

Efficient removal of carmoisine dye from aqueous solution using Fe₃O₄ magnetic nanoparticles modified with asparagine

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ABSTRACT

In the present study, Fe₃O₄@SiO₂-NH₂-Asn magnetic nanoparticles (MNPs) were prepared and used for the first time as an efficient adsorbent for the removal of Carmoisine dye from aqueous solutions. Characterization of the synthesized adsorbent was performed by transmission electron microscopy, field emission scanning electron microscopy, Fourier transform infrared spectroscopy, X-ray diffraction, and vibrating sample magnetometer instruments. Taguchi experimental design method (OA₁₆) was utilized to evaluate the effect of adsorption parameters on the dye removal efficiency from aqueous solutions. Experimental results showed 96.6% removal efficiency of Carmoisine dye from aqueous solutions at pH = 3, adsorbent weight = 0.08 g, ionic strength = 0.05 mol L⁻¹, and contact time = 20 min. The adsorption isotherm studies with Freundlich, Langmuir, and Temkin isotherm models revealed that the adsorption data were best fitted to the Freundlich model ($R^2 = 0.9989$, $n = 0.19$), which showing multilayer adsorption of the dye on the adsorbent surface. The kinetic data were investigated by pseudo-first-order, pseudo-second-order, intra-particle diffusion, and Elovich kinetic models. According to obtained data, the pseudo-second-order kinetic model was the best model for describing the adsorption kinetic ($R^2 = 0.9999$). In addition, the Fe₃O₄@SiO₂-NH₂-Asn MNPs could be easily recovered by an external magnet and it displayed reusability for the subsequent seven runs. The results of Carmoisine removal from real samples showed that the Fe₃O₄@SiO₂-NH₂-Asn MNPs are appropriate adsorbents for the elimination of this pollutant from aqueous media.

Keywords: Asparagine; Carmoisine; Dye; Fe₃O₄@SiO₂-NH₂-Asn; Magnetite; Removal

1. Introduction

In the last years, protection of water has been a deepening worldwide challenge on account of growing water contamination and water reduction discharged (disposed) of the chemical industry with the process of urbanization and industrialization [1–3]. Different pollutants such as

antibiotics, organic dyes, benzene, and its derivatives, and heavy metals, etc. would result in unavoidable influences on human health and even induce various crucial illnesses like cerebrovascular diseases, leukemia, cancer, etc. due to their toxicity of cumulation, mutagenicity, and even carcinogenicity [4–8]. Moreover, organic dyes could hardly be degraded with the conventional purification technique because of their low biodegradability and high dissolubility [9]. Carmoisine

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(C₂₀H₁₂N₂Na₂O₇S₂) is a water-soluble, sulfonated, anionic, mono-azo dye that is utilized in producing sausages and confectionery products, marzipan, candies, jams, soups, sauces, sweets, preserves, beverages, and a variety of other foodstuffs. On account of the different utilizes of carmoisine in food processing, carmoisine is usually found in the food processing factories effluent [10]. Thus, researching and developing effective and economic decontamination technology to resolve the aforementioned pollutions from wastewater remains a great challenge in water treatment.

Traditional techniques like chemical oxidation, coagulation, photocatalysis, adsorption, and ion exchange have been utilized for eliminating organic dyes from polluted waters [11–16]. These techniques are restricted to several factors like the utilization of special equipment, high cost, dye incomplete elimination, and production of poisonous residues causing secondary pollution.

More consideration has lately been paid to the adsorption process because of its effectiveness, low cost, simplicity of design, and ease of operation [17–20]. This method can be employed for large-scale contaminated water repeatedly as it can handle fairly large flow rates, generating a high quality of water with no generating notorious sludge and residual contaminant. The development of dependable and cost-effective dye adsorbents has hence been a crucial issue to address.

The magnetic separation technique is affordable; it functions mainly in the swift adsorption of dyes [21,22]. Following the adsorption is completed using an external magnetic field, the adsorbents can be separated from the water system to avoid secondary pollution. The organic modified Fe₃O₄ nanocomposites are one of the most generally utilized magnetic materials, have been extensively utilized in lots of fields like magnetic resonance imaging, drug delivery, catalysis, and biotechnology [23–26]. Apart from this, organic modification Fe₃O₄ nano-composites had been broadly utilized in wastewater treatment because of their regeneration, easy separation, non-toxicity, and regeneration [26]. For instance, Toutounchi et al. [27] reported that magnetic ordered mesoporous carbon nanocomposite for the elimination of Ponceau 4R from the surface waters and dye industry. Cui et al. [28] reported urchin-like Fe₃O₄@PDA-Ag hollow microspheres could boost the efficiency of removal of rhodamine B and methylene blue from wastewater.

In this research, we have successfully fabricated Fe₃O₄@SiO₂-NH₂-Asn MNPs with a simple route and investigated MNPs performance for removal of Carmoisine dye from aqueous solutions. The effect of parameters affecting the adsorption of Carmoisine onto Fe₃O₄@SiO₂-NH₂-Asn, including the initial solution pH, ionic strength, adsorbent amount, and contact time, were systematically examined by batch adsorption experiments. The characteristic reflects that the Fe₃O₄@SiO₂-NH₂-Asn could be a high-efficiency adsorbent for the removal of Carmoisine from an aqueous solution.

2. Experimental

2.1. Chemicals and reagents

Ferrous chloride tetrahydrate (FeCl₂·4H₂O) (≥98.0%), ferric chloride hexahydrate (FeCl₃·6H₂O), hydrochloric acid (HCl) (37%, w/w), ammonia solution (25%, w/w), ethanol, toluene,

sodium chloride (NaCl), and Carmoisine were purchased from Merck Company (Darmstadt, Germany). Tetraethyl orthosilicate (TEOS) (98%), (3-aminopropyl) triethoxysilane (APTES) (99%), and L-Asparagine (≥98% (HPLC)) were bought from Sigma Company (Milwaukee, WI, USA). All chemical materials and solvents were used without further purification.

2.2. Instruments and apparatus

Fourier transform infrared (FT-IR) spectra were acquired in the range of 400–4,000 cm⁻¹, with a Shimadzu FT-IR 8600 spectrophotometer (Japan). The crystal phases of the prepared MNPs were evaluated at a scanning speed of 2°min⁻¹ from 10° to 80° (2θ), utilizing Philips Xpert X-ray powder diffraction (XRD) diffractometer (Cu K_α radiation, λ = 0.154056 nm, Netherlands). The size and morphology of the synthesized MNPs were studied utilizing the field-emission scanning electron microscopy (FESEM, Sigma-VP, Zeiss Company, Germany). The structural characteristics of the adsorbent were investigated utilizing transmission electron microscopy (TEM) with the Zeiss-EM10C device. A vibrating sample magnetometer (VSM, LDJ9600) was utilized for investigating the magnetic properties of fabricated MNPs. UV-vis spectra were recorded using Cary 60 UV-vis Spectrophotometer from Agilent Technologies (USA) equipped with a quartz cell. The pH of solutions was measured utilizing Bante 901 digital pH meter (China). For magnetic separation, a super-strong magnet (1 cm × 3 cm × 5 cm) with a 1.4 T magnetic field was employed. To investigate the surface charges of synthesized adsorbent, Zeta potential analyzer (Malvern Instruments Ltd., Malvern, United Kingdom) was used.

2.3. Preparation of Fe₃O₄@SiO₂-NH₂-Asn MNPs

2.3.1. Synthesis of Fe₃O₄

Fe₃O₄ MNPs were prepared via the co-precipitation method described in the literature. Briefly, FeCl₂·4H₂O (6.0 g), FeCl₃·6H₂O (9.3 g), and HCl 37% (4.5 mL) were dissolved in distilled water and the solution was adjusted to the mark of a 50 mL volumetric flask. Then, the solution was degassed for 20 min utilizing N₂ gas. In the next step, 250 mL of ammonia solution (1.5 mol L⁻¹) was added into a three-necked flask containing a magnet and was heated to 80°C in the oil bath. The solution of iron chlorides was added drop by drop to the solution of ammonia in a degassed environment for 60 min. After completion of the reaction, the MNPs were rinsed with double distilled water several times and were separated from the reaction environment with a super-strong magnet (1.4 T). The fabricated MNPs were kept in NaOH (0.1 mol L⁻¹) solution (24 h) to avoid the accumulation of MNPs. Finally, MNPs were rinsed with distilled water and were dried at 120°C in the oven for 120 min [29,30].

2.3.2. Aminopropyl surface modification of the Fe₃O₄ to form Fe₃O₄@SiO₂-NH₂

For silica coating, first, 0.7 g Fe₃O₄ was added in a solution containing ethanol (40 mL), 10 mL distilled water, and 0.6 mL ammonia solution, and then the solution was

sonicated for 30 min at 80°C. Afterward, 0.5 mL TEOS was added to the suspension and the mixture was strongly stirred at room temperature (r.t, 24 h). The mixture was separated by a magnet and rinsed three times with a 1:1 mixture of distilled water/ethanol, and finally dried at 70°C for 5 h. In the next step, for the synthesis of $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2$, a suspension including 1.0 g of $\text{Fe}_3\text{O}_4@ \text{SiO}_2$ in 100 mL toluene was sonicated (30 min). Next, 1 mL of APTES was added to the suspension, and the mixture was stirred for 24 h at r.t. The mixture was separated by a magnet and rinsed three times with toluene/ethanol (1:1), and finally dried at 70°C for 8 h.

2.3.3. Synthesis of $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2\text{-Asn}$

The synthesized $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2$ MNPs were functionalized with Asparagine. First, a suspension of 0.8 g $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2$ and 3.3 g Asparagine in 40 mL ethanol was sonicated for 10 min. Then, the mixture was refluxed for 8 h (80°C). Finally, the nanoparticles were washed with ethanol and dried in an oven (Fig. 1).

3. Results and discussion

3.1. Characterization of $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2\text{-Asn}$

Characterization of the fabricated $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2\text{-Asn}$ was performed by several physicochemical methods such as FESEM, TEM, FT-IR, XRD, and VSM.

FESEM image of the prepared $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2\text{-Asn}$ MNPs is demonstrated in Fig. 2. As can be seen from

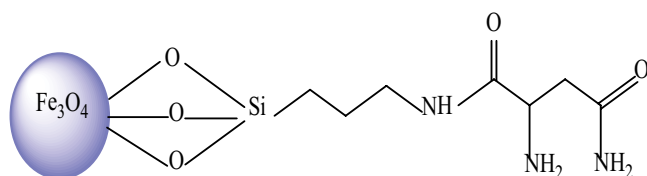


Fig. 1. Schematic structure of $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2\text{-Asn}$ MNPs.

Fig. 2, the synthesized MNPs have good morphology with dimensions between 21 and 66 nm.

The size and shape of the resulting adsorbent were further studied by TEM (Fig. 3). As can be observed, the synthesized MNPs have good core-shell structures and were composed of aggregated spherical particles with sizes below 30 nm. Furthermore, numerous nanoparticles are encapsulated in the SiO_2 .

The FT-IR spectra of the Fe_3O_4 , $\text{Fe}_3\text{O}_4@ \text{SiO}_2$, $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2$, asparagine, and $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2\text{-Asn}$ are displayed in Fig. 4. The band at 554 cm^{-1} corresponds to the stretching vibration of the Fe–O bond of Fe_3O_4 . In addition, the peaks at $1,631$ and $3,354 \text{ cm}^{-1}$ are attributed to the stretching vibration of the hydroxyl (–OH) groups on the surface of the Fe_3O_4 nanoparticles (Fig. 4a). Furthermore, Fig. 4b attributed to $\text{Fe}_3\text{O}_4@ \text{SiO}_2$, the band that appeared at $1,070 \text{ cm}^{-1}$ is corresponding to Fe–O–Si. Fig. 4c shows characteristic bands of both Fe_3O_4 and amino groups in $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2$. The bands at $2,804$ and $1,582 \text{ cm}^{-1}$ can be ascribed to the NH bending. In the spectrum of Asparagine

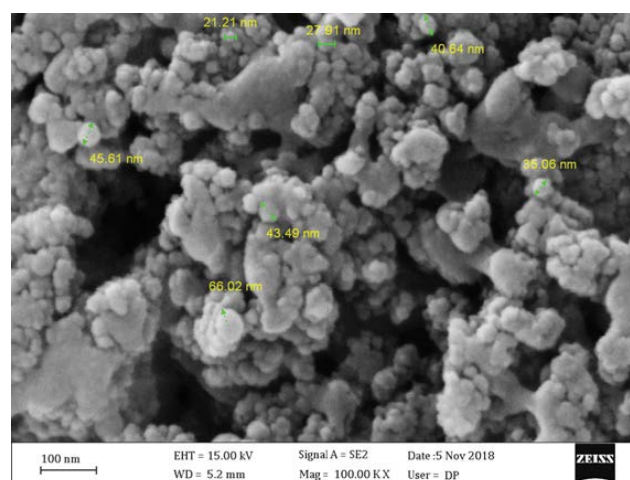


Fig. 2. FESEM image of synthesized $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2\text{-Asn}$ MNPs.

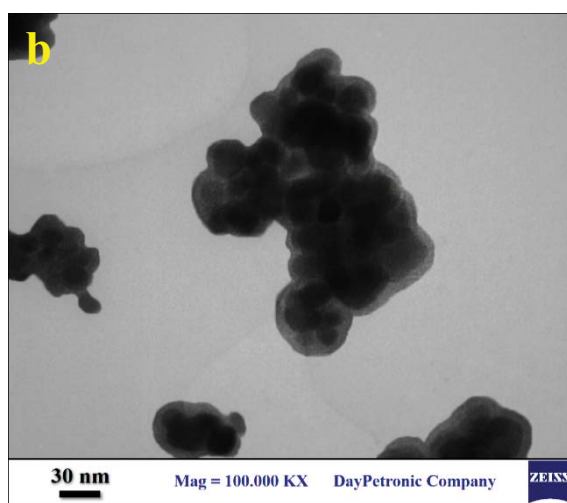
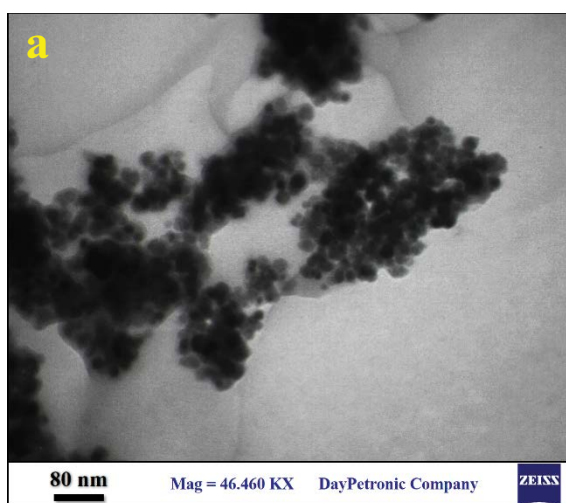


Fig. 3. TEM micrograph of $\text{Fe}_3\text{O}_4@ \text{SiO}_2\text{-NH}_2\text{-Asn}$ at different magnifications (a and b).

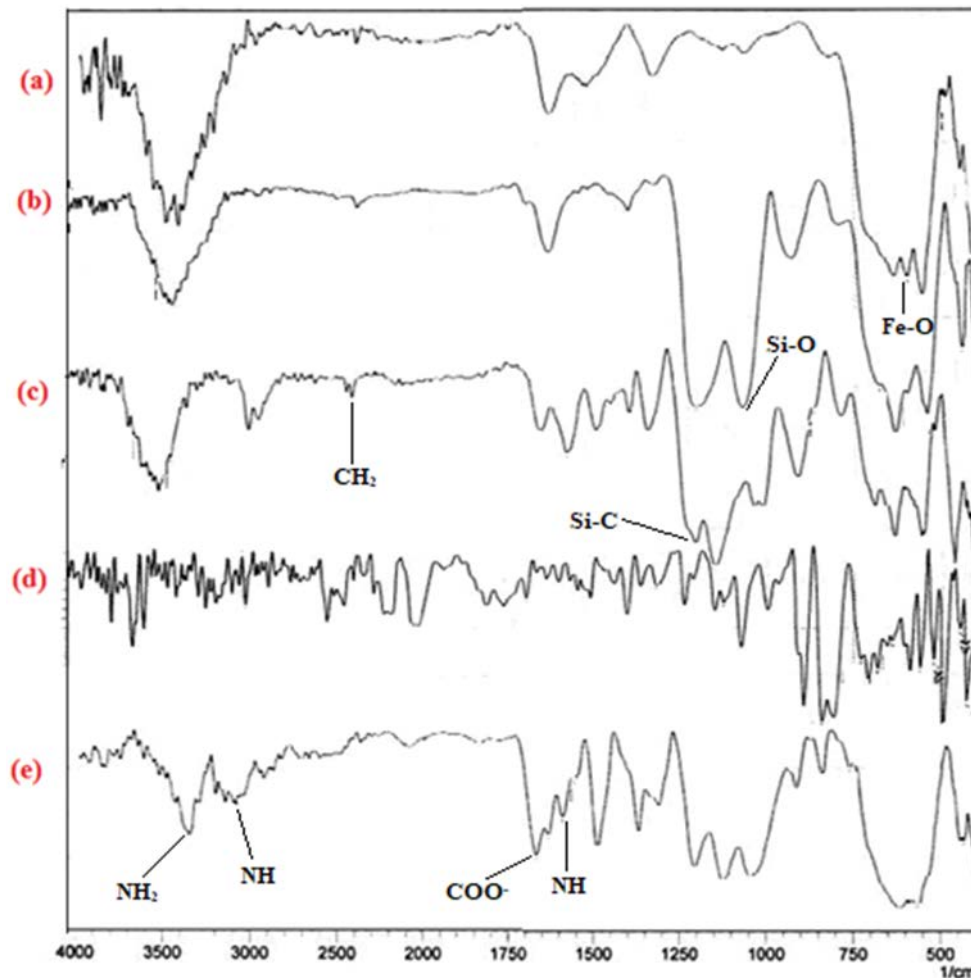


Fig. 4. FT-IR spectra of (a) Fe_3O_4 , (b) $\text{Fe}_3\text{O}_4@SiO_2$, (c) $\text{Fe}_3\text{O}_4@SiO_2-NH_2$, (d) Asparagine, and (e) $\text{Fe}_3\text{O}_4@SiO_2-NH_2-Asn$ MNPs.

(Fig. 4d), the bands that emerged at $3,207\text{ cm}^{-1}$ are ascribed to the NH stretching vibration of the amino group. The bands at $1,751$ and $1,502\text{ cm}^{-1}$ belong to the symmetric and asymmetric stretching vibrations of COO^- . The strong absorption band at 580 cm^{-1} is corresponding to the Fe–O bond stretching vibration of Fe_3O_4 , which confirms the existence of asparagine on the Fe_3O_4 surface.

X-ray diffraction (XRD) pattern of synthesized $\text{Fe}_3\text{O}_4@SiO_2-NH_2-Asn$ MNPs is demonstrated in Fig. 5. As illustrated in Fig. 5, the six characteristic dominant XRD peaks are located at $2\theta = 30.29^\circ, 35.67^\circ, 37.50^\circ, 43.35^\circ, 53.74^\circ, 57.29^\circ, 62.92^\circ,$ and 74.63° which can be relevant to (220), (222), (300), (400), (422), (511), (440), and (622) planes of Fe_3O_4 , respectively (JCPDS No. 19-692). These peaks are well-defined and confirm the well-crystallized structure of Fe_3O_4 with a typical cubic spinel phase. This result corroborated the existence of magnetite core in the structure of prepared MNPs.

The vibrating sample magnetometer (VSM) curve of the $\text{Fe}_3\text{O}_4@SiO_2-NH_2-Asn$ MNPs is demonstrated in Fig. 6. VSM measurement was carried out by taking the solid sample on the tips of the vibrating rod and analyzing it at r.t in an applied magnetic field sweeping from -20 to 20 kOe . The saturated magnetization value of

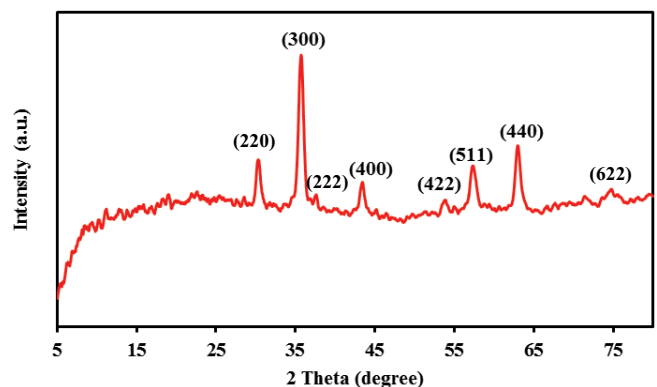


Fig. 5. XRD diffraction pattern of synthesized $\text{Fe}_3\text{O}_4@SiO_2-NH_2-Asn$ MNPs.

$\text{Fe}_3\text{O}_4@SiO_2-NH_2-Asn$ MNPs was 47.1 emu g^{-1} which indicates the synthesized $\text{Fe}_3\text{O}_4@SiO_2-NH_2-Asn$ MNPs have a proper magnetic response to the magnetic fields.

To study the surface charge of synthesized MNPs which can affect their physical stability in solution, zeta-potential as an indirect measuring the net charge on the surface of NPs was measured utilizing a particle

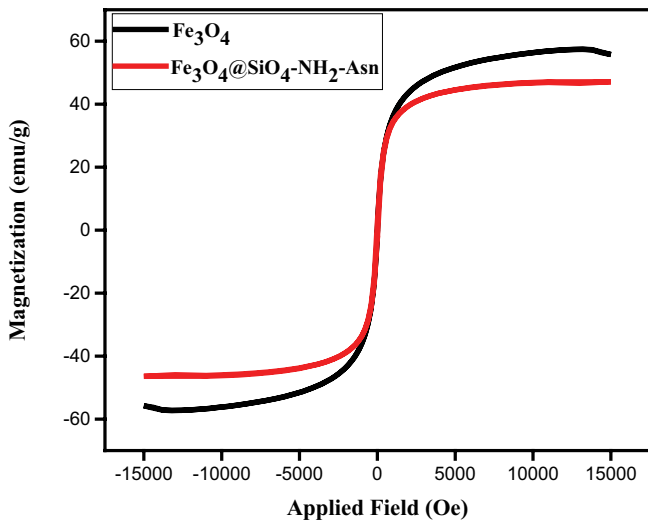


Fig. 6. VSM of pure Fe_3O_4 and $\text{Fe}_3\text{O}_4@SiO_2-NH_2-Asn$ MNPs.

Charge Reader. Its value is utilized as a dispersion stability index and can be utilized to specify the particles' tendency to aggregate in the aqueous medium. In the present research, the zeta potential and mobility were measured as 31.1 mv and $2.44 \mu\text{m cm Vs}^{-1}$, respectively at 298 K with a count rate of 172.4 kcps (Fig. 7). The large zeta potential obtained in this study predicts a more stable dispersion of synthesized MNPs and shows the positive charge of the surface of MNPs that makes it suitable for electrostatic interaction with anionic dye.

3.2. Carmoisine adsorption optimization

All the batch mode tests were performed by agitating a certain quantity of adsorbent in 50 mL of dye solution of favored concentration, contact time, pH, and ionic strength in a beaker. The pH effect on the adsorption of Carmoisine dye was assessed on the pH range of 1–6. The pH was adjusted utilizing 0.1 mol L^{-1} HCl or NaOH solutions. The effect of adsorbent mass on the elimination of Carmoisine was analyzed in the range of 0.02–0.11 g per 50 mL dye (40 mg L^{-1}) at pH 7 for 50 min. Batch equilibrium adsorption experiments were conducted by contacting 50 mL of 40 mg L^{-1} Carmoisine solution with 0.11 g of the adsorbent for 20 min at r.t and pH 6. The samples were agitated and

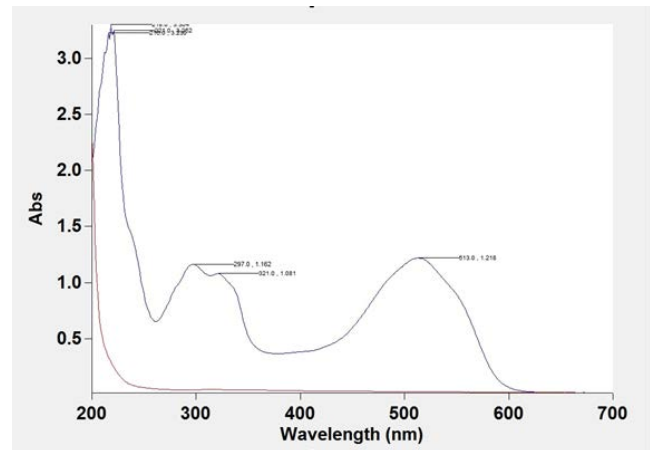


Fig. 8. UV-vis spectra of Carmoisine before and after removal by $\text{Fe}_3\text{O}_4@SiO_2-NH_2-Asn$ MNPs.

withdrawn from the beaker at pre-determined time intervals. The adsorbent was separated from the solution of dye by a magnet. The concentration of the supernatant was measured utilizing a UV-vis spectrophotometer as given in section 2.3 (Preparation of $\text{Fe}_3\text{O}_4@SiO_2-NH_2-Asn$ MNPs). According to obtained results, 513 nm was selected as the best wavelength for quantitative measurements (Fig. 8). The removal percentage of the Carmoisine in solution was calculated utilizing the following equation:

$$\% \text{Removal efficiency} = \frac{C_0 - C_t}{C_0} \times 100 \quad (1)$$

where C_0 and C_t are initial and equilibrium concentrations of Carmoisine after treatment with adsorbent, respectively.

3.3. Taguchi method for Carmoisine adsorption optimization

To obtain better removal efficiency of Carmoisine from aqueous solutions, the experimental conditions were optimized using orthogonal Taguchi array design to achieve the optimum experimental parameters with a minimum number of experiments. For this purpose, different conditions affecting the adsorption process such as adsorbent weight (0.02, 0.05, 0.08, and 0.11 g), contact time (5, 10, 15, and 20 min), ionic strength (0, 0.01, 0.05, and 0.2 mol L^{-1})

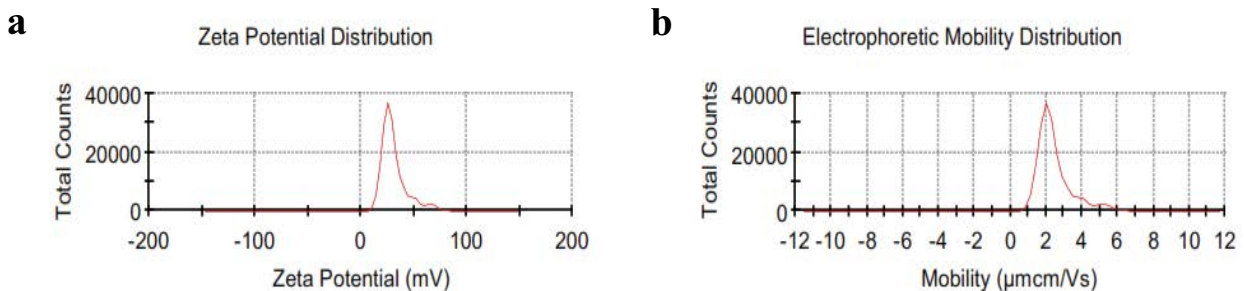


Fig. 7. Zeta potential distribution (a), and electrophoretic mobility distribution (b) of MNPs.

and solution pH (3, 4, 5, and 6) were investigated at four levels at constant volume of 50 mL and 40 mg L⁻¹ Carmoisine concentration (Table 1).

One of the crucial parameters in the adsorption procedure is the primary pH value of the solution which needs to be optimized to achieve desirable adsorption efficiency. In the present research, the effect of pH on Carmoisine dye adsorption efficiencies was examined in the pH range of 1–6. Optimization experiments were performed in accordance with the following procedure. First, the pH of the Carmoisine dye solution (40 mg L⁻¹) was adjusted and the absorbance was recorded by spectrophotometer. Next, a certain amount of Fe₃O₄@SiO₂-NH₂-Asn adsorbent was added to the solution and stirred for a while on a magnetic stirrer. After that, the container containing the solution was placed on a super magnet to separate and remove the adsorbent from the solution. The separated solution was transferred to the quartz cell and its absorbance was recorded by a spectrophotometer at 513 nm (Fig. 8). In accordance with the results, the Carmoisine dye sorption by Fe₃O₄@SiO₂-NH₂-Asn was more effective at a pH range of 2–6. However, by enhancing the solution pH, the elimination efficiency was reduced. Greater Carmoisine removal under an acidic medium can be owing to the protonation of the surface of the adsorbent and electrostatic interactions between the anionic dye molecules and adsorbent that facilitates the diffusion process.

The adsorbent amount is one of the crucial factors in the adsorption process. To investigate this factor, the adsorbent amounts of 0.02 (0.4 g L⁻¹), 0.05 (1.0 g L⁻¹), 0.08 (1.6 g L⁻¹), and 0.11 g (2.2 g L⁻¹) were considered (Fig. 9). According to the results, the optimum adsorbent weight was obtained to be 0.08 g (1.6 g L⁻¹). Because there are more available active sites for Carmoisine adsorption, the removal efficiency increases by increasing in an adsorbent amount from 0.4 to 1.6 g L⁻¹. The dye removal efficiency

was decreased in higher adsorbent amounts (2.2 g L⁻¹). This can be caused by the high adsorbent concentration for this purpose and excess particle interactions, like aggregation, that would result in a reduction in the total surface area of the adsorbent [31].

The influence of contact time of Fe₃O₄@SiO₂-NH₂-Asn MNPs on Carmoisine removal efficiency was examined in the range of 5, 10, 15, and 20 min (Fig. 9). It was seen that the removal efficiency of Carmoisine was enhanced at 20 min. In fact, with increasing contact time there are more opportunities for Carmoisine ions to contact with the adsorbent surface.

To investigate the ionic strength effect on the removal of Carmoisine using Fe₃O₄@SiO₂-NH₂-Asn MNPs, NaCl was

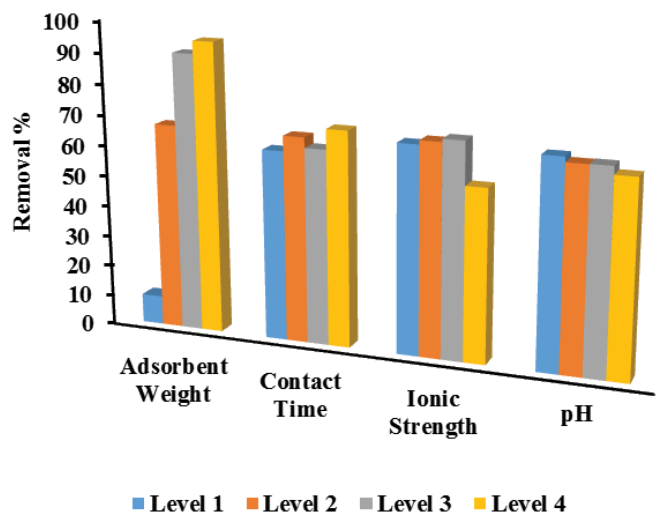


Fig. 9. Influence of adsorbent weight, contact time, ionic strength, and pH on Carmoisine removal percentage.

Table 1
Design of experiments by OA16 matrix for Carmoisine

Run	Adsorbent amount (g)	pH	Contact time (min)	Ionic strength (mol L ⁻¹)	Removal (%)
1	0.02	3	5	0	3.8
2	0.05	3	10	0.01	78.3
3	0.08	3	15	0.05	95.78
4	0.11	3	20	0.2	90.8
5	0.02	4	15	0.01	10.5
6	0.05	4	20	0	74.8
7	0.08	4	5	0.2	2.45
8	0.11	4	10	0.05	94.5
9	0.02	5	20	0.05	23.3
10	0.05	5	15	0.2	49.9
11	0.08	5	10	0	93.5
12	0.11	5	5	0.01	95.8
13	0.02	6	10	0.2	0
14	0.05	6	5	0.05	65
15	0.08	6	20	0.01	89.8
16	0.11	6	15	0	97

added to the solution at concentrations of 0, 0.01, 0.05, and 0.2 mol L⁻¹. As displayed in Fig. 9, the optimum amount of ionic strength was 0.05 mol L⁻¹. The results revealed that with the increase in ionic strength from 0 to 0.05 mol L⁻¹, the removal efficiency of adsorbent is increased which may be because of reduced solubility of the Carmoisine dye in water and improvement of the interaction between the dye and the Fe₃O₄@SiO₂-NH₂-Asn MNPs in the ionic medium [24]. In higher ionic strength (0.2 mol L⁻¹), salt addition had a negative effect on the removal efficiency. This corresponded to Carmoisine dye molecules and salt ions competition for the sorption on the surface of Fe₃O₄@SiO₂-NH₂-Asn.

Carmoisine has sulfonic acid functional groups. In solution, it produces protons and negative ions. Also at acidic pHs, NH₂ groups of Fe₃O₄@SiO₂-NH₂-Asn MNPs are protonated to form NH₃⁺. In this study, acidic pHs of 3, 4, 5, and 6 were selected to optimize the effect of solution pH. As revealed in Fig. 9, the maximum adsorption capacity of Carmoisine is recorded at pH = 3. At this pH, the anionic Carmoisine is electrostatically adsorbed to the surface of Fe₃O₄@SiO₂-NH₂-Asn MNPs.

To explore the repeatability of the removal process under optimal conditions (pH = 3, adsorbent weight = 0.08 g, ionic strength = 0.05 mol L⁻¹, and contact time = 20 min),

this pattern was repeated three times and the mean removal efficiency was acquired about 96.6% ± 0.08%.

3.4. Adsorption isotherms

Adsorption isotherms, which illustrate the correlation between the equilibrium concentration of the adsorbate in the solution and on the adsorbent surface at a constant temperature, are usually employed to describe the adsorption process.

Here, to determine the adsorption isotherms, Temkin, Langmuir, and Freundlich adsorption isotherm models, were investigated (Fig. 10). Optimum conditions were obtained at different Carmoisine concentrations of 1, 5, 10, 25, 40, 75, 100, and 250 mg L⁻¹ at room temperature. Then, the absorbance of the residual solution was recorded at each concentration by UV-vis spectrophotometer.

Langmuir equations can be expressed as Eq. (2):

$$\frac{C_e}{q_e} = \frac{C_e}{q_{\max}} + \frac{1}{Kq_{\max}} \quad (2)$$

where q_e and C_e respectively, refer to the mass of Carmoisine adsorbed onto the adsorbent in mg g⁻¹, and the equilibrium concentration of Carmoisine in mg L⁻¹, K , and q_{\max}

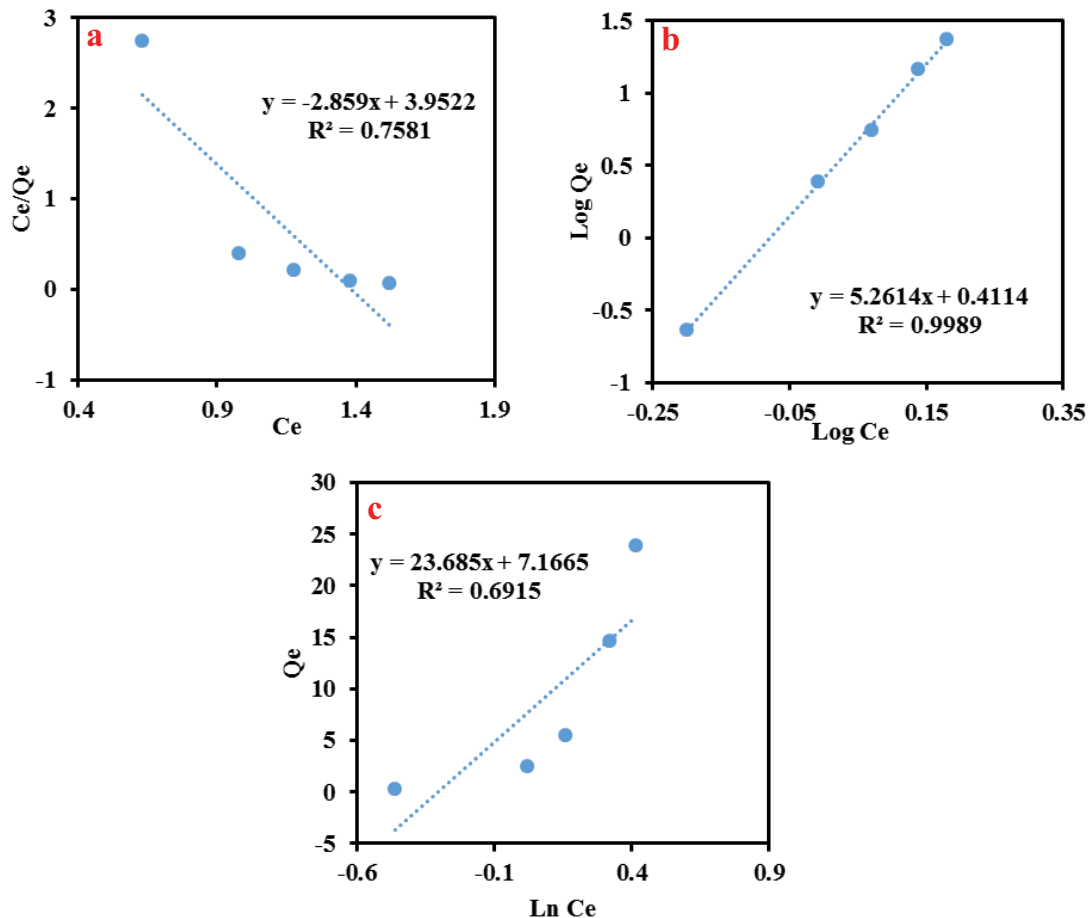


Fig. 10. (a) Langmuir, (b) Freundlich, and (c) Temkin adsorption isotherm plots for the removal of Carmoisine (pH = 3; adsorbent dose = 0.08 g; contact time = 20 min; ionic strength = 0.05 mol L⁻¹).

are, respectively, the adsorption equilibrium constant in terms of L mg^{-1} , and the maximum adsorption capacity in terms of mg g^{-1} .

As shown in Fig. 10a, adsorption data does not match with the Langmuir isotherm ($R^2 = 0.7581$).

Freundlich isotherm is commonly represented by Eq. (3):

$$\log q_e = \log K_F + \frac{1}{n_F} \log C_e \quad (3)$$

where q_e is the value of adsorbed Carmoisine at equilibrium (mg g^{-1}); K_F and n are, respectively, the Freundlich constants showing the adsorption capacity and the adsorption intensity, and also C_e is an aqueous concentration of adsorbate at equilibrium (mg L^{-1}).

Temkin isotherm [32] is described by the following equation:

$$q_e = K_1 \ln(K_2) + K_1 \ln(C_e) \quad (4)$$

where K_2 and K_1 are, respectively, the dimensionless Temkin isotherm constant, and related to the heat of adsorption (L g^{-1}) (Fig. 10c). Based on the correlation coefficient of this model ($R^2 = 0.6915$), the removal of Carmoisine ions was not matched by this model.

The investigation of the adsorption isotherms, Langmuir, Freundlich, and Temkin models was demonstrated in Fig. 10, and the determined values for the three model's parameters are presented in Table 2. The outcomes revealed that the experimental data for Carmoisine adsorption onto the $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-NH}_2\text{-Asn}$ is fitted with the Freundlich isotherm model with R^2 values of 0.9989 which is better compared to the obtained values by the Langmuir and Temkin isotherm models. In the current research, the outcomes of fitting experimental data demonstrate which the adsorption of the Carmoisine is carried out by the sites of the adsorbent which are heterogeneous, signifying non-uniform, and multi-layer adsorption.

3.5. Kinetic study

To investigate the kinetics of Carmoisine dye removal by synthetic $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-NH}_2\text{-Asn}$ MNPs, designed experiments were accomplished under optimum conditions at 40 mg L^{-1} of dye in 0–90 min (Fig. 11).

In this research, various models including Lagergren's pseudo-first-order, pseudo-second-order, intra-particle, and Elovich kinetic models were investigated (Figs. 12a–d). Kinetic studies were performed at optimal conditions and the solutions were stirred in time intervals ranged from 0 to 90 min. In different studied kinetic models, as shown in Fig. 12b, the best model was chosen based on the linear

regression correlation coefficient (R^2 values). Regarding the high regression coefficient of the pseudo-second-order kinetic model ($R^2 = 0.999$), the kinetic of the Carmoisine adsorption process is best described by this model (Table 3). It demonstrates that chemisorption occurs during the adsorption of the Carmoisine on the surface of $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-NH}_2\text{-Asn}$ MNPs.

In accordance with the calculated results, the maximum adsorption capacity of the $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-NH}_2\text{-Asn}$ was estimated to be 24.1 mg g^{-1} .

3.6. Applicability of adsorbents for removal of Carmoisine from real samples

To explore the reliability and applicability of the synthesized $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-NH}_2\text{-Asn}$ MNPs for dye removal in aqueous solutions, five aqueous samples with various matrixes including river water (Zarjoob River, Rasht, Iran), seawater (Caspian Sea, Ghazian, Iran), tap water (Rasht, Guilan, Iran), lagoon water (Anzali, Iran), and sand wastewater (Rasht, Iran) were collected from Guilan Province in Iran. To study the matrix impact of each sample on the removal efficiency of dye, the samples were spiked by Carmoisine individually, in such a way the final concentration of Carmoisine was fixed at 40 mg L^{-1} . The spiked samples were acted in the proposed removal process under optimized conditions (adsorbent weight = 0.08 g , $\text{pH} = 3$, ionic strength = 0.05 mol L^{-1} , and time = 20 min). Results showed good removal efficiency of Carmoisine in tap water (95%), seawater (74%), lagoon water (99%), Zarjoob river water (90%), and sand wastewater (74%) and confirming the potential of the synthesized MNPs for removal of Carmoisine dye from real water samples.

3.7. Reusability of $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-NH}_2\text{-Asn}$ MNPs

To investigate the reusability ability of $\text{Fe}_3\text{O}_4@\text{SiO}_2\text{-NH}_2\text{-Asn}$ MNPs, different repetitive Carmoisine adsorption tests

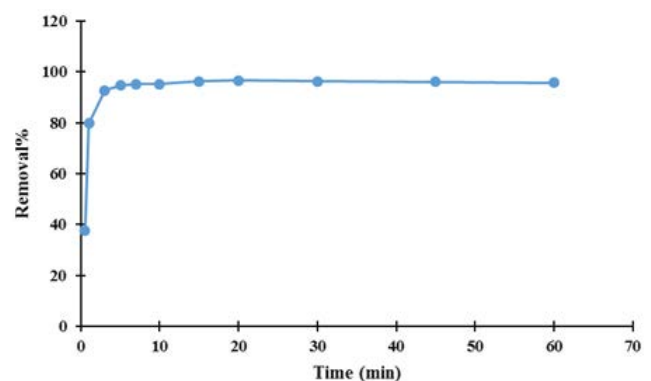


Fig. 11. Carmoisine removal percentage.

Table 2
Adsorption isotherms for adsorptive removal of Carmoisine

Temkin			Freundlich			Langmuir		
R^2	K_2	K_1	R^2	n	K_F	R^2	q_m	K
0.6915	1.34	23.68	0.9989	0.19	2.57	0.7581	-0.34	-0.72

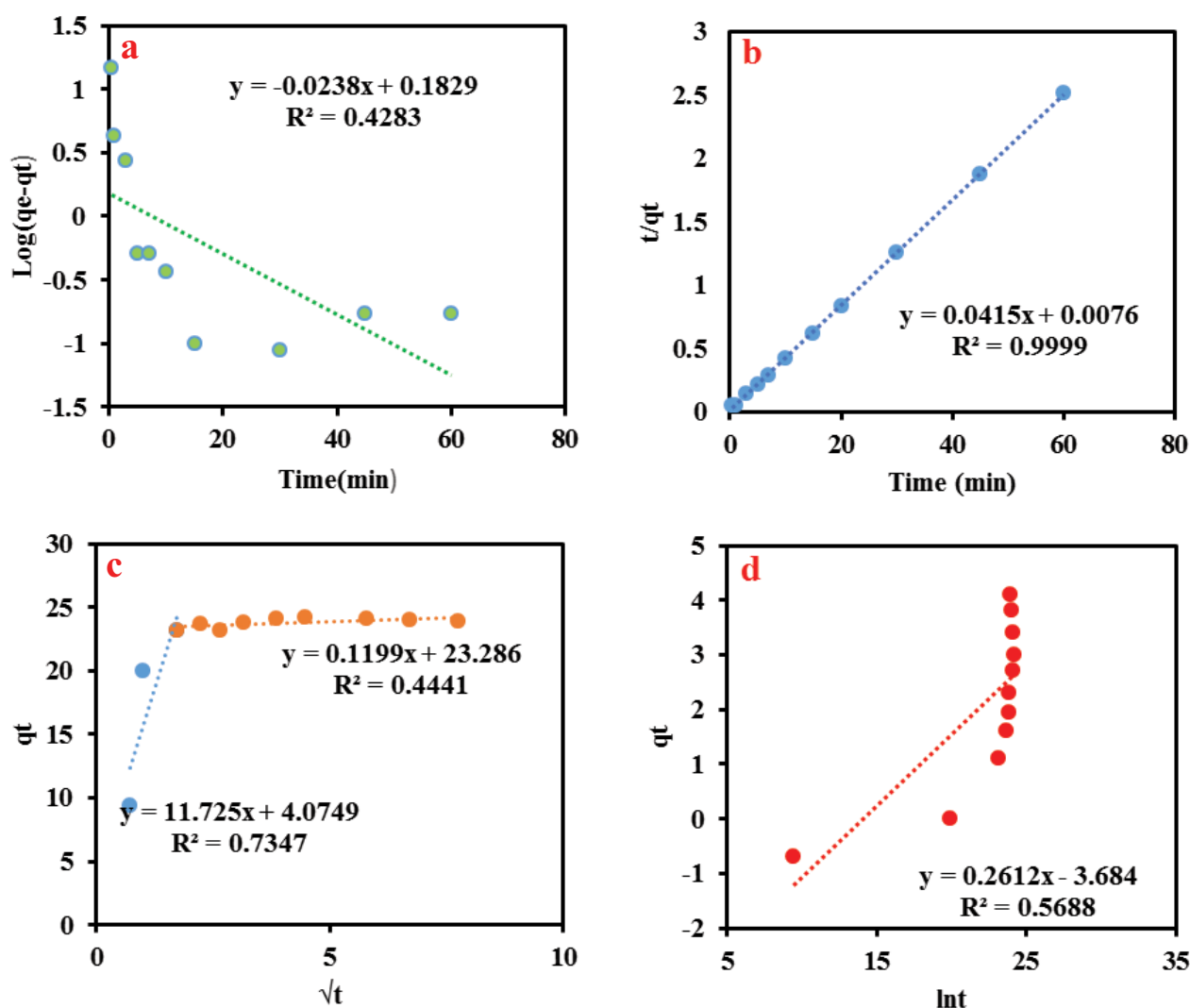


Fig. 12. (a) Pseudo-first-order, (b) pseudo-second-order, (c) intra particle, and (d) Elovich kinetic models.

Table 3
Kinetic study for adsorptive removal of Carmoisine

Elovich		Intra particle kinetic			Pseudo-second-order			Pseudo-first-order			
R^2	α	β	R^2	C	K_{ip}	R^2	q_e	K_2	R^2	q_e	K_1
0.5688	3×10^{-6}	3.8	0.4441	23.286	0.1199	0.9999	24.1	0.22	0.4283	1.19	0.023
			0.7347	4.079	11.725						

were performed at optimum conditions utilizing the same adsorbent. Dye desorption experiments were performed using NaOH (0.1 mol L⁻¹) for washing and removing the dye molecules from the adsorbent and finally drying the adsorbent to regenerate it at 100°C. After seven successive runs, the high magnetic sensitivity of recycled Fe₃O₄@SiO₂-NH₂-Asn MNPs still retained and the MNPs can be collected from the solution using a super magnet. As demonstrated in Fig. 13, after the seventh cycle, the adsorption efficiency for Carmoisine reduced from 96.6% to 79%.

The results show an efficacious regeneration of the Fe₃O₄@SiO₂-NH₂-Asn by NaOH (0.1 mol L⁻¹) solution and reuse with an insignificant decrease in its adsorption efficiency that can corroborate the economical of the adsorption process.

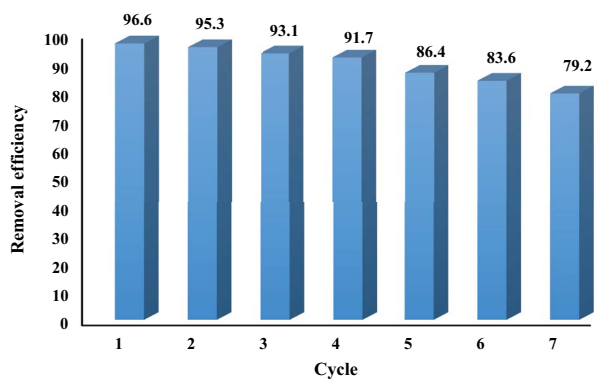
3.8. Comparison with other adsorbents

Carmoisine removal efficiency by Fe₃O₄@SiO₂-NH₂-Asn was compared with previously reported adsorbents, and

Table 4

Comparison of maximum adsorption capacity of Carmoisine in various adsorbents

Adsorbents	Dye	Kinetic model	Isothermic model	q_{\max} (mg g ⁻¹)	Ref.
Fe ₃ O ₄ @SiO ₂ -CMK-8 MNCs	Ponceau 4R	Pseudo-second order	Freundlich	78.74	[27]
Fe ₃ O ₄ @SiO ₂ @NH ₂	Methyl red	Pseudo-second-order	Langmuir	125	[33]
Methyl propylaminopropanoate-coated Fe ₃ O ₄ @SiO ₂ nanoparticles	Acid red 114	Pseudo-second-order	Langmuir	105	[34]
Fe ₃ O ₄ @SiO ₂ nanospheres	Congo red	Pseudo-second-order	Langmuir	50	[35]
Fe ₃ O ₄ @SiO ₂ -NH ₂ -Asn	Carmoisine	Pseudo-second-order	Freundlich	24.1	Present work

Fig. 13. Reusability of Fe₃O₄@SiO₂-NH₂-Asn for adsorption of the Carmoisine.

the results are demonstrated in Table 4. The results show that the Fe₃O₄@SiO₂-NH₂-Asn for Carmoisine removal was proper and exhibited satisfactory removal performance for Carmoisine.

4. Conclusions

This research revealed the application of Fe₃O₄@SiO₂-NH₂-Asn MNPs for the removal of the anionic Carmoisine dye from aqueous solutions. The highest removal efficiency for Carmoisine dye (~96.6%) was achieved at pH = 3, 0.08 g of Fe₃O₄@SiO₂-NH₂-Asn MNPs and 20 min. A study of kinetic models displayed that adsorption of Carmoisine is obeyed from pseudo-second-order kinetic model showing chemisorption. The Freundlich isotherm demonstrated the best interpretation of the results. Short adsorption time, separation with an external magnet, reusability, and easy operation are the main advantages of the synthesized adsorbent. Moreover, the detailed study of adsorption behavior on real samples confirmed that synthesized MNPs are beneficial in industrial applications for the removal of Carmoisine from wastewater.

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