micropollutant removal degree during the O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub> (O<sub>3</sub> dose equal to 10 mg/L).

compounds is not always related to its complete mineralization. The decomposition of a micropollutant often leads to the formation of several by-products.

#### 3.1. Identification of micropollutant decomposition by-products

The GC-MS analysis conducted in the TIC mode indicated the formation of several decomposition by-products of the tested compounds. The mass spectra of each peak noted on the chromatograms next to the peak corresponding to the parent compound was compared to the NIST v17 mass spectra library. Compound with a matching similarity over 70% were considered to be the possible formed intermediated. Table 4 summarizes all compounds matched in samples collected from both, sunlight supported and dark chamber experiments.

The largest number of decomposition by-products was observed during the DCF decomposition in the process of O<sub>2</sub>/sunlight irradiation. This pharmaceutical compound decomposed in the first 10 min to 7 intermediates that is, 4',5-dihydroxydiclofenac, 5-hydroxydiclofenac, 2,6-dichlorodiphenylamine, 2,6-dichloroaniline, 2,6-dichloro-4-aminophenol, 2-aminophenyl acetic acid, and 2-hydroxyphenyl acetic acid. The DCF intermediates detected during the performed oxidation processes were similar to those noted in future studies [33] and during experiments conducted by Yu et al. [34]. Also, CBZ and IBU decomposed to 5 by-products, which in the case of CBZ were: 3-hydroxycarbamazepine, 10, 11-dihydro-10-hydroxycarbamazepine, dihydrocarbamazepine-10, 11-trans-diol, 9-acridone and acridine, whereas IBU post-processed samples contained: 1-hydroxyibuprofen, 1-(4-isobutylphenyl) ethanol, 4'-isobutylacetophenone, 4-acetylbenzoic acid, and 4-ethylbenzaldehyde. During the decomposition of BE, CAF, and EE2 only one intermediate could be identified. The CAF by-product N,N'dimethylparabanic acid was also identified by Neves et al [35], which investigated the possibility of CAF oxidation by the use of H<sub>2</sub>O<sub>2</sub> catalyzed by metalloporphyrins processes. Special attention should be paid to ACR, which was formed during the CBZ decomposition. The oxidation of this compound leads to the generation of three intermediates with the same molecular formula C<sub>13</sub>H<sub>9</sub>NO and therefore, also with the same molecular weight.

The formation of diallate during TRI decomposition raises concerns. This compound was classified by the Human Health Assessment Group in EPA's Office of Health and Environmental Assessment as a pesticide with possible human carcinogen possibilities [36]. Also the oxidation of P4 leads to the formation of 3 intermediates: corticosterone, aldosterone, and cortisone, which are well-known hormones. The connection of a second –OH group to the E2 compound resulted in the formation of 2-hydroxyestradiol, which was also detected by Mboula et al. [37] during the photocatalytic degradation of E2 under simulated solar light.

It was noted, that the concentration of intermediates observed in samples exposed to sunlight supported processes increases in the first 20 min of process duration. The concentration increase was estimated based on the increase of the peak areas corresponding to identify by-products. For example, the concentration of the TRI and TCS intermediates increased between 10 and 20 min of the O<sub>3</sub>/sunlight process by over 20%, while the concentration of the E2 by-products 2-hydroxyestradiol and estradiol-3, 4-quinone increases in the same period by nearly 12% and 15% respectively. The continuation of the sunlight exposure resulted in a fast decomposition of the main of newly formed intermediates. Therefore the samples after 60 min of sun irradiation were characterized by a significantly lower number of decomposition by-products. An inverse relation was observed for the dark chamber  $O_3/H_2O_2$  process. The number and concentration of intermediates increases with the increase in the processing time.

#### 3.2. Toxicity analysis of post-processed water samples

The decrease of compounds concentrations after the conducted processes and the detection of several micropollutant intermediates force the performance of a toxicological analysis on different indicator organisms belonging to bacteria, crustaceans, and vascular plants. Figs. 5-7 compare the toxic effect of micropollutant water solutions before and after oxidation processes. The used toxicity bioassays are characterized by a different sensitivity to the tested compound groups. The estimation of the toxic effect by the use of the Microtox® test of compound solutions before decomposition shows that only the TCS solution can be classified according to the toxicity classification (Table 3) as highly toxic. The EE2 and ACR solutions were described by this test as low toxic, while other compound water solutions were found to be non-toxic. Whilst the DAPHTOXKIT F® test classified the TRI and TCS solution as toxic and the EE2 solution, similar to the Microtox<sup>®</sup> test, as low toxic (Fig. 6). The highest sensitivity against ODZ was noted for the Lemna sp. GTI (Fig. 7). The vascular plant classified this compound as highly toxic.

The subjection of the tested micropollutant solutions to the decomposition processes resulted in an increase of their toxicity. The observed toxicity effect corresponded to the results of the mass spectrometry analysis. The formed intermediates had a harmful effect on the tested organism's behavior. The highest toxic effect was observed for both, saltwater bacteria, freshwater crustaceans and vascular plant bioassays in samples subjected to the  $O_3/H_2O_2$  dark chamber process. Only in the case of CAF and DCF, a higher toxic response was noted in samples after the  $O_3$ /sunlight process. Also the *Lemna* sp. GIT was more sensitive to intermediates formed during the  $O_3$ /sunlight decomposition of BHT than to them formed after other processes.

Irrespective of the decomposition process BE, CAF, DCF and IBU post-processed samples were classified by all toxicity tests as non-toxic. Only the pharmaceutical CBZ solution was after the O<sub>3</sub>/sunlight process characterized by low toxicity according to all bioassays, and highly toxic (Microtox<sup>®</sup> and DAPHTOXKIT F<sup>®</sup>test) after the O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub> dark chamber process.

The toxicity results obtained for the hormone post-processed samples by the Microtox<sup>®</sup> and DAPHTOXKIT F<sup>®</sup>tests were very similar. For example, both tests classified the EEME solutions subjected to the action of the dark chamber and the sunlight  $O_3/H_2O_2$  as toxic, whereas the  $O_3$ /sunlight lead to the increase of the toxicity only to a low toxic level. A different toxic effect was only noted in the case of P4 solutions exposed

## Table 4 Summary of micropollutant decomposition by-products

Parent compound	Identified compound	Molecular weight	Sunlight supported			1	Dark chamber O <sub>3</sub> /H <sub>2</sub> O <sub>2</sub>	
1	1	(g/mol)	0		0/H 0			
			10 min	60  min	10  min	60  min	10 min	60 min
BF	ethyl 4-hydroxybenzoate	166 17	+	+	+	_	+	+
CAF	N.N'-dimethylparabanic acid	142 11	+	+	+	_	+	_
CBZ	3-hydroxycarbamazepine	252.27	+	_	+	_	_	+
CDE	10.11-dibydro-10-	254.28	+	_	+	_	_	+
	hydroxycarbamazepine							
	dihvdrocarbamazepine-10,	270.28	+	+	+	_	_	+
	11-trans-diol							
	acridone	195.22	+	+	+	_	_	_
	acridine	179.22	+	+	+	_	_	_
DCF	4',5-dihydroxydiclofenac	328.10	+	_	+	_	+	+
	5-hydroxydiclofenac	312.10	+	-	-	_	+	+
	2,6-dichlorodiphenylamine	238.11	+	+	_	-	_	-
	2,6-dichloroaniline	162.01	+	+	-	-	_	_
	2,6-dichloro-4-aminophenol	178.01	+	-	+	-	+	+
	2-aminophenylaceticacid	151.16	+	+	-	-	_	-
	2-hydroxyphenylacetic acid	152.15	+	-	-	-	+	+
	2,3-dihydroxyphenylacetic acid	168.15	-	-	+	-	+	+
IBU	1-hydroxyibuprofen	222.28	+	-	-	-	-	+
	1-(4-isobutylphenyl)ethanol	178.27	+	-	+	-	-	+
	4'-isobutylacetophenone	176.25	+	-	-	-	-	+
	4-acetylbenzoic acid	164.16	+	+	+	+	+	+
	4-ethylbenzaldehyde	134.17	+	-	-	-	+	+
E2	2-hydroxyestradiol	288.40	+	-	+	-	-	+
	estradiol-3,4-quinone	286.40	+	-	-	-	-	+
	4-(1-hydroxyethyl)phenol	138.16	+	-	+	-	+	+
EE2	4-hydroxy-ethinylestradiol	312.40	-	+	-	-	-	+
EEME	2,6-di-tert-	222.32	+	-	+	+	+	+
	butylhydroquinone							
	2-hydroxy-3-methoxy-estrone	300.40	+	-	-	-	-	+
P4	corticosterone	346.50	+	-	+	-	+	+
	aldosterone	360.40	+	-	-	-	+	+
	cortisone	360.40	+	-	-	-	+	+
TRI	diallate	270.22	+	+	-	-	+	+
	N,N-diisopropylformamide	129.20	+	-	+	-	+	+
TCS	2,3-dichlorophenol	163.00	+	-	+	-	+	+
	4-chlorophenol	128.56	+	_	+	-	+	+
ODZ	5-tert-butyl-3-(2,4-dichloro-	303.14	+	+	_	_	+	+
	5-hydroxyphenyl)-1,3,4-							
	oxadiazol-2 (3H)-one							
	4,6-dichlororesorcinol	178.00	+	+	+	+	+	+
BHT	2,6-di-tert-	222.32	_	+	+	_	+	+
	butylhydroquinone							
	tert-butylhydroquinone	166.22	+	+	+	_	+	+
ACR	acridone	195.22	+	+	+	_	+	+
	acridine-10-oxide	195.22	+	+	+	_	_	+
	2-hydroxyacridine	195.22	+	_	+	_	_	+

+ - compound identified in the sample; - - compound not identified in the sample



Fig. 5. Toxicity of post-processed samples after 60 min of process duration – estimated by the Microtox<sup>®</sup> test (where: non – samples before the decomposition process;  $O_3/sun$  – samples exposed to  $O_3$  and sunlight radiation;  $O_3/H_2O_2/sun$  – samples exposed to  $O_3$  and  $H_2O_2$  supported by sunlight;  $O_3/H_2O_2$  – samples subjected to the action of  $O_3$  and  $H_2O_2$ ).



Fig. 6. Toxicity of post-processed samples after 60 min of process duration – estimated by the DAPHTOXKIT  $F^{\oplus}$  (where: non – samples before the decomposition process;  $O_3$ /sun – samples exposed to  $O_3$  and sunlight radiation;  $O_3/H_2O_2$ /sun – samples exposed to  $O_3$  and  $H_2O_2$  supported by sunlight;  $O_3/H_2O_2$  – samples subjected to the action of  $O_3$  and  $H_2O_2$ ).



Fig. 7. Toxicity of post-processed samples after 60 min of process duration – estimated by the *Lemna* sp. GTI (where: non – samples before the decomposition process;  $O_3$ /sun – samples exposed to  $O_3$  and sunlight radiation;  $O_3/H_2O_2$ /sun – samples exposed to  $O_3$  and  $H_2O_2$  supported by sunlight;  $O_3/H_2O_2$  – samples subjected to the action of  $O_3$  and  $H_2O_2$ ).

to the O<sub>3</sub>/sunlight process, where the Microtox<sup>®</sup> test shows a low toxicity and the DAPHTOXKIT F<sup>®</sup>tests indicate a higher toxic value, which classifies the sample as toxic. The *Lemna* sp. GTI indicated an over 58% toxic effect in all hormone water samples after 60 min of the O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub>/dark chamber process. It can, therefore, be assumed that the vascular plants are sensitive to the generated decomposition intermediates. Adeel et al. [38] indicated a harmful effect on different types of endocrine-disrupting chemicals occurring in the water environment on a plant, animal and human health.

Special attention should be pay to the pesticide post-processed samples, which in general had a negative impact on living organisms. For example, the Microtox<sup>®</sup> and DAPHTOXKIT F<sup>®</sup>test classified the TRI solution after all tested processes as highly toxic. Also, the TCS post-processed solutions were considered being highly toxic according to the DAPHTOXKIT F<sup>®</sup>test. Only ODZ solutions were classified by the Microtox<sup>®</sup> as low toxic or toxic, whereas the DAPHTOXKIT F<sup>®</sup> test assigned them as toxic. The *Lemna* sp. GTI show an over 92% toxic effect of all pesticide samples subjected to the O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub>/dark chamber process, also the TRI and ODZ samples were classed as highly toxic after the O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub>/sunlight and the O3/sunlight process respectively.

Differences in the sensitivity of the used bioassays were also noted in the case of ACR post-processed solutions. For example, the Microtox<sup>®</sup> test indicates a higher toxic effect of all tested samples containing this compound then the DAPHTOXKIT F<sup>®</sup>, however, both tests assigned the samples to the same toxicity classes. Only the *Lemna* sp. GTI indicated a toxic level of ACR O<sub>3</sub>/H<sub>2</sub>O<sub>2</sub>/dark chamber samples, whereas the bacterial and the crustaceans test show low toxicity of those water samples. Belmont et al. [39] indicated that acridine and acridone analogues show potential cytotoxicity. On the other hand, acridine and acridone derivatives becoming more and more interesting do to their anticancer activity [40].

#### 4. Conclusions

The results obtained during the conducted studies indicated that sunlight strongly increases the effectiveness of O<sub>2</sub> decomposition of all types of studied micropollutants. The highest compound removal degrees, which exceeded 92%, were noted for micropollutants belonging to the group of hormones and pesticides. However, the removal of compounds depended on their chemical structure and the types of bound occurring between the atoms of the molecule. It was noted, that the presence of H<sub>2</sub>O<sub>2</sub> during the O<sub>2</sub>/sunlight process resulted in faster decomposition of compounds especially CBZ, IBU, BHT, and all tested hormones and pesticides. A second type of oxidant lead also to a decrease in the number of generated micropollutant intermediates. The conduction of the O<sub>2</sub>/H<sub>2</sub>O<sub>2</sub> process without the exposure to sunlight not only effects on a slower decomposition of tested compounds but also lead to the increase in the concentration of particular intermediates, which were more slowly oxidized than their parent compounds. The conducted toxicological analysis confirmed the reduction of the toxic nature of samples subjected to sunlight assisted O<sub>2</sub>/H<sub>2</sub>O<sub>2</sub> process compared to samples treated by the action of  $O_{a}$ H<sub>2</sub>O<sub>2</sub> performed in a dark chamber. The chosen toxicological test showed different sensitivity to the formed toxic compound intermediates.

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