

51 (2013) 3591–3596 April



Ti-salt flocculation for dissolved organic matter removal in seawater

Sanghyun Jeong, Yosef Okour, Tien Vinh Nguyen, Ho Kyong Shon, Saravanamuthu Vigneswaran*

Faculty of Engineering and IT, University of Technology, Sydney (UTS), PO Box 123, Broadway, NSW, 2007, Australia Tel. +61 2 9514 2614; Fax: +61 2 9514 2633; email: s.vigneswaran@uts.edu.au

101 2 3011 2011, 1ux. 101 2 3011 2030, chan. 5.01ghe5uurun@ul

Received 29 June 2012; Accepted 15 October 2012

ABSTRACT

In this study, the removal of different fractions of organic matter in seawater was investigated using titanium tetrachloride (TiCl₄) flocculation and compared with ferric chloride (FeCl₃) flocculation. The organic matter fractions were characterised using liquid chromatography–organic carbon detector (LC–OCD). Results showed the hydrophobic compounds removal was dominant by both flocculants. However, the removal of hydrophilic organic compounds, such as humics and low-molecular weight neutral compounds of seawater, was superior by TiCl₄ flocculation compared to FeCl₃ flocculation and this removal increased considerably with the increase of TiCl₄ doses. The flocculated sludge after TiCl₄ flocculation was incinerated to produce titanium dioxide (TiO₂) nanoparticle. TiO₂ from seawater sludge characterised by X-ray diffraction (XRD) and scanning electron microscope/energy-dispersive X-ray spectroscopy (SEM/EDS) showed predominant anatase phase with Si as a main dopant.

Keywords: Seawater; Flocculation; Titanium tetrachloride (TiCl₄); Ferric chloride (FeCl₃); Titanium dioxide (TiO₂) nanoparticle

1. Introduction

Natural organic matter (NOM) is one of the main foulants related to membrane processes that has a potential to form additional fouling by interaction between organic foulant itself or biomass [1,2]. This fouling is due to the adsorption onto the membrane surface or inside the pores. In addition, NOM can aggregate on the membrane surface and consequently form a sticky gel layer presenting high hydraulic resistance [3].

NOM usually have negatively functional groups such as carboxyl (–COOH) and phenolic groups (–OH) [4]. Pre-treatment methods such as Fe-salt and Ti-salt flocculation can remove a portion of NOM through three mechanisms namely charge neutralisation, electrostatic patch and bridging flocculation to reduce membrane fouling [5,6]. In general, flocculation preferentially removes the hydrophobic NOM fraction, whereas the neutral hydrophilic fraction is responsible for much of the irreversible fouling [7].

Coagulation–flocculation is a well-known pre-treatment method that can remove particles and colloids in water and wastewater treatment. The use of FeCl₃ as Fe-salt flocculant is considerably increased due to its high DOC removal efficiency with no detrimental effect to the living environment compared to aluminium (Al) salt [8]. However, the application of Ti-salt flocculant in water treatment, which was firstly investigated, by Upton and Buswell [9] has attracted a new

^{*}Corresponding author.

^{1944-3994/1944-3986 © 2013} Balaban Desalination Publications. All rights reserved.

attention in seawater treatment. Recently, Okour et al. [6] studied the application of Ti-salt flocculant as a pre-treatment for seawater reverse osmosis (SWRO). They reported that flocculation followed by granular activated carbon (GAC) filtration significantly reduced the turbidity, silt density index (SDI₁₅), dissolved organic carbon (DOC), colour and UV absorbance of flocculated seawater. In addition, TiCl₄ flocculation as a pre-treatment to SWRO was compared with FeCl₃ flocculation with respect to flocculation performance, membrane autopsy of fouled RO and sludge recovery after TiCl₄ flocculation. The authors found that the residual Ti salts did not cause any severe membrane fouling compared to Fe salts. Zhao et al. [10] investigated the flocculation mechanism by TiCl₄ and they stated that the flocculation was not only processed by charge neutralisation but also might be by a chemical bond. During flocculation, NOM might absorb by hydroxide solid at an optimum pH of 8.0. Floc size by TiCl₄ flocculant was larger than that of FeCl₃, polyferric sulphate (PES), Al₂(SO₄)₃ and polyaluminium chloride (PACl). TiCl₄ flocculation has an advantage in application over a wider range of high pH [11]. However, no efforts were made to study the organic matter removal in detail by Ti-salt flocculant.

A significant disadvantage of flocculation is the production of a large amount of sludge. The sludge requires an additional treatment and disposal in ocean and landfills. In recent years, due to serious oceanic contamination and damage of the fragile ecology of the coastal area, disposal of the waste into the ocean has been restricted. Shon et al. [12,13] developed a method to recover multi-functional titanium dioxide (TiO₂) nanoparticles from the TiCl₄ sludge. The prices of Tisalt coagulation are five times higher than those of Alsalt while the sludge recycling and TiO₂ production compensate for the high Ti-salt price and ultimately provide numerous benefits with revenue to promote a water treatment plant [14]. These benefits of adopting Ti-salt coagulation, sludge recycling and by-product production have been proven during the last six years of research studies. Titanium dioxide is used in a number of industries. It is used as white pigment, sunscreen, a thickener in cosmetic and skin-care products and particularly a photocatalyst under ultraviolet (UV) light. Lee et al. [15] evaluated aquatic toxicity of this TiO₂ nanoparticle produced from flocculated sludge of seawater in terms of LC50 and mortality of Daphnia magna and EC50 of Microtox[®] test. They found that TiCl₄ coagulant and TiO₂ produced from flocculated seawater sludge had very low toxicity in aqueous condition compared with Degussa TiO₂-P25.

Therefore, the advantages of Ti-salt coagulation are: (1) it is required at lower dosage; (2) it is active at low

water temperatures; (3) it facilitates short sedimentation time; (4) it has better removal of organic/inorganic materials; and (5) it generates a valuable by-product. In this study, the flocculation performance of TiCl₄ of organic matters in seawater was investigated in terms of NOM fractionations removal. NOM removal of TiCl₄ was also compared with that of commonly used FeCl₃ flocculant. Finally, TiO₂ recovered from flocculated sludge of seawater was characterised in terms of particle structure and atomic composition to evaluate its use.

2. Materials and methods

2.1. Seawater

Seawater conducted in this study was drawn from Chowder bay, Sydney, Australia. It was withdrawn from 1 m below the surface level of the sea and then filtered through the centrifuge to remove large particles. The range of turbidity, pH and dissolved organic carbon (DOC) values of the seawater during the study period was 0.41–0.42 NTU, 7.98–8.04 and 1.30–1.45 mg/L, respectively.

2.2. Flocculation test

TiCl₄ and FeCl₃were used as flocculants in this study. TiCl₄ was prepared as 10% stock solution and FeCl₃ was prepared as 1000 mg/L of stock solution using FeCl₃·6H₂O. The flocculation tests were carried out using standard jar test as indicated below. The seawater was placed in 1 L beakers and predetermined concentrations of titanium (Ti⁴⁺) and ferric (Fe³⁺) of 1.3–6.3 mg/L and 1.0–5.0 mg/L were added, respectively. The samples were then stirred rapidly for 2 min at 120 rpm, followed by 20 min of slow mixing at 30 rpm and 30 min of settling. The supernatant was filtered through 0.45 µm microfilter and the filtrate was used for further dissolved organic carbon (DOC) analysis.

2.3. Organic fractionation

Total DOC and detailed organic fractions were measured (two replicates) using a liquid chromatographyorganic carbon detector (LC–OCD) Model 8 (DOC-Labor, Karlsruhe, Germany), which is an automated size-exclusion chromatography coupled to three detectors, organic carbon (OCD), organic nitrogen (OND) and UV-absorbance (UVD). The measurement procedure has been described in detail elsewhere [20]. In this study, a Toyopearl TSK HW50S column (TOSOH Bioscience GmbH, Stuttgart, Germany) was utilized with phosphate buffer as mobile phase of pH 6.4 (2.6 g L^{-1} KH₂PO₄ and 1.5 m L^{-1} Na₂HPO₄) at a flow rate of 1.1 mLmin^{-1} . Injection volumes and retention time were $1000 \,\mu\text{L}$ and $120 \,\text{min}$, respectively. The chromatographic column was a weak cation exchange column on polymethacrylate basis. In this paper, mean values (from two replicates) of DOC data were used and standard variation was less than 5%.

2.4. TiO_2 recovery

The flocculated sludge of TiCl₄ was collected, filtered and dried in the oven at 100 °C for three days to remove the water content. Then it was grinded and placed in a furnace at 600 °C for 24 h. After incineration, the colour was changed from black to white indicating the formation of TiO₂.

2.5. TiO₂ characterisation

To identify TiO_2 particle structure, X-ray diffraction (XRD) was investigated using MDI Jade 5.0 (Materials Data Inc., USA). The aggregated particle image and composition of TiO_2 were observed using scanning electron microscopy (SEM, Rigaku, Japan).

3. Results and discussion

3.1. Organic matter removal

In this study, $TiCl_4$ was used as Ti-salt flocculant and its performance was compared with that of $FeCl_3$. Table 1 presents the DOC of flocculated effluent after $TiCl_4$ and $FeCl_3$ flocculation.

Table 1 The removal of DOC after flocculation with TiCl₄ and FeCl₃ Organic matter was divided into two parts by LC– OCD. Hydrophobic organic carbon (HOC) was calculated as a difference of dissolved organic carbon (DOC) with chromatographic DOC (CDOC). All organic matter retained in the column was defined as hydrophobic. This could be either dissolved hydrocarbons or microparticulate including humics. CDOC is calculated from the area enclosed by the total chromatogram (Fig. 1).

Although the seawater samples were taken from the same sampling site, they were collected at different times for TiCl₄ and FeCl₃ flocculation tests. This is the reason why the seawater used in flocculation with TiCl₄ had more hydrophobic matters (40.7%) than that with FeCl₃ (25.4%).

The results showed that the DOC removal efficiency increased with the increase in flocculant doses. Hydrophobic compound removal was significant by both flocculants. The removal efficiency of hydrophobic compounds by FeCl₃ flocculation was much higher than that of hydrophilic compounds. Most hydrophobic compounds (94%) and a part of hydrophilic compounds (49%) were removed at ferric (Fe³⁺) dosage of 5.0 mg/L.

In case of TiCl₄, the difference in hydrophobic and hydrophilic compounds removal was only 12% at a dose of 5.0 mg of Ti⁴⁺/L. Interestingly, at all experimental concentrations, around 75% of hydrophobic compounds in seawater were removed by TiCl₄ flocculation. On the other hand, the removal of hydrophilic compounds was improved significantly as TiCl₄ concentration was increased from 1.3 to 5.0 mg/L.

	DOC (mg/L) ^a	Removal efficiency (%) ^b	HOC (mg/L) ^a Hydrophobic	Removal efficiency (%) ^b	CDOC (mg/L) ^a Hydrophilic	Removal efficiency (%) ^b
(a) TiCl	$_4$ (as mg of Ti ⁴	+/L)				
0.0 ^c	1.45	_	0.59	-	0.86	_
1.3	0.62	57.2	0.15	74.6	0.47	45.3
2.5	0.57	60.7	0.15	74.6	0.42	51.2
3.8	0.52	64.1	0.15	74.6	0.37	57.0
5.0	0.47	67.6	0.15	74.6	0.32	62.8
(b) FeCl	$_3$ (as mg of Fe ³	³⁺ /L)				
0.0 ^c	1.30	_	0.33	_	0.97	_
0.5	0.70	46.2	0.05	84.8	0.65	33.0
1.0	0.65	50.0	0.05	84.8	0.60	38.1
3.0	0.60	53.8	0.04	87.9	0.56	42.3
5.0	0.52	60.0	0.02	93.9	0.50	48.5

^aConcentrations of the different organic fractions in seawater.

^bRemoval efficiencies of different organic fractions in seawater after the pre-treatment.

^cSeawater with no flocculant.

Similar results were obtained by Okour et al. [6]. They reported that biopolymers, fulvic acids and low-molecular weight compounds with molecular weight of 1200, 950 and less than 650 Dalton were removed by Ti-salt flocculant.

3.2. Detailed natural organic matter (NOM) fraction

Natural organic matter (NOM) in seawater mainly contains biopolymers (BP), humic substances (HS or humics), building blocks (BB) and low-molecular weight neutrals (LN). It was observed that $TiCl_4$ floc-culation led to a higher amount of CDOC removal than FeCl₃ (Table 2).

3.2.1. Biopolymers (BP)

BP have very high molecular weight (20,000-100,000 g/mol) and it represent compounds such as polysaccharides, amino sugars, polypeptides, proteins, "extracellular polymeric substances", hydrophilic fraction and not UV-absorbing. In surface water, BP exist as colloidal transparent exopolymer particles (TEP) and polysaccharide. These fractions were identified as possible fouling active substances [16–18]. BP decreased significantly after flocculation with both flocculants (Fig. 1 and Table 2). The comparison of LC–OCD chromatograms shows that TiCl₄ flocculation retained more organic biopolymers than the FeCl₃ flocculation. BP removal efficiency increased as TiCl₄ doses increased with complete removal occurring at a dose of 5.0 mg of Ti^{4+}/L .

3.2.2. Humic substances (HS)

Humic substances (HS) represent compounds with molecular weights approximately 1000 g/mol. Zazouli et al. [19] reported that the flux reduction on NF membrane increased with increasing humics concentration in foulants. As can be seen from Fig. 1 and Table 2, HS removal was marginal by flocculation with FeCl₃ (20.6–26.5%). On the other hand, as TiCl₄ dose increased from 1.3 to 5.0 mg/L, the HS was removed remarkably from 40.9% to 63.6%.

3.2.3. Building blocks (BB)

Building blocks (BB) are defined as HS-hydrolysates, sub-units of HS with molecular weights between 300 and 450 g/mol. There are mainly weathering and oxidation products of HS. According to Huber et al. [20], BB cannot be removed by typical flocculation processes. Flocculants or coagulants as well as flocculated



Fig. 1. LC–OCD chromatogram of seawater and pre-treated seawater using $TiCl_4$ and $FeCl_3$.

particles sometimes should be considered as another factor in the formation of BB. In the same manner, in our study also BB did not show high removal (Table 2). BB removal slightly decreased with the increase of flocculant doses. Removal efficiencies of BB by FeCl₃ and TiCl₄ flocculants at a dose of 5.0 mg of Ti⁴⁺/L were below 38.1% and 44.4%, respectively.

3.2.4. Low-molecular weight neutrals (LMW neutrals or LN)

Low-molecular weight neutrals (LMW Neutrals; LN) are the only low-molecular weight weakly charged hydrophilic or slightly hydrophobic "amphiphilic" compounds such as alcohols, aldehydes, ketones and amino acids. Dittmar and Kattner [21] stated that LMW neutrals could be described as amphiphilic dissolved organic matter (DOM) recalcitrant to biodegradation such as metabolic intermedi-

	FeCl ₃ (r	ng of Fe ³⁺ /l	L)		$TiCl_4$ (mg of Ti^{4+}/L)					
	0.0 ^a	0.5	1.0	3.0	5.0	0.0 ^a	1.3	2.5	3.8	5.0
BP	0.14	0.08	0.07	0.05	0.04	0.09	0.06	0.04	0.01	0.00
HS	0.34	0.27	0.27	0.26	0.25	0.44	0.26	0.24	0.21	0.16
BB	0.21	0.19	0.16	0.16	0.13	0.18	0.13	0.11	0.11	0.10
LN	0.28	0.11	0.10	0.09	0.08	0.15	0.01	0.01	0.01	0.01

Table 2 Amount of different hydrophilic fractions of seawater removed by flocculants of different doses

^aSeawater with no flocculant.

ates and bacterial membranes moieties. Therefore, effective LN removal may reflect the reduction of microbial activity. Some researchers indicated that organic fouling is primarily caused by LN [2].

Both flocculation tests indicated high LN removal efficiencies, particularly with TiCl₄. Only trace of LN remained after TiCl₄ flocculation with removal efficiency reaching up to 93.0% (Table 2).

3.3. Sludge recovery

During coagulation processes, sludge disposal and treatment is the question pressing for serious environment considerations. In order to recover valuable TiO_2 nanoparticle from flocculated sludge, Ti-salt sludge was calcinated at 600 °C to remove organic matters.

XRD pattern of recovered TiO₂ particles is shown in Fig. 2. Recovered TiO₂ was found to have only anatase phase after calcination at 600 °C. Many researchers hydrothermally crystallised titanium dioxide gel and obtained anatase phase at temperature lower than 600 °C [22]. However, the incineration temperature of 600 °C was suggested in terms of energy consumption



Fig. 2. XRD pattern of the ${\rm TiO}_2$ recovered from ${\rm TiCl}_4$ flocculation.



Fig. 3. SEM image of the $\rm TiO_2$ recovered from $\rm TiCl_4$ flocculation.

and better photocatalytic activity of TiO₂ produced from Ti-flocculated sludge [11].

It was observed from SEM image of TiO_2 recovered from $TiCl_4$ flocculation that TiO_2 nanoparticles were doped with Si. Their atomic compositions of Ti, Si and O were 23.8%, 0.2% and 76.0%, respectively. In Fig. 3, violet small dots and light-blue background represented Si and Ti, respectively. Okour et al. [6] suggested that Si could be diminished through flocculation process and it was coated with TiO_2 .

4. Conclusion

The performance of Ti-salt flocculation of seawater was compared to that with Fe-salt flocculation in terms of detailed organic fractionation matter removal. The following are the finding of the experimental study.

- The removal of hydrophilic compounds of seawater by TiCl₄ flocculation was superior compared to FeCl₃ flocculation and this removal increased significantly as TiCl₄ doses increased.
- (2) Complete removal of biopolymers of NOM was achieved during TiCl₄ flocculation.
- (3) Higher humics removal of 63.6% was observed with TiCl₄ flocculation compared to only 26.5% with FeCl₃ flocculation.
- (4) Both flocculant showed low percentage removal for building blocks of NOM.
- (5) TiCl₄ flocculation indicated high LMW neutrals removal even at low doses. LMW neutral is one of the significant compounds causing organic fouling of membranes.
- (6) From XRD and SEM/EDX analyses, the recovered TiO₂ nanoparticles from TiCl₄ flocculated sludge were found to be Si-doped anatase structure.

Acknowledgements

This study was supported by the National Centre of Excellence in Desalination (membrane flocculation hybrid system as pre-treatment to brackish water reverse osmosis desalination system: Emphasis on chemical use reduction and recovery).

Abbreviations

-	building blocks
-	bio polymers
-	chromatographic dissolved
	organic carbon
-	dissolved organic carbon
-	hydrophobic organic carbon
-	humic substances
-	liquid chromatography-organic carbon
	detector
-	low-molecular weight neutrals
-	natural organic matter
	- - - - -

References

- M. Moonkhum, Y.G. Lee, Y.S. Lee, J.-H. Kim, Review of seawater natural organic matter fouling and reverse osmosis transport modelling for seawater reverse osmosis desalination, Desal. Water Treat. 15 (2010) 92–107.
- [2] S. Hong, M. Elimelech, Chemical and physical aspects of natural organic matter (NOM) fouling of nanofiltration membranes, J. Membr. Sci. 132 (1997) 159–181.
- [3] J. Kim, Z. Cai, M.M. Benjamin, NOM fouling mechanisms in a hybrid adsorption/membrane system, J. Membr. Sci. 349 (2010) 35–43.
- [4] A. Seidel, M. Elimelech, Coupling between chemical and physical interaction in natural organic matter (NOM) fouling of nanofiltration membranes: Implications for fouling control, J. Membr. Sci. 203 (2002) 245–255.

- [5] S. Jeong, T.V. Nguyen, S. Vigneswaran, Submerged membrane coagulation hybrid system as pre-treatment to organic matter removal from seawater, Water Sci. Technol. Water Supply 11(3) (2011) 352–357.
- [6] Y. Okour, I.E. Saliby, H.K. Shon, S. Vigneswaran, J.-H. Kim, J. Cho, I.S. Kim, Recovery of sludge produced from Ti-salt flocculation as pre-treatment to seawater reverse osmosis, Desalination 247 (2009) 53–63.
- [7] S. Lee, W.S. Ang, M. Elimelech, Fouling of reverse osmosis membranes by hydrophilic organic matter: Implication for water reuse, Desalination 187 (2006) 313–321.
- [8] N. Qureshi, R.H. Malmberg, Reuducing aluminium residuals in finished water, J. Am. Water Works Assoc. 77(10) (1985) 101–108.
- [9] W.V. Upton, A.M. Buswell, Titanium salts in water purification, Ind. Eng. Chem. 29(8) (1937) 870–871.
- [10] Y.X. Zhao, B.Y. Gao, B.C. Cao, Z.L. Yang, Q.Y. Yue, H.K. Shon, J.-H. Kim, Comparison of coagulation behaviour and floc characteristics of titanium tetrachloride (TiCl₄) and polyaluminum chloride (PACl) with surface water treatment, J. Chem. Eng. 166 (2011) 544–550.
- [11] Y.X. Zhao, B.Y. Gao, H.K. Shon, B.C. Cao, J.-H. Kim, Coagulation characteristics of titanium (Ti) salt coagulant compared with aluminium (Al) and iron (Fe) salts, J. Hazard. Mater. 185 (2011) 1536–1542.
- [12] H.K. Shon, S. Vigneswaran, I.S. Kim, J. Cho, G.J. Kim, J.-B. Kim, J.-H. Kim, Preparation of functional titanium oxide (TiO_2) from sludge produced by titaniumtetrachloride $(TiCl_4)$ flocculation of wastewater, Environ. Sci. Technol. 41(4) (2007) 1372–1377.
- [13] H.K. Shon, S. Vigneswaran, J. Kandasamy, M.H. Zareie, J.B. Kim, D.L. Cho, J.-H. Kim, Preparation and characterization of titanium dioxide (TiO₂) from sludge produced by TiCl₄ floc-culation with FeCl₃, Al₂(SO₄)₃ and Ca(OH)₂ coagulant aids in wastewater, Sep. Sci. Technol. 44 (2009) 1525–1543.
 [14] J.H. Kim, D.L. Cho, G.J. Kim, B. Gao, H.K. Shon, Titania
- [14] J.H. Kim, D.L. Cho, G.J. Kim, B. Gao, H.K. Shon, Titania nanomaterials produced from Ti-salt flocculated sludge in water treatment, Catal. Surv. Asia 15(7) (2011) 117–126.
- [15] B.C. Lee, S. Kim, H.K. Shon, S. Vigneswaran, S.D. Kim, J. Cho, I.S. Kim, K.H. Choi, J.B. Kim, H.J. Park, J.-H. Kim, Aquatic toxicity evaluation of TiO₂ nanoparticle produced from sludge of TiCl₄ flocculation of wastewater and seawater, J. Nanopart. Res. 11 (2009) 2087–2096.
- [16] L.O. Villacorte, M.D. Kennedy, G.L. Amy, J.C. Schippers, The fate of Transparent Exopolymer Particles (TEP) in integrated membrane systems: Removal through pre-treatment processes and deposition on reverse osmosis membranes, Water Res. 43 (2009) 5039–5052.
- [17] S. Rosenberger, C. Laabs, B. Lesjean, R. Gnirss, G. Amy, M. Jekel, J.-C. Schrotter, Impact of colloidal and soluble organic material on membrane performance in membrane bioreactors for municipal wastewater treatment, Water Res. 40 (2006) 710–720.
- [18] C. Laabs, G. Amy, M. Jekel, Understanding the size and character of fouling-causing substances from effluent organic matter (EfOM) in low-pressure membrane filtration, Environ. Sci. Technol. 40(14) (2006) 4495–4499.
- [19] M.A. Zazouli, S. Nasseri, M. Ulbricht, Fouling effects of humic and alginic acids in nanofiltration and influence of solution composition, Desalination 250 (2010) 688–692.
- [20] S.A. Huber, A. Balz, M. Abert, W. Pronk, Characterisation of aquatic humic and non-humic matter with size-exclusion chromatography-organic carbon detection-organic nitrogen detection (LC-OCD-OND), Water Res. 45 (2011) 879–885.
- [21] T. Dittmar, G. Kattner, The bio geochemistry of the river and shelf ecosystem of the Arctic Ocean: A review, Mar. Chem. 83 (2003) 103–120.
- [22] F. Dachille, P.Y. Simons, R. Roy, Pressure-temperature studies of anatase, brookite, rutile, and TiO₂(II), Am. Mineral. 53 (1968) 1929–1939.