

52 (2014) 178–183 January



# Kinetic and equilibrium studies of simultaneous adsorption of monochlorophenols and chlorophenoxy herbicides on activated carbon

Krzysztof Kuśmierek\*, Monika Sankowska, Andrzej Świątkowski

Institute of Chemistry, Military University of Technology, 00-908 Warsaw, Poland Tel. +48 22 683 95 61; Fax: +48 22 683 95 82; email: kkusmierek@wat.edu.pl

Received 14 December 2012; Accepted 21 February 2013

## ABSTRACT

Adsorption on activated carbon is one of the well-established and effective techniques for the removal of chloroorganic pollutants from surface water, groundwater, and drinking water. Since these water contaminants occur often together in the present study, kinetics and equilibria of simultaneous adsorption of selected chlorophenols and chlorophenoxy herbicides from aqueous solutions are investigated and described. For investigations, three monochlorophenols (2-chlorophenol, 3-chlorophenol, and 4-chlorophenol), as well as chlorophenoxy hebicides (2,4-dichlorophenoxyacetic acid and 2-methyl-4-chlorophenoxyacetic acid), are chosen. As adsorbent granular-activated carbon Filtrasorb 300 ( $938 \text{ m}^2/\text{g}$ ) was used. Adsorption quantities were determined by HPLC method. Kinetics of adsorption was described by pseudo-second-order model and adsorption equilibria by Freundlich equation. Proposed method can be used for adsorption from multicomponent aqueous solutions.

*Keywords:* Chlorophenols; Chlorophenoxy herbicides; Activated carbon; Adsorption kinetics; Adsorption equilibria

#### 1. Introduction

Halogenated organic contaminations of surface water, groundwater, and drinking water are a serious threat to living organisms. They include in particular chlorophenols and chlorophenoxy herbicides [1,2]. Among chlorophenols can be distinguished groups of isomers of equal number of chlorine atoms in the molecule, for example three monochlorophenols. They differ in the position of the chlorine atom in the aromatic ring: 2-chlorophenol, 3-chlorophenol, and 4-chlorophenol. In the published works, the adsorption of chlorophenols on activated carbon is rarely used for comparing two isomers [3–8] or even three [9,10] of one Cl atom in molecule. These studies were carried out separately for each adsorbate [11–16], mainly for 4-CP. In the case of chlorophenoxy herbicides, most commonly studied by adsorption is 2,4-D (two Cl atoms in the aromatic ring) [17–25]. In the few works is also MCPA used for comparison [26–30]. The difference between them lies in the replacement in the 2,4-D one chlorine atom in the 2-position by a –CH<sub>3</sub> group. Chlorophenols are formed as by-products often during the production of herbicides, and therefore both groups may be present very common in the environment (especially in surface water and groundwater) simultaneously. However, in the literature,

<sup>\*</sup>Corresponding author.

<sup>1944-3994/1944-3986 © 2013</sup> Balaban Desalination Publications. All rights reserved.

both chlorophenols and herbicides are examined separately. To the best of our knowledge, a direct comparison of the adsorption kinetic and equilibrium of chlorophenols and herbicides onto activated carbon has not been described.

The objective of the present study is to investigate and describe kinetics and equilibria of simultaneous adsorption of selected chlorophenols (2-, 3-, and 4chlorophenol) and chlorophenoxy herbicides (2,4-D and MCPA) on granular-activated carbon from aqueous solutions.

### 2. Materials and methods

#### 2.1. Chemicals and reagents

2-Chlorophenol, >99% (2-CP), 3-chlorophenol, 98% (3-CP), and 4-chlorophenol, >99% (4-CP) were from Sigma (St Louis, MO, USA). 2,4-Dichlorophenoxyacetic acid, >99% (2,4-D), 2-methyl-4-chlorophenoxyacetic acid, 99% (MCPA), and acetic acid were obtained from POCH (Gliwice, Poland). HPLC-grade acetoni-trile was from Acros Organics (Geel, Belgium).

#### 2.2. Adsorbent

The granular-activated carbon Filtrasorb 300 used in this study was purchased from Chemviron (Feluy, Belgium). Prior to use, the carbon was pretreated by washing in distilled water several times. Ash content decreased in that way from 8.05 to 7.85 wt.%. Finally, the activated carbon was dried in an oven at 120 °C for 6 h and stored in a desiccator until use. The main properties characterizing the prepared carbon are as follows: the BET surface area of the carbon = 938 m<sup>2</sup>/ g, iodine number = 927 mg/g, NaOH neutralization ability 0.07 mmol/g, and surface oxygen content from EDS—4.57 wt.% [12].

## 2.3. Adsorption procedure

The kinetic experiments were carried out with following procedure. A fixed amount of the activated carbons (0.2 g) and a 100 ml of the solutions containing a initial concentration of adsorbates  $C_0 = 100 \text{ mg/l}$ were placed in an Erlenmeyer flask, shaken at 25 °C, and theirs concentrations were analyzed after 1, 2, 3, 4, 5, 6, and 7 h. The amount of adsorption at time *t*, *q*<sub>t</sub> (mg/g), was calculated by equation:

$$q_t = V \frac{C_0 - C_t}{m} \tag{1}$$

where  $C_0$  and  $C_t$  are the initial concentration and adsorbate concentration at time *t* (mg/l), respectively,

m is the mass of the adsorbent (g), and V is the volume of the solution (l).

For the determination of adsorption isotherms, a fixed amount of the activated carbons (0.2 g) and a 100 ml of the solutions containing a known concentration of monochlorophenols and chlorophenoxy herbicides (ranged from 5 to 100 mg/l) were placed in an Erlenmeyer flask and shaken at 25 °C for 6 h. After mixing, solutions were filtered through a 0.2  $\mu$ m poresize filter and analyzed. The uptake of the adsorbates at equilibrium,  $q_e$  (mg/g), was calculated by the following equation:

$$q_{\rm e} = V \frac{C_0 - C_{\rm e}}{m} \tag{2}$$

where  $C_{e}$  is the equilibrium concentration of adsorbates (mg/l) in solution.

## 2.4. Chromatographic analysis

The concentration of monochlorophenols and chlorophenoxy herbicides in water solutions was measured by high-performance liquid chromatography with diode-array detector (Shimadzu LC-20, Kyoto, Japan). Separation of analytes was performed using a Phenomenex Luna  $C_{18}$  (4.6 × 150 mm, 3 µm) column (Torrance, CA, USA). For separation of the adsorbates, gradient elution was used. The elution profile was as follows: 0–10 min 25–55% B; 10–12 min 55% B; where elution solvent (A) was water adjusted to pH 3.0 with acetic acid and (B) acetonitrile. The temperature was 25°C, the flow rate 1.0 ml/min, and the detector wavelength was from 274 to 283 nm. Twenty µl of the sample was injected into the chromatographic column.

#### 3. Results and discussion

#### 3.1. Chromatography

Under applied chromatographic conditions, eluted peaks were distinctly separated. Typical chromatogram is shown in Fig. 1. Identification of peaks was based on comparison of retention times and diodearray spectra, taken at real time of analysis, with corresponding set of data obtained for authentic compounds. The calibration curves were constructed by plotting peak height vs. analytes' concentration and the curves were fitted by least squares linear regression analysis. The calibration range was 0.2–100 mg/l for all compounds. The equations for the linear regression lines and regression coefficients are presented in Table 1.



Fig. 1. Chromatogram of a starting monochlorophenols and chlorophenoxy acids mixture in water before the adsorption measurements; concentration of each compound 50 mg/l; chromatographic conditions as described in text: Peaks: (1) 2-CP; (2) 4-CP; (3) 3-CP; (4) MCPA; (5) 2,4-D.

Table 1 Calibration and validation results

Compounds	Linear regression equation y = ax + b	Regression coefficient R <sup>2</sup>	Analytical wavelength (nm)
2-CP	y = 3.4409x + 0.7268	0.9993	274
3-CP	y = 2.8759x + 0.2958	0.9994	274
4-CP	y = 3.1748x - 0.3761	0.9994	281
2,4-D	y = 0.8755x + 2.6746	0.9975	283
MCPA	y = 0.9850x + 0.5845	0.9971	278

### 3.2. Adsorption rate constant

Fig. 2 shows the adsorption kinetics of selected chlorophenols and herbicides on granular-activated carbon Filtrasorb 300 at 25 °C. In order to investigate the kinetics of adsorption of selected chloroorganic compounds on activated carbon, the rate constants were determined in terms of the pseudo-first-order



Fig 2. Adsorption kinetics of selected phenols and herbicides on granular-activated carbon Filtrasorb 300 at  $25^{\circ}$ C, initial concentration 100 mg/l.

Table 2

The pseudo-first and pseudo-second-order-rate constants of selected phenols and herbicides on granular-activated carbon Filtrasorb 300 at  $25^{\circ}$ C; initial concentration 100 mg/l

Compounds	Pseudo-first- order		Pseudo-second-order	
	<i>k</i> <sub>1</sub> (1/h)	$R^2$	$\overline{k_2}$ (g/mg h)	$R^2$
2-CP	0.689	0.989	21.241	0.997
3-CP	0.725	0.987	17.560	0.998
4-CP	0.714	0.986	17.316	0.997
2,4-D	0.811	0.986	18.842	0.997
MCPA	0.830	0.988	19.172	0.997

and pseudo-second-order models. The pseudo-first-order kinetic model is expressed as [31]:

$$\log(q_{\rm e} - q_t) = \log q_{\rm e} - \frac{k_1}{2.303}t$$
(3)

where  $q_e$  and  $q_t$  are the amounts of adsorption at equilibrium (mg/g) and at time *t* (h), respectively, and  $k_1$  is the rate constant of adsorption (1/h). Values of  $k_1$  were calculated from the plots of  $\log(q_e - q_t)$  vs. *t* for different concentrations of selected adsorbates.

If the sorption follows pseudo-second-order mechanism, the equation has the form [32]:

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} t \tag{4}$$

where  $q_e$  and  $q_t$  are the amounts of adsorption at equilibrium and at time *t*, respectively, and  $k_2$  is the rate constant of second-order adsorption (g/mg h). Values of  $k_2$  were calculated from the intercept and slope of the plots of  $t/q_t$  vs. t. The results are summarized in Table 2.

The pseudo-second-order model fits the experimental data quite well for all adsorbates with the correlation coefficients greater than 0.99. These results indicate that the adsorption system belongs to the second-order kinetic model.

#### 3.3. Adsorption isotherms

Adsorption isotherms of monochlorophenols and chlorophenoxy herbicides on the activated carbon are shown in Fig. 3. The experimental isotherms were modeled according to the Langmuir [33] and Freundlich [34] models. The Langmuir empirical model is represented by:



Fig 3. Adsorption isotherms of 2-chlorophenol, 3-chlorophenol, 4-chlorophenol, 2,4-dichlorophenoxyacetic acid, and 2-methyl-4-chlorophenoxyacetic acid on granular-activated carbon Filtrasorb 300 at 25 °C.

$$q_{\rm e} = \frac{bq_{\rm m}C_{\rm e}}{1 + bC_{\rm e}} \tag{5}$$

where *b* is the constant related to the free energy of adsorption (l/mg) and  $q_m$  the maximum adsorption capacity (mg/g). After integrating and applying the initial conditions, the integrated form of Eq. 4 becomes:

$$\frac{1}{q_{\rm e}} = \frac{1}{bq_{\rm m}C_{\rm e}} + \frac{1}{q_{\rm m}}$$
(6)

In order to obtain the rate constants and correlation coefficients, the straight-line plots of  $1/q_e$  vs.  $1/C_e$  for the selected adsorbates have been tested.

The experimental data were also fitted to the Freundlich equation:

$$q_{\rm e} = K_{\rm F} C_{\rm e}^{1/n} \tag{7}$$

which can be linearized to linear form:

$$\ln q_{\rm e} = \ln K_{\rm F} + \frac{1}{n} \ln C_{\rm e} \tag{8}$$

where  $K_{\rm F}$  is a constant indicative of the relative adsorption capacity of the adsorbent ((mg/g) (l/mg)<sup>1/n</sup>) and *n* is a constant indicative of the intensity of the adsorption. The straight-line plots of ln  $q_{\rm e}$  against ln  $C_{\rm e}$  were constructed.  $K_{\rm F}$  and 1/n values were obtained from the intercept and slope in linear regression result.

The results are summarized in Table 3.

In general, the linear regression correlation coefficient values show that the equilibrium data obtained for all adsorbates were better described by the Freundlich model than by the Langmuir isotherm model. The Freundlich constant  $K_F$  can be considered as an indicative parameter of the adsorption strength. The values of  $K_F$  determined from the Freundlich plots decreased in the order 4-CP>3-CP>2-CP>MCPA> 2,4-D. This suggests that chloroorganics adsorption by

Table 3

Langmuir and Freundlich equations correlation coefficients as well as  $K_{\rm F}$  and 1/n parameters for the adsorption of selected phenols and herbicides on granular-activated carbon Filtrasorb 300 at 25 °C

Compounds	Langmuir R <sup>2</sup>	Freundli	Freundlich		
		$K_{\rm F}^{*}$	1/n	$R^2$	
2-CP	0.911	11.646	0.251	0.946	
3-CP	0.961	12.554	0.260	0.946	
4-CP	0.959	12.667	0.267	0.954	
2,4-D	0.788	9.244	0.410	0.934	
MCPA	0.881	9.708	0.391	0.947	

\*((mg/g)  $(l/mg)^{1/n}$ ).

granular-activated carbon Filtrasorb 300 decreased in similar order. Moreover, chlorophenols are better adsorbed on activated carbon than chlorophenoxy hebicides.

## 4. Conclusions

Selected adsorbates-three monochlorophenols and two chlorophenoxy herbicides-are typical water pollutants. In environmental conditions, most often in surface water, groundwater, and even drinking water, many pollutants are present simultaneously. Despite this, both groups of compounds (chlorophenols and herbicides) are generally considered and studied separately. In this work, it is shown that the investigation of simultaneous adsorption of several chloroorganic compounds from aqueous solution on activated carbon is possible. In the case of kinetic studies, it is stated that dependence of adsorption quantity on time follows better model: pseudo-second-order than pseudo-first-order. For all adsorbates,  $R^2$  reaches high values. Chlorophenols are better adsorbed on the surface of activated carbon than herbicides. Adsorption equilibria are very well described by Freundlich equation for all adsorbates used.

# Acknowledgment

This work was partially supported by Ministry of Science and Higher Education (Poland) project No. N N209 0990 37.

#### References

- M. Czaplicka, Sources and transformations of chlorophenols in the natural environment, Sci. Total Environ. 322 (2004) 21–39.
- [2] M. Stoytcheva, Pesticides—Formulations, Effects, Fate, Intech, Rijeka, 2011.
- [3] M.W. Jung, K.H. Ahn, Y. Lee, K.P. Kim, J.S. Rhee, J.T. Park, K.J. Paeng, Adsorption characteristics of phenol and chlorophenols on granular activated carbons (GAC), Microchem, J. 70 (2001) 123–131.
- [4] G. Gryglewicz, K. Grabas, E. Lorenc-Grabowska, Preparation and characterization of spherical activated carbons from oil agglomerated bituminous coals for removing organic impurities from water, Carbon 40 (2002) 2403–2411.
- [5] P.J.M. Carrott, P.A.M. Mourao, M.M.L. Ribeiro Carrott, E.M. Goncüalves, Separating surface and solvent effects and the notion of critical adsorption energy in the adsorption of phenolic compounds by activated carbons, Langmuir 21 (2005) 11863–11869.
- [6] O. Hamdaoui, E. Naffrechoux, Modeling of adsorption isotherms of phenol and chlorophenols onto granular activated carbon Part I. Two-parameter models and equations allowing determination of thermodynamic parameters, J. Hazard. Mater. 147 (2007) 381–394.
- [7] Q.S. Liu, T. Zheng, P. Wang, J.P. Jiang, N. Li, Adsorption isotherm, kinetic and mechanism studies of some substituted phenols on activated carbon fibers, Chem. Eng. J. 157 (2010) 348–356.

- [8] Q. Lu, G.A. Sorial, The effect of functional groups on oligomerization of phenolics on activated carbon, J. Hazard. Mater. 148 (2007) 436–445.
- [9] A. Deryło-Marczewska, A.W. Marczewski, Effect of adsorbate structure on adsorption from solutions, Appl. Surf. Sci. 196 (2002) 264–272.
- [10] A. Deryło-Marczewska, K. Mirosław, A.W. Marczewski, D. Sternik, Studies of adsorption equilibria and kinetics of o-, m-, p-nitro- and chlorophenols on microporous carbons from aqueous solutions, Adsorption 16 (2010) 359–375.
- [11] A.A.M. Daifullah, B.S. Girgis, Removal of some substituted phenols by activated carbon obtained from agricultural waste, Water Res. 32 (1998) 1169–1177.
- [12] S. Biniak, G. Trykowski, M. Pakuła, A. Świątkowski, Z. Malinowska, S. Popiel, Effects of ozone dissolved in water on the physicochemical properties of activated carbons applied in drinking water treatment, Adsorpt. Sci. Technol. 28 (2010) 521–531.
- [13] F.C. Wu, R.L. Tseng, S.C. Huang, R.S. Juang, Characteristics of pseudo-second-order kinetic model for liquid-phase adsorption: A mini-review, Chem. Eng. J. 151 (2009) 1–9.
- [14] R.L. Tseng, K.T. Wu, F.C. Wu, R.S. Juang, Kinetic studies on the adsorption of phenol, 4-chlorophenol, and 2,4-dichlorophenol from water using activated carbons, J. Environ. Manage. 91 (2010) 2208–2214.
- [15] M.S. Bilgili, G. Varank, E. Sekman, S. Top, D. Özçimen, R. Yazıcı, Modeling 4-chlorophenol removal from aqueous solutions by granular activated carbon, Environ. Model. Assess. 17 (2012) 289–300.
- [16] S. Biniak, A. Świątkowski, M. Pakuła, M. Sankowska, K. Kuśmierek, G. Trykowski, Cyclic voltammetric and FTIR studies of powdered carbon electrodes in the electrosorption of 4chlorophenols from aqueous electrolytes, Carbon 51 (2013) 301–312.
- [17] J.Y. Hu, Y. Aizawa, Y. Ookubo, T. Morita, Y. Magara, Adsorptive characteristics of ionogenic aromatic pesticides in water on powdered activated carbon, Water Res. 32 (1998) 2593–2600.
- [18] Z. Aksu, E. Kabasakal, Batch adsorption of 2,4-dichlorophenoxy-acetic acid (2,4-D) from aqueous solution by granular activated carbon, Sep. Purif. Technol. 35 (2004) 223–240.
- [19] P. Chingombe, B. Saha, R.J. Wakeman, Effect of surface modification of an engineered activated carbon on the sorption of 2,4-dichlorophenoxy acetic acid and benazolin from water, J. Colloid Interf. Sci. 297 (2006) 434–442.

- [20] B.H. Hameed, J.M. Salman, A.L. Ahmad, Adsorption isotherm and kinetic modeling of 2,4-D pesticide on activated carbon derived from date stones, J. Hazard. Mater. 163 (2009) 121–126.
- [21] J.M. Salman, B.H. Hameed, Adsorption of 2,4-dichlorophenoxyacetic acid and carbofuran pesticides onto granular activated carbon, Desalination 256 (2010) 129–135.
- [22] K.Y. Foo, B.H. Hameed, Detoxification of pesticide waste via activated carbon adsorption process, J. Hazard. Mater. 175 (2010) 1–11.
- [23] V.O. Njoku, B.H. Hameed, Preparation and characterization of activated carbon from corncob by chemical activation with H<sub>3</sub>PO<sub>4</sub> for 2,4-dichlorophenoxyacetic acid adsorption, Chem. Eng. J. 173 (2011) 391–399.
- [24] J.M. Salman, V.O. Njoku, B.H. Hameed, Batch and fixed-bed adsorption of 2,4-dichlorophenoxyacetic acid onto oil palm frond activated carbon, Chem. Eng. J. 174 (2011) 33–40.
- [25] J.M. Salman, V.O. Njoku, B.H. Hameed, Adsorption of pesticides from aqueous solution onto banana stalk activated carbon, Chem. Eng. J. 174 (2011) 41–48.
- [26] K. Ignatowicz-Owsieniuk, I. Skoczko, Dependence of sorption of phenoxyacetic herbicides on their physico-chemical properties, Pol. J. Environ. Stud. 11 (2002) 339–344.
- [27] T.Y. Kim, S.S. Park, S.J. Kim, S.Y. Cho, Separation characteristics of some phenoxy herbicides from aqueous solution, Adsorption 14 (2008) 611–619.
- [28] K. Ignatowicz, Selection of sorbent for removing pesticides during water treatment, J. Hazard. Mater. 169 (2009) 953–957.
- [29] A. Deryło-Marczewska, M. Błachnio, A.W. Marczewski, A. Świątkowski, B. Tarasiuk, Adsorption of selected herbicides from aqueous solutions on activated carbon, J. Therm. Anal. Calorim. 101 (2010) 785–794.
- [30] R. Ocampo-Pérez, M.M. Abdeldaiem, J. Rivera-Utrilla, J.D. Méndez-Díaz, M. Sánchez-Polo, Modeling adsorption rate of organic micropollutants present in landfill leachates onto granular activated carbon, J. Colloid Interf. Sci. 385 (2012) 174–182.
- [31] S. Lagergren, Theorie der sogenannten adsorption geloester stoffe, Vetenskapsakad. Handl. 24 (1898) 1–39.
- [32] Y.S. Ho, G. McKay, Pseudo-second-order model for sorption processes, Process Biochem. 34 (1999) 451–465.
- [33] İ. Langmuir, The constitution and fundamental properties of solids and liquids, J. Am. Chem. Soc. 38 (1916) 2221–2295.
- [34] H.M.F. Freundlich, Über die adsorption in lösungen, Z. Phys. Chem. 57 (1906) 385–470.