



A QICAR model for quantifying connection between metal ionic character and biosorption capacity of *Pleurotus eryngii*

Nan He, Wan Li, Heng Xu*

Key Laboratory of Bio-resources and Eco-environment (Ministry of Education), College of Life Science, Sichuan University, Chengdu, Sichuan 610064, China

Tel. +86 28 85414644; Fax: +86 28 85418262; email: xuheng64@sina.com

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ABSTRACT

Quantitative ion character–activity relationship (QICAR) was used for quantifying connection between metal ionic characteristics with maximum biosorption capacity (q_{\max}). q_{\max} of *Pleurotus eryngii* was determined by Langmuir isotherm decreasing in the order of $\text{Pb}^{2+} > \text{Cr}^{3+} > \text{Cu}^{2+} > \text{Zn}^{2+} > \text{Cd}^{2+} > \text{Ni}^{2+} > \text{K}^+$. In batch studies, Minimum Run Res V Design was used to determine the most significant medium factors. It was found that pH, biomass loading, and contact time manifest stronger influence on biosorption of Pb^{2+} and Cd^{2+} . In the 22 physiochemical characteristics of metal ions, Covalent Index $X_m^2 r$ was correlated best with q_{\max} for all metal ions tested ($R^2=0.69$). Classifying metal ions appropriately could improve models and more ionic properties could be significantly correlated with q_{\max} . It turned out that the best fitting parameter for divalent metal ions was $X_m^2 r$ ($R^2=0.93$) and for transition metal ions was $|\log K_{\text{OH}}|$ ($R^2=0.90$). Moreover, two-variable model had greater ability to improve the fitting result ($R^2=0.99$).

Keywords: Biosorption; Metal ionic character; QICAR; Mushroom fruit body

1. Introduction

Nowadays, heavy metal pollution of wastewater is becoming a worldwide environmental problem. Heavy metal has toxicity toward aquatic life, including plants, animals, microbes, and even be harm for the environment. Meanwhile, it has a great impact on human health. Many reports indicate that excessive intake of copper by humans may lead to severe mucosal irritation, hepatic and renal damage, capillary damage, gastrointestinal irritation, and central nervous system irritation [1]. Excessive zinc enters the human body and accumulates in the liver and kidneys resulting in

hemochromatosis and gastrointestinal catarrh diseases. High concentration of nickel enters the body would cause cancers of the lungs, nose, and bone [2]. Thus, this heavy metal pollution crisis is extremely urgent. To solve the expanding problem, various methods have been employed to eliminate metal cations from aqueous solution, such as reverse osmosis, ion exchange, carbon adsorption, electroflotation, and chemical precipitation [3]. Adsorption method was widely researched and applied because of its high efficiency, limited pollution, and low cost. There are many factors that can influence adsorption capacity especially: metal ionic characteristics (e.g. atomic weight, ion radius, valence, etc.), the features of the adsorbents

*Corresponding author.

and adsorption conditions (e.g. pH, temperature, contact time, etc.) [4]. However, a large proportion of researchers have studied on reaction condition and adsorption mechanism of certain adsorbent rather than the influence of metal ionic character to the adsorption [5–7].

Quantitative structure activity–relationships (QSAR) is a method to establish the correlation between the bioactivity (e.g. toxicity or bioavailability), and chemical parameters of organic compounds in pharmacology and toxicology [8,9]. During the last few decades, some scientific researchers have studied correlations between physical and chemical properties of metal ions and their toxicity [10–13]. To predict metal toxicity, quantitative ion character–activity relationship (QICAR) have been developed by Newman and co-workers based on metal–ligand–binding tendencies [10,14,15]. QICAR can even be used for correlating metal ionic character with maximum biosorption capacity (q_{\max}), since carboxyl, hydroxyl, amino, and hydrosulfuryl play momentous roles in biosorption and the mechanism of adsorbing heavy metal ion include complexation and ion exchange [16–19].

Biosorption is a novel technique which developed rapidly in recent years with its advantage of efficiently dealing with metal cations contaminated water. From plants to microorganism, different kinds of organisms have been used as adsorbent, such as lichen and bamboo [20,21]. Fungi are a sort of novel bioadsorbent which possess extraordinary ability to remove metal cations from aqueous solution due to its abundant materials source and excellent degradability [22,23]. As reported earlier, plenty kinds varieties, of fungi have been widely used as adsorbents to metal cations removal recently, such as Pb^{2+} and Cd^{2+} removed by *Amanita rubescens*, Cu^{2+} and Pb^{2+} uptaked used by *Lentinus edodes* [24,25]. In this study, we choose *Pleurotus eryngii* a kind of common mushrooms as the adsorbent to remove various toxic metals (Pb^{2+} , Cd^{2+} , Cr^{3+} , Cu^{2+} , Zn^{2+} , Ni^{+} , K^{+}). Factorial design was also used to screening many factors to find the important effect and interations [23]. QICAR models is created to deduce maximum biosorption capacity and to understand the metal–biomass interactions.

2. Materials and methods

2.1. Preparation of the biosorbent

Fresh *P. eryngii* was collected from a mushroom production site in the suburbs of Chengdu, China. It was washed with generous amounts of deionized water and dried in an oven at 50°C for 3d. Then, dried biosorbent was grounded with a pulverizing mill (Joy-

oung, JYL-350B, China) and sieved with a 200-mesh to a size <0.075 mm.

2.2. Metal solution

Stock metal solutions of 1,000 mg/L were prepared by dissolving appropriate amounts of $Pb(NO_3)_2$, $Cr(NO_3)_3 \cdot 9H_2O$, KNO_3 , $Cu(NO_3)_2 \cdot 3H_2O$, $Zn(NO_3)_2 \cdot 4H_2O$, $Ni(NO_3)_2 \cdot 6H_2O$, and $Cd(NO_3)_2 \cdot 4H_2O$ (All reagents used here were analytical purity purchased from Changzheng Chemical Reagent company, Chengdu, China) in ultrapure water. The required working solutions of metal cations for the adsorption experiments were obtained by diluting each stock solution. Real concentration of metal ions in solutions was confirmed by flame atomic absorption spectroscopy (AAS, VARIAN, SpectrAA-220Fs, USA).

2.3. Biosorption experiments

According to pre-experiment, a series of flasks (150 ml) containing 50 ml metal solution were prepared for all the adsorption study. The pH was adjusted by adding HNO_3 (0.1, 1 M) and $NaOH$ (0.1, 1 M) solutions. The adsorption studies were carried out in a shaker incubator (SUKUN, SKY-211B, China), and flame atomic adsorption spectrometry was used to measure the metal concentration of filtrated solution.

The removal rate and amount of adsorbed metal ions (Q_e) per gram of *P. eryngii* were calculated as follows:

$$\text{Removal rate (\%)} = 100 \times (C_i - C_e) \times 1/C_i \quad (1)$$

$$\text{Adsorption amount (mg/g): } Q_e = (C_i - C_e)V \times 1/M \quad (2)$$

where C_i and C_e are the metal ions concentrations (mg/L) initially and at a given time t , respectively; V is the volume of the heavy metal solutions (L); M is the weight of adsorbent (g). Experiments were conducted in triplicate and the average values were taken as a result.

2.4. Factorial design methodology

The factorial design method determines which factors have significant effects on a response as well as how the effect of one factor varies according to the level of the other factors [26,27]. In order to evaluate the factors that affected the removal rate (%) of metal ions, a Minimum Run Res V Design was applied. The 6 statistically significant main factors of the process

(temperature, pH, initial metal ions concentration, biomass loading, contact time, and agitation speed) were selected in our study. In the full factorial design, 32 experiments are required. However, fractional factorial design was chosen to analyze the effects of each variable on the adsorption of metallic ions could shortcut batch experiments to 22. Each factor was represented at two levels—high and low, denoted by (+1) and (−1) signs, respectively [28]. The factors and their respective level are summarized in Table 1.

2.5. Ion characteristics and model development

For the modeling experiment, 22 metal ionic physiochemical properties were chosen to be variables. These ionic characteristics were as follows: r (Å), AN, ΔE_0 (V), ΔIP (eV), X_m , $|\log K_{OH}|$, X_m^2/r , Z^2/r , AN/ ΔIP , σ_p , OX, AR, AW, IP, AR/AW, $Z^*/Z^{*2}/r$, N , Z/r^2 , Z/AR^2 , Z/r , Z/AR given in Table 2 [10,29,30].

The software Eviews 6.0 was used to perform regression models of q_{max} values with 22 metal ionic characteristics. The level of significance was set as $\alpha=0.05$ and the following statistic parameters were computed: R =correlation coefficient, R^2 =coefficient of determination, R^2_{adj} =adjusted R^2 , SE=standard error of regression, F ratio= F test, P =probability of significance; MAPE=mean absolute percent error between observed and predicted values in prediction.

2.6. Fourier transform-Infrared spectroscopic analysis

High-resolution (0.1 cm^{-1}) Fourier transform-infrared (FT-IR) spectra for the biomass of *P. eryngii* (before and after the Pb^{2+} sorption) were recorded under vacuum on a VERTEX 80 v (Bruker optics). FT-IR spectrometer equipped with a DTGS (with KBr window) detector. Freeze-dried biomass was mixed with KBr powder, ground at room temperature and then compressed into a thin pellet.

Table 1
Experimental ranges and levels of the factors studied in the factorial design

| Signal | Factor | Units | Levels and range | |
|--------|----------------------------------|-------|------------------|-----|
| | | | −1 | +1 |
| A | Temperature | °C | 20 | 40 |
| B | Initial metal ions concentration | mg/L | 10 | 100 |
| C | pH | | 2 | 5 |
| D | Biomass loading | g/L | 1 | 6 |
| E | Agitation speed | rpm | 50 | 200 |
| F | Contact time | min | 10 | 240 |

3. Results and discussion

3.1. Screening of significant effects

Factorial design was employed to reduce the total number of experiments in order to achieve the best overall optimization of the process. Pb^{2+} and Cd^{2+} were selected as sample to represent soft ions and borderline ions. The removal of Cd^{2+} and Pb^{2+} are presented in Table 3. The analysis of variance (ANOVA) for biosorption study of Pb^{2+} and Cd^{2+} ions with *P. eryngii* was used in order to ensure a good model. The normal curves for the adsorption of the ions showed the main significant factors in the adsorption of each metallic ion. Values of “Prob>F” less than 0.05 indicate model terms are significant (Table 4). The R^2 of 0.9034, 0.8518, and the adjusted R^2 of 0.8986, 0.8452 were in reasonable agreement for Pb^{2+} , Cd^{2+} removal. The models proposed are as follows:

$$Pb(II) \text{ removal } (\%) = +0.361 + 0.029A + 0.032B - 0.166C + 0.130D + 0.079E + 0.143F \tag{3}$$

$$Cd(II) \text{ removal } (\%) = +0.295 - 0.013A + 0.009B - 0.026C + 0.083D + 0.0150E + 0.063F \tag{4}$$

where A, B, C, D, E, and F were defined in Table 1. Based on Eqs. (3) and (4) pH, biomass loading and contact time have a main effect on the adsorption. The significant factors affecting the Pb^{2+} , Cd^{2+} adsorption can be observed in Fig. 1. It was found that for Pb^{2+} , temperature, pH, contact time, biomass loading, and agitation speed had a positive effect while initial ion concentration was negative. It can be observed that the decreasing of initial concentration and temperature lead to better results of adsorption of Cd^{2+} . Considering the conclusion mentioned above, temperature for 30°C, pH for 5, biomass loading for 6 g/L, agitation speed for 200 rpm were optimum combination for metal cations removal.

3.2. Maximum sorption capacity

The maximum sorption capacity (q_{max}) of metal ions was calculated by the Langmuir isotherm model which assumes that uptake takes place on a homogeneous surface by monolayer sorption without any interaction between the adsorbed molecules. The linear form is expressed by the following equation.

Table 2
Values of metal ionic characteristics used in correlations

| Properties | Nomenclature | Pb | Cd | Cr | Cu | Zn | Ni | K |
|------------------|---|---------|---------|---------|---------|---------|----------|---------|
| AN | Atomic number | 82 | 48 | 24 | 29 | 30 | 28 | 19 |
| r (Å) | Pauling ionic radius (Å) | 1.18 | 0.95 | 0.62 | 0.73 | 0.75 | 0.69 | 1.38 |
| ΔIP (eV) | Change in ionization potential (eV) | 7.61 | 7.91 | 14.46 | 12.57 | 8.57 | 10.52 | 4.34 |
| ΔE_0 (V) | Electrochemical potential of the ion and its first stable reduced state (V) | 0.13 | 0.4 | 0.41 | 0.16 | 0.7618 | 0.23 | 2.92 |
| X_m | Electronegativity | 2.33 | 1.69 | 1.66 | 1.9 | 1.81 | 1.91 | 0.82 |
| $ \log K_{OH} $ | Absolute value of log of the first hydrolysis constant | 7.7 | 10.1 | 4 | 8 | 9 | 9.9 | 14.5 |
| X_m^2/r | Covalent index | 6.41 | 2.71 | 1.71 | 2.64 | 2.04 | 2.52 | 0.93 |
| Z^2/r | The cation polarization force | 3.39 | 4.21 | 14.52 | 5.48 | 5.33 | 5.8 | 0.72 |
| $AN/\Delta IP$ | Atomic number/change in ionization potential | 10.78 | 6.07 | 1.66 | 2.31 | 3.5 | 2.66 | 4.38 |
| σ_p | Softness index | 0.131 | 0.081 | 0.107 | 0.104 | 0.115 | 0.126 | 0.232 |
| OX | Oxidation number | 2 | 2 | 3 | 2 | 2 | 2 | 1 |
| AR | Atomic radius | 1.54 | 1.48 | 1.25 | 1.53 | 1.31 | 1.25 | 2.31 |
| AW | Atomic weight | 207.19 | 112.4 | 51.996 | 63.54 | 65.37 | 58.71 | 39.102 |
| IP | Ionization potential | 15.0322 | 16.908 | 30.96 | 20.2924 | 17.9644 | 18.16884 | 4.34066 |
| AR/AW | The ratio between atomic radius and atomic weight | 0.0074 | 0.0132 | 0.024 | 0.024 | 0.02 | 0.0213 | 0.0591 |
| Z^* | Effective charge | 19.8 | 16.4 | 11.35 | 14.25 | 14.9 | 13.6 | 7.4 |
| Z^{*2}/r | The cation polarization force | 297 | 274.449 | 198.118 | 282.03 | 267.482 | 237.128 | 41.173 |
| N | The number of valence shell electrons | 20 | 18 | 11 | 17 | 18 | 16 | 8 |
| Z/r^2 | The cation polarization force | 1.417 | 2.216 | 7.732 | 3.753 | 3.55 | 4.201 | 0.525 |
| Z/AR^2 | The similar polarization force | 0.843 | 0.913 | 1.92 | 1.183 | 1.165 | 1.28 | 0.187 |
| Z/r | The cation polarization force | 1.695 | 2.105 | 4.839 | 2.74 | 2.665 | 2.899 | 0.725 |
| Z/AR | The similar polarization force | 1.299 | 1.351 | 2.4 | 1.307 | 1.526 | 1.6 | 0.433 |

$$1/q_e = 1/q_{\max} + 1/(q_{\max}b)C_e \quad (5)$$

It could be transformed for fitting of the experimental data as following equation:

$$C_e/q_e = (1/q_{\max})C_e + 1/(q_{\max}b) \quad (6)$$

where q_e (mg/g) is the equilibrium metal uptake, C_e (mg/L) represents the concentration of solution at equilibrium, q_{\max} (mmol/g) is the maximum adsorption and b (L/mg) is the Langmuir constant positive related to the energy of adsorption. The values of q_{\max} for different metal ions were listed in Table 5.

It showed that q_{\max} decreased in the following order: $Pb^{2+} > Cr^{3+} > Cu^{2+} > Zn^{2+} > Cd^{2+} > Ni^{2+} > K^+$ and presented *P. eryngii* might have prominent capacity to remove Pb^{2+} from liquid which was proved by some similar biosorbent [31]. Comparing with other biosorbent, *P. eryngii* displayed superiority to remove Pb^{2+} from solution. In this study, q_{\max} of Pb adsorbed by

P. eryngii was 0.412 mmol/g, namely 85.284 mg/g. It's more than 75.8 mg/g of lichen (*Parmelina tiliaceae*) biomass [20] and 77.8 mg/g of bacterium *Pseudomonas* sp [32]. Several other studies also indicated this capacity order, for example, the biosorption affinity of *Tricholoma lobayense* was $Pb^{2+} > Cu^{2+} > Cd^{2+}$ [23] and biomass for biosorption of metal ions by *Rhizopus nigricans* was $Pb^{2+} > Cu^{2+} > Zn^{2+} > Ni^{2+}$ [33]. A study of biosorption of Cd(II) and Cr(III) from aqueous solution by moss (*Hylocomium splendens*) biomass also presented the maximum biosorption capacity (q_{\max}) was $Cr^{3+} > Cd^{2+}$ [34]. According to the principal of HSAB (hard-soft-acid-base), soft ions (Pb^{2+}) mainly interact with the biological ligands via covalent bond, hard ions (K^+) mainly via electrostatic interaction [35,36] and borderline ions (Cd^{2+} , Cr^{3+} , Cu^{2+} , Zn^{2+} , Ni^{2+}) are variant. Cadmium cation was mainly removed through apparently chelation and nickel was mainly ion exchange [37,38]. It might explain the order of abovementioned uptake capacity.

Table 3
Factorial design experimental data

| Std. | Factors | | | | | | Responses (% removal) | |
|------|---------|-----|---|---|-----|-----|-----------------------|------|
| | A | B | C | D | E | F | Pb | Cd |
| 1 | 20 | 10 | 2 | 6 | 50 | 10 | 79.2 | 48.7 |
| 2 | 20 | 10 | 2 | 1 | 200 | 10 | 26.1 | 24.5 |
| 3 | 20 | 100 | 2 | 1 | 200 | 10 | 92.8 | 68.5 |
| 4 | 40 | 10 | 2 | 6 | 50 | 240 | 41.9 | 28.1 |
| 5 | 20 | 100 | 2 | 6 | 200 | 10 | 36.7 | 25 |
| 6 | 40 | 100 | 5 | 1 | 50 | 240 | 39.6 | 23.4 |
| 7 | 40 | 100 | 2 | 1 | 50 | 10 | 48.4 | 15.2 |
| 8 | 20 | 100 | 2 | 6 | 50 | 240 | 67.5 | 24.3 |
| 9 | 20 | 100 | 5 | 1 | 50 | 10 | 24.4 | 21 |
| 10 | 20 | 100 | 5 | 6 | 200 | 240 | 74.8 | 68.1 |
| 11 | 20 | 10 | 5 | 6 | 50 | 240 | 77.3 | 23 |
| 12 | 40 | 10 | 5 | 1 | 50 | 10 | 92.7 | 80.9 |
| 13 | 40 | 10 | 2 | 6 | 200 | 240 | 10.2 | 17.3 |
| 14 | 20 | 10 | 5 | 6 | 200 | 10 | 24.5 | 38.4 |
| 15 | 20 | 10 | 2 | 1 | 50 | 240 | 40.7 | 43.9 |
| 16 | 40 | 100 | 5 | 6 | 50 | 10 | 34 | 12.8 |
| 17 | 40 | 100 | 2 | 6 | 200 | 240 | 15.3 | 26.2 |
| 18 | 40 | 100 | 5 | 1 | 50 | 10 | 9.1 | 14.7 |
| 19 | 40 | 10 | 2 | 1 | 200 | 240 | 89.6 | 69.6 |
| 20 | 40 | 10 | 5 | 6 | 200 | 240 | 26.3 | 11.8 |
| 21 | 40 | 100 | 5 | 1 | 200 | 10 | 80.1 | 48.9 |
| 22 | 20 | 10 | 5 | 1 | 200 | 240 | 12.1 | 19.5 |

Table 4
ANOVA for the regression model

| Term | Sum of squares (SS) | | F-Value | | P-value | |
|-------------------------------|---------------------|----------|---------|-------|---------|---------|
| | Pb | Cd | Pb | Cd | Pb | Cd |
| Model | 1.36 | 0.62 | 23.32 | 12.13 | <0.0001 | <0.0001 |
| A | 0.012 | 0.007775 | 39.11 | 0.56 | 0.1487 | 0.2851 |
| B | 0.028 | 0.001259 | 2.84 | 0.08 | 0.0809 | 0.5210 |
| C | 0.51 | 0.47 | 2.5 | 48.71 | <0.0001 | <0.0001 |
| D | 0.43 | 0.064 | 38.27 | 9.60 | <0.0001 | 0.0007 |
| E | 0.12 | 0.008 | 21.36 | 1.42 | 0.0013 | 0.2619 |
| F | 0.39 | 0.15 | 14.09 | 12.97 | <0.0001 | 0.0027 |
| Residual | 0.13 | 0.09 | | | | |
| Cor. total | 1.49 | 0.71 | | | | |
| R ² | 0.9034 | 0.8518 | | | | |
| R ² _{adj} | 0.8986 | 0.8452 | | | | |

3.3. Correlation ionic properties with q_{max}

3.3.1. Models for all metal ions

The models were built with the q_{max} values of seven metal ions and their corresponding ionic properties by using software Eviews 6.0. The results revealed that

among 22 kinds of parameter only 2 (X_m^2r , AW_m) were statistical significant (at the level of significance 0.005) (Table 6). X_m^2r showed the highest statistical significance, but only could explain 64% of the variation in q_{max} values. The relationship between q_{max} and X_m^2r was depicted in Fig. 2(a).

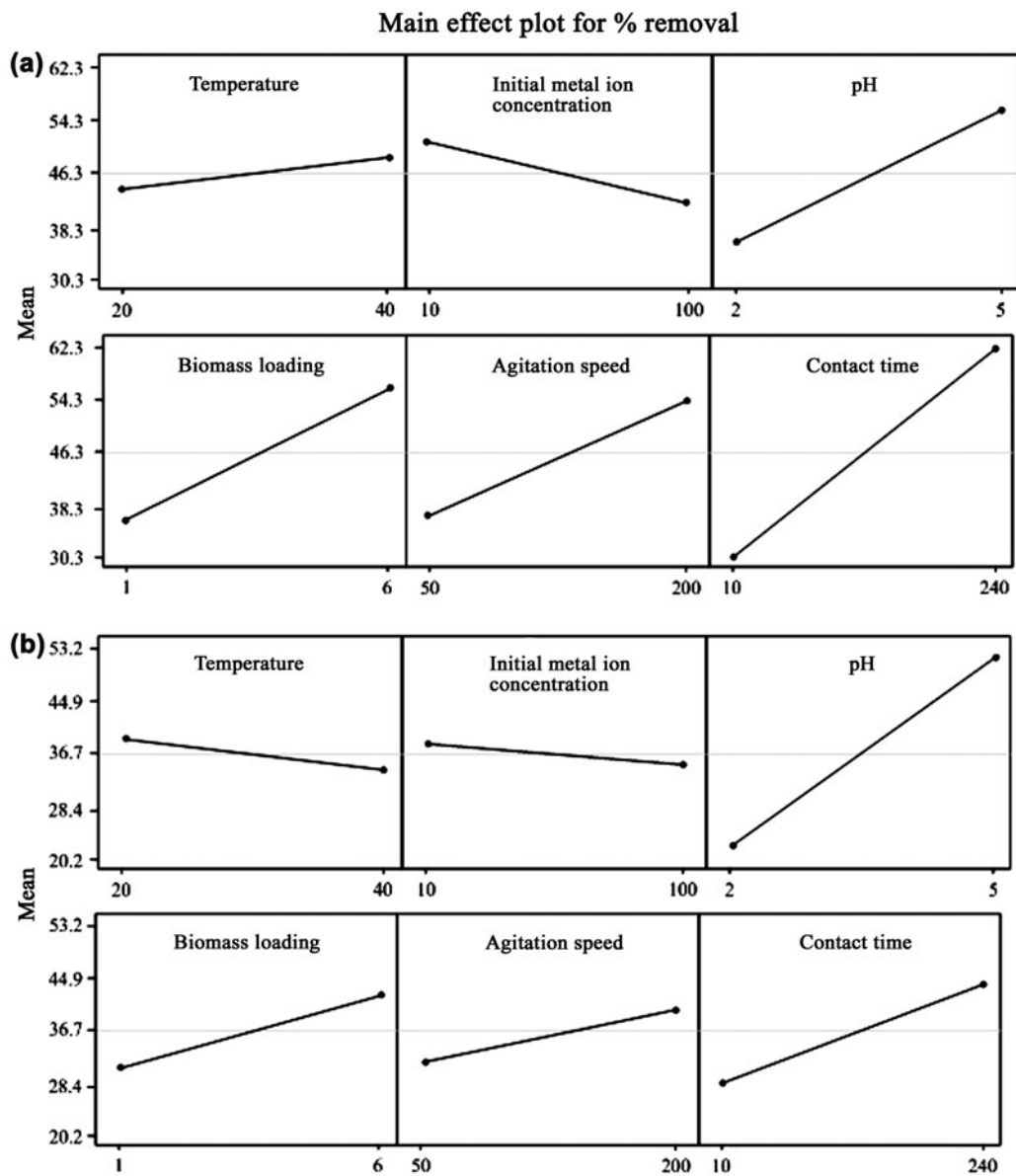


Fig. 1. Main effects plot for (a) the removal of Pb(II) and (b) removal of Cd(II) by *P. eryngii*.

Table 5
Maximum uptake capacity (q_{\max}) by *P. eryngii*

| Metal | q_{\max} (mmoml/g) | R^2 | Outer electronic configuration | Class |
|------------------|----------------------|-------|----------------------------------|---------------------|
| Pb ²⁺ | 0.412 | 0.932 | 6s ² 6p ² | Nontransition metal |
| Cr ³⁺ | 0.253 | 0.974 | 3d ⁵ 4s ¹ | Transition metal |
| Cu ²⁺ | 0.217 | 0.933 | 3d ¹⁰ 4s ¹ | Transition metal |
| Zn ²⁺ | 0.202 | 0.958 | 3d ¹⁰ 4s ² | Transition metal |
| Cd ² | 0.196 | 0.912 | 4d ¹⁰ 5s ² | Transition metal |
| Ni ²⁺ | 0.183 | 0.967 | 3d ⁸ 4s ² | Transition metal |
| K ⁺ | 0.112 | 0.982 | 4s ¹ | Nontransition metal |

Table 6

Regression models of relationship between q_{\max} and metal ion characteristics for all metal ions tested ($n=7$)

| Model ($q_{\max} =$) | R^2 | R^2_{adj} | SE | F | p | MAPE |
|--------------------------|-------|--------------------|-------|--------|-------|--------|
| 1. $0.045X_m^2r + 0.076$ | 0.694 | 0.639 | 0.042 | 24.904 | 0.004 | 13.656 |
| 2. $0.001AW + 0.088$ | 0.564 | 0.492 | 0.457 | 15.059 | 0.012 | 21.042 |

Fig. 2(a) indicated the biosorption capacity of the biomass rise along with the Covalent Index Value of metal ion. Similar result was obtained by Brady for *Rhizopus arrhizus* and Chen for *Saccharomyces cerevisiae* [39,40], who both built the linear relation between q_{\max} and X_m^2r and found out they were positively correlated. Nieboer and McBryde [41] introduced that Covalent Index had a tendency to form metal ionic complexes in aqueous solution. According to Nieboer, the greater the Covalent Index values the softer the metal ions. These ions were combined with the functional groups of biological in the order of $S \rightarrow N \rightarrow O$ and easily formed stable complexes with the group including S and N like S^{2-} , RS^- , R_2S , CN^- , H^- , R^- , then less stable R_2NH , $R_3N=N^-$, $-CO-N-R$, RNH_2 . On the contrary, hard ions firstly formed stable complexes with the group including O, such as ROH , $RCOO^-$,

CO , ROR , HPO_4^{2-} , OH^- , O^{2-} , H_2O , NO_3^- , $ROSO_3^-$, CO_3^{2-} . Therefore, we can conclude that the covalent interactions between ions and organisms should not be neglected for its important effect in ion adsorption mechanism.

AW also had close bond with q_{\max} . Some studies proved that with increasing atomic weight, the biosorption increased in the same order [42,43]. Javier Bayo indicated atomic weight can explain the affinity order for the four heavy metals was $Pb(II) > Cu(II) > Ni(II)$ [42].

3.3.2. Models for divalent metal

When models were set up with only divalent metal ions, more ionic characteristics became statistical significant (AN , X_m , $r(\text{\AA})$, Z^2/r , $AN/\Delta IP$, N , Z/r^2 , Z/r),

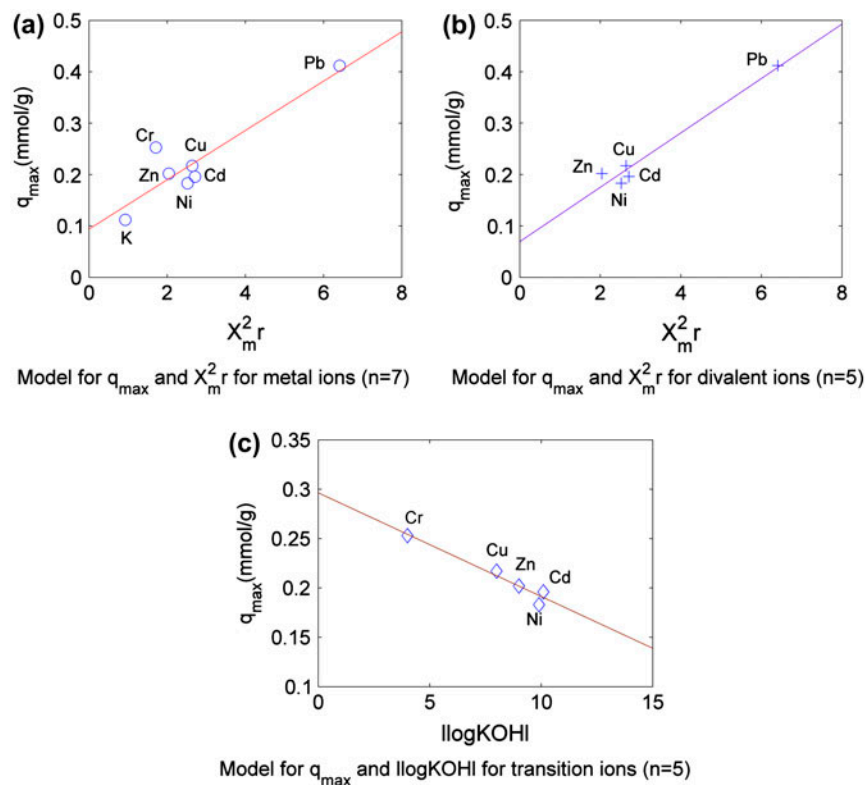


Fig. 2. Models for q_{\max} and X_m^2r for all metal ions ($n=7$) (a), q_{\max} and X_m^2r for divalent metal ions ($n=5$) (b) and q_{\max} and $l\log KOHl$ for transition metal ions ($n=5$) (c).

Table 7

Regression models of relationship between q_{\max} and metal ion characteristics for divalent metal ions ($n = 5$)

| Model ($q_{\max} =$) | R^2 | R^2_{adj} | SE | F | p | MAPE |
|--|-------|--------------------|-------|---------|-------|--------|
| 4. $0.053X_m^2r + 0.096$ | 0.928 | 0.904 | 0.021 | 78.365 | 0.003 | 7.214 |
| 5. $0.328 X_m + 0.042$ | 0.731 | 0.649 | 0.038 | 17.566 | 0.025 | 13.057 |
| 6. $0.001AW + 0.088$ | 0.666 | 0.569 | 0.043 | 13.298 | 0.036 | 14.190 |
| 7. $0.035Z^* - 0.312$ | 0.671 | 0.576 | 0.047 | 13.591 | 0.035 | 13.797 |
| 8. $0.403r(\text{\AA}) - 0.105$ | 0.557 | 0.438 | 0.056 | 8.831 | 0.059 | 14.395 |
| 9. $0.582 - 0.074Z^2/r$ | 0.701 | 0.613 | 0.038 | 15.437 | 0.029 | 15.619 |
| 10. $0.022AN/\Delta IP + 0.112$ | 0.548 | 0.428 | 0.050 | 8.555 | 0.061 | 15.792 |
| 11. $0.229 X_m + 0.019 Z^* - 0.508$ | 0.983 | 0.967 | 0.012 | 117.596 | 0.008 | 3.202 |
| 12. $0.023Z^* - 0.037 \log K_{\text{OH}} - 0.171$ | 0.910 | 0.824 | 0.026 | 20.662 | 0.046 | 8.300 |

and the former parameters (X_m^2r , AW , Z^*) showed greater fitness (Table 7) ($\alpha = 0.005$). Most parameters such as X_m^2r , AW , X_m , Z^* , $r(\text{\AA})$, $AN/\Delta IP$ were positively correlated with metal uptake capacities, and Z^2/r was inversely correlated with q_{\max} . Some similar results were reported by Tobin et al. [44], and they found that the amount of uptake of divalent cations was directly related with ionic radius $r(\text{\AA})$. X_m^2r was still the best fitting variable ($R^2_{\text{adj}} = 0.847$, $MAPE = 8.542$) (Fig. 2(b)). And from Table 7, we can realize that appropriate bivariate models generally could increase the imitative effect (model. 11 and 12).

3.3.3. Models for transition metal ions

This study selected divalent metal ions (Cd^{2+} , Cr^{3+} , Cu^{2+} , Zn^{2+} , Ni^{2+}) to build models as revealed in Table 8. Several dissimilar ionic characteristics such as $|\log K_{\text{OH}}|$, IP , Z/r^2 , Z/AR^2 became statistical significant ($\alpha = 0.005$). Among them metal uptake capacities only increased with the decreasing of $|\log K_{\text{OH}}|$, and the

most valuable parameter ($R^2_{\text{adj}} = 0.871$, $MAPE = 2.169$) shown in Fig. 2(c). It was also noted from model 19–22 that two-variable model had greater ability to improve the fitting results. A combination of Z/r^2 and $|\log K_{\text{OH}}|$ provided the best fit.

Z/r^2 , Z/AR^2 , Z/r and Z^2/r were different forms of the cation-polarizing power, which presented the strength of ion interaction of metal and cells. Padeste [45] reported carbonate with transition metal ions was easier to hydrolyze than ions II A and I A. Cation-polarizing power and $|\log K_{\text{OH}}|$ were inversely correlated. Ion hydrolysis ability enhanced with cation-polarizing power increasing and resulting to the reduction of $|\log K_{\text{OH}}|$. From Table 8, we can infer that ion hydrolysis played an important role in biosorption of metal especially transition metal. The close connection between q_{\max} and ionization potential indicated that transition metals had unfilled valence shell and better electron affinity.

The best univariate model 13 showed $|\log K_{\text{OH}}|$ could explain 87% variation of q_{\max} , and mean

Table 8

Regression models of relationship between q_{\max} and metal ion characteristics for transition metal ions ($n = 5$)

| Model ($q_{\max} =$) | R^2 | R^2_{adj} | SE | F | p | MAPE |
|---|-------|--------------------|-------|--------|-------|--------|
| 13. $0.296 - \log K_{\text{OH}} + 0.011$ | 0.903 | 0.871 | 0.000 | 57.016 | 0.005 | 2.169 |
| 14. $0.005Z^2/r + 0.171$ | 0.597 | 0.485 | 0.145 | 10.182 | 0.049 | 12.121 |
| 15. $0.003IP + 0.119$ | 0.769 | 0.699 | 0.011 | 21.359 | 0.019 | 8.843 |
| 16. $0.038Z/r^2 + 0.049$ | 0.709 | 0.623 | 0.039 | 15.998 | 0.028 | 9.725 |
| 17. $0.209Z/AR^2 - 0.057$ | 0.700 | 0.612 | 0.400 | 15.363 | 0.030 | 10.074 |
| 18. $0.077Z/r - 0.023$ | 0.790 | 0.726 | 0.033 | 23.956 | 0.016 | 6.913 |
| 19. $0.366 - 0.003Z^2/r - 0.016 \log K_{\text{OH}} $ | 0.955 | 0.910 | 0.008 | 23.625 | 0.041 | 1.985 |
| 20. $0.378 - 0.008Z/r^2 - 0.016 \log K_{\text{OH}} $ | 0.999 | 0.999 | 0.001 | 1350.2 | 0.001 | 0.267 |
| 21. $0.396 - 0.041Z/AR^2 - 0.016 \log K_{\text{OH}} $ | 0.998 | 0.997 | 0.001 | 1213.7 | 0.001 | 0.283 |
| 22. $0.008IP - 0.065Z/AR^2 + 0.119$ | 0.903 | 0.810 | 0.008 | 19.037 | 0.049 | 2.450 |

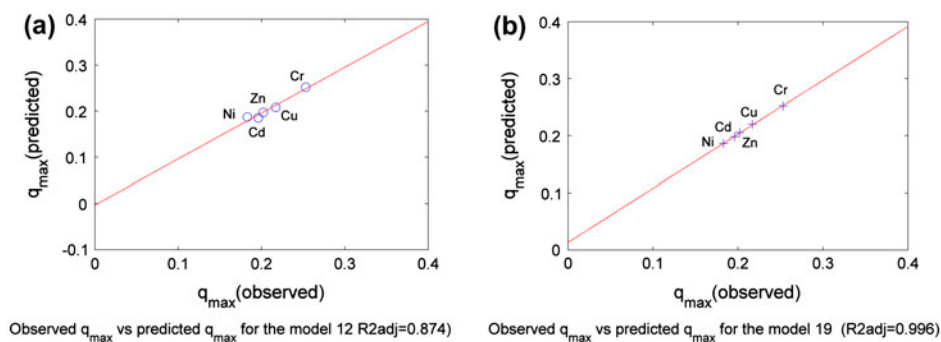


Fig. 3. Observed q_{max} vs. predicted q_{max} for the model 13 ($R^2_{adj}=0.874$) (a) and Observed q_{max} vs. predicted q_{max} for the model 20 ($R^2_{adj}=0.996$) (b).

absolute percent error was only 2.169. Therefore, the value of observed q_{max} and predicted q_{max} were very close (Fig. 3(a)). That two-variable model 20 had more predictive ability than 13 (Fig. 3(b)) It presented these

QICAR models could predict metal uptake capacity according to metal ionic characteristics excellently.

3.4. Fourier transform-infrared analysis

FT-IR spectra of the control biomass (metal free) were shown in Fig. 4(a). The absorption band at $3,384\text{ cm}^{-1}$ was assigned to the shake-up adsorption peak of $-\text{OH}$ and $-\text{NH}_2$ groups on the adsorbent surfaces (ν ($-\text{OH}$) and ν ($-\text{NH}_2$)) [46]. The peak at $2,926$ was due to aliphatic hydrocarbons symmetric stretching [47]. The formation of the band at $1,630\text{ cm}^{-1}$ was typical for $\gamma\text{C}=\text{O}$ of amide. And the peaks at $1,453$ – $1,404\text{ cm}^{-1}$, $1,251$ – $1,204\text{ cm}^{-1}$ represented C–N stretching vibration of amino acid. In 4.b, the FT-IR patterns of Pb^{2+} loaded samples showed that the peak shift from $3,384$ to $3,439\text{ cm}^{-1}$ suggesting possible interaction between amino group and Pb^{2+} [16]. After contacting with Pb^{2+} , both peak wave numbers of two adsorbents at $1,251$ and $1,204\text{ cm}^{-1}$ decreased. The IR spectra before and after Pb^{2+} binding presented that amide I, II, IV, and sulfamide groups were involved in Pb^{2+} binding. The carboxyl band position shifted from $1,453$ to $1,400\text{ cm}^{-1}$ and $1,404$ to $1,384\text{ cm}^{-1}$ after biosorption of Pb^{2+} which also indicated that carboxyl group interacts with Pb^{2+} .

Conclusion

In the present study, *P. eryngii* performed well as metal cations absorbent.

Medium biomass loading, contact time, and pH were found to be key factors to affect removal Pb^{2+} and Cd^{2+} .

FT-IR spectra of biomass of *P. eryngii* before and after Pb^{2+} biosorption showed that amino/amido, sulfamide and carboxyl groups interacted with Pb^{2+} and major contribution was due to N-containing groups.

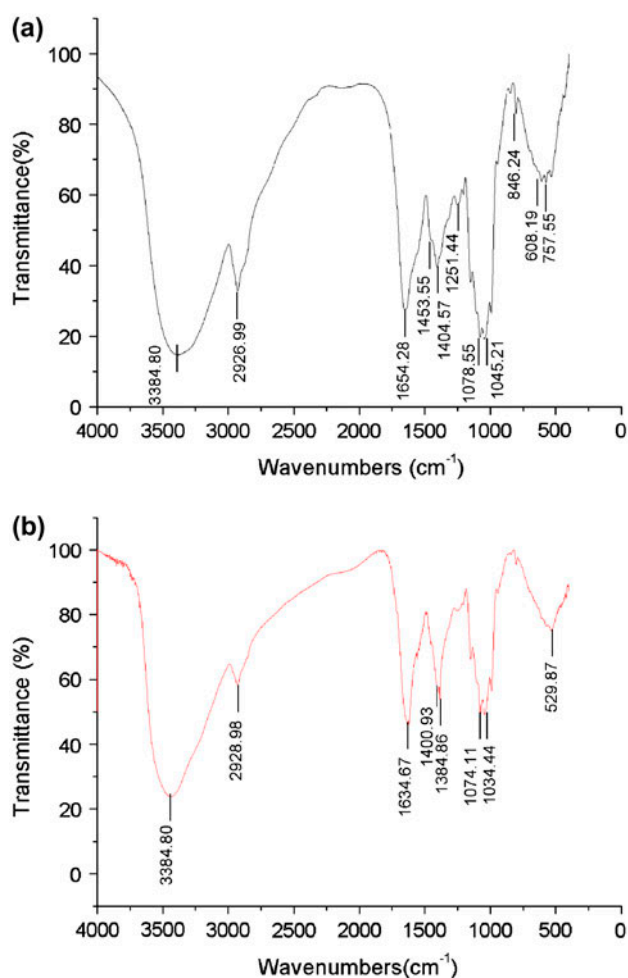


Fig. 4. FT-IR spectra of the intact *P. eryngii*(a) and *P. eryngii* with lead nitrate solution (200 mg l^{-1}) (b).

The metal uptake capacity of *P. eryngii* was $Pb^{2+} > Cr^{3+} > Cu^{2+} > Zn^{2+} > Cd^{2+} > Ni^{2+} > K^{+}$ calculated by the Langmuir isotherm model. QICAR models could successfully correlate biosorption capacity with metal ionic characteristics.

In the 22 ion properties $r(\text{Å})$, AN, $\Delta E_0(V)$, $\Delta IP(eV)$, X_{mv} , $|\log K_{OH}|$, X_m^2/r , Z^2/r , AN/ ΔIP , σ_p , OX, AR, AW, IP, AR/AW, $Z^*/Z^{*2}/r$, N, Z/r^2 , Z/AR^2 , Z/r , Z/AR , Covalent Index Value displayed excellent linear correlation with q_{max} for all tested metal ions. It could be inferred that covalent binding principally affect surface biosorption.

Appropriate classified metal ions could improve connection between ionic characteristics and biosorption capacity. Divalent metal ions and transition metal ions both presented significant linear relations with more ionic properties which might explain different biosorption principles of different metal ions. QICAR models could predict metal uptake capacity according to metal ionic characteristics excellently.

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References

- [1] S. Larous, A.H. Meniai, M.B. Lehocine, Experimental study of the removal of copper from aqueous solutions by adsorption using sawdust, *Desalination* 185 (2005) 483–490.
- [2] C. Wang, J. Liu, Z. Zhang, B. Wang, H. Sun, Adsorption of Cd(II), Ni(II), and Zn(II) by tourmaline at acidic conditions: Kinetics, thermodynamics and mechanisms, *Ind. Eng. Chem. Res.* 51 (2012) 4397–4406.
- [3] S. Rengaraj, S.H. Moon, Kinetics of adsorption of Co(II) removal from water and wastewater by ion exchange resins, *Water Res.* 36 (2002) 1783–1793.
- [4] C. Chen, J. Wang, Influence of metal ionic characteristics on their biosorption capacity by *Saccharomyces cerevisiae*, *Appl. Microbiol. Biotechnol.* 74 (2007) 911–917.
- [5] V. Prigione, M. Zerlotti, D. Refosco, V. Tadini, A. Anastasi, G.C. Varese, Chromium removal from a real tanning effluent by autochthonous and allochthonous fungi, *Bioresour. Technol.* 100 (2009) 2770–2776.
- [6] M. Tsezos, Biosorption of metals. The experience accumulated and the outlook for technology development, *Hydrometall.* 59 (2001) 241–243.
- [7] A. Mansri KIB, J. François, Chromium removal using modified poly(4-vinylpyridinium) bentonite salts, *Desalination* 245 (2009) 95–107.
- [8] J.J. Hostýnek, P.S. Magee, Fragrance allergens classification and ranking by QSAR, *Toxicology in Vitro* 11 (1997) 377–384.
- [9] D.J.W. Blum, R.E. Speece, Determining chemical toxicity to aquatic species, *Environ. Technol.* 24 (1990) 284–293.
- [10] M.C. Newman, J.T. McCloskey, Predicting relative toxicity and interactions of divalent metal ions Microtox bioluminescence assay, *Environ. Toxicol. Chem.* 15 (1996) 275–281.
- [11] J.D. Walker, M. Enache, J.C. Dearden, Quantitative cationic-activity relationships for predicting toxicity of metals, *Environ. Toxicol. Chem.* 22 (2003) 1916–1935.
- [12] H.T. Wolterbeek, T.G. Verburg, Predicting metal toxicity revisited general properties vs. specific effects, *Sci. Total Environ.* 279 (2001) 87–115.
- [13] B. Thomas, U.Y. Kinraide, A scale of metal ion binding strengths correlating with ionic charge, Pauling electronegativity, toxicity, and other physiological effects, *J. Inorg. Biochem.* 101 (2007) 1201–1213.
- [14] M.C. Newman, J.T. McCloskey, C.P. Tataru, Using metal-ligand binding characteristics to predict metal toxicity quantitative ion character-activity relationships (QICARs), *Environ. Health Perspect.* 106 (1998) 1419–1425.
- [15] C.P. Tataru, M.C. Newman, J.T. McCloskey, P.L. Williams, Use of ion characteristics to predict relative toxicity of mono-, di- and trivalent metal ions *Caenorhabditis elegans* LC50, *Aquat. Toxicol.* 42 (1998) 255–269.
- [16] S.S. Zamil, S. Ahmad, M.H. Choi, J.Y. Park, S.C. Yoon, Correlating metal ionic characteristics with biosorption capacity of *Staphylococcus saprophyticus* BMSZ711 using QICAR model, *Bioresour. Technol.* 100 (2009) 1895–1902.
- [17] J. Remacle, The cell wall and metal binding, In: B. Volesky (Ed.), *Biosorption of Heavy Metals*, CRC press, Boca Raton, 1990, pp. 7–44.
- [18] B. Volesky, Removal and recovery of heavy metals by biororption, In: B. Volesky (Ed.), *Biosorption of Heavy Metals*, CRC press, Boca Raton, pp. 7–44, 1990.
- [19] S.V. Avery, J.M. Tobin, Mechanism of adsorption of hard and soft metal ions to *Saccharomyces cerevisiae* and influence of hard and soft anions, *Applied Environ. Microbiol.* 59 (1993) 2851–2856.
- [20] O.D. Uluozlu, A. Sari, M. Tuzen, M. Soylok, Biosorption of Pb(II) and Cr(III) from aqueous solution by lichen (*Parmelina tiliaceae*) biomass, *Bioresour. Technol.* 99 (2008) 2972–2980.
- [21] S.Y. Wang, M.H. Tsai, S.F. Lo, M.J. Tsai, Effects of manufacturing conditions on the adsorption capacity of heavy metal ions by Makino bamboo charcoal, *Bioresour. Technol.* 99 (2008) 7027–7033.
- [22] X. Jing, Y. Cao, X. Zhang, D. Wang, X. Wu, H. Xu, Biosorption of Cr(VI) from simulated wastewater using a cationic surfactant modified spent mushroom, *Desalination* 269 (2011) 120–127.
- [23] Y. Cao, Z. Liu, G. Chen, X. Jing, H. Xu, Exploring single and multi-metal biosorption by immobilized spent *Tricholoma lobayense* using multi-step response surface methodology, *Chem. Eng. J.* 164 (2010) 183–195.
- [24] A. Sari, M. Tuzen, Kinetic and equilibrium studies of biosorption of Pb(II) and Cd(II) from aqueous solution by macrofungus (*Amanita rubescens*) biomass, *J. Hazard. Mater.* 164 (2009) 1004–1011.
- [25] I. Kiran, T. Akar, S. Tunali, Biosorption of Pb(II) and Cu(II) from aqueous solutions by pretreated biomass of *Neurospora crassa*, *Process Biochem.* 40 (2005) 3550–3558.
- [26] M.E.R. Carmona, M.A.P. da Silva, S.G. Ferreira Leite, Biosorption of chromium using factorial experimental design, *Process Biochem.* 40 (2005) 779–788.
- [27] T. Sahan, H. Ceylan, N. Sahiner, N. Aktas, Optimization of removal conditions of copper ions from aqueous solutions by *Trametes versicolor*, *Bioresour. Technol.* 101 (2010) 4520–4526.
- [28] L.S. De Lima, M.D.M. Araujo, S.P. Quináia, D.W. Migliorini, J.R. Garcia, Adsorption modeling of Cr, Cd and Cu on activated carbon of different origins by using fractional factorial design, *Chem. Eng. J.* 166 (2011) 881–889.

- [29] D.F.V. Lewis, M. Dobrota, M.G. Taylor, Metal toxicity in two rodent species and redox potential: Evaluation of quantitative structure-activity relationships, *Environ. Toxicol. Chem.* 18 (1999) 2199–2204.
- [30] Y.T. Zhang, X. Sun, The structural data mining of solubility of metallic sulphide, *Comput. Appl. Chem.* 21 (2004) 690–694.
- [31] N.L. Iskandar, N.A.I.M. Zainudin, S.G. Tan, Tolerance and biosorption of copper (Cu) and lead (Pb) by filamentous fungi isolated from a freshwater ecosystem, *J. Environ. Sci.* 23 (2011) 824–830.
- [32] W. Huang, Z. Liu, Biosorption of Cd(II)/Pb(II) from aqueous solution by biosurfactant-producing bacteria: Isotherm kinetic characteristic and mechanism studies, *Colloids Surf. B* 105 (2013) 113–119.
- [33] A. Kogej, A. Pavko, Comparison of *Rhizopus nigricans* in a pelleted growth form with some other types of waste microbial biomass as biosorbents for metal ions, *World J. Microbiol. Biotechnol.* 17 (2007) 677–685.
- [34] A. Sari, D. Mendil, M. Tuzen, M. Soylak, Biosorption of Cd (II) and Cr(III) from aqueous solution by moss (*Hylocomium splendens*) biomass: Equilibrium, kinetic and thermodynamic studies, *Chem. Eng. J.* 144 (2008) 1–9.
- [35] R.G. Pearson, Hard and soft acids and bases, *Am. Chem. Soc.* 85 (1963) 3533–3539.
- [36] E. Nieboer, D.H.S. Richardson, The replacement of the node-script term 'heavy metals' by a biological and chemically significant classification of metal ions, *Environ. Pollut. B* 1 (1980) 3–26.
- [37] S.V. Avery, J.M. Tobin, Mechanism of adsorption of hard and soft metal ions to *Saccharomyces cerevisiae* and influence of hard and soft anions, *Appl. Environ. Microbiol.* 59 (1993) 2851–2856.
- [38] O. Raize, Y. Argaman, S. Yannai, Mechanisms of biosorption of different heavy metals by brown marine macroalgae, *Biotechnol. Bioeng.* 87 (2004) 451–458.
- [39] M.J. Brady, J.M. Tobin, Binding of hard and soft metal ions to *Rhizopus arrhizus* biomass, *Enzyme Microb. Technol.* 17 (1994) 791–796.
- [40] C. Chen, J. Wang, Correlating metal ionic characteristics with biosorption capacity using QSAR model, *Chemosphere* 69 (2007) 1610–1616.
- [41] E. Nieboer, W.A.E. McBryde, Free-energy relationships in coordination chemistry. III. A comprehensive index to complex stability, *Can. J. Chem.* 51 (1973) 2512–2524.
- [42] J. Bayo, Kinetic studies for Cd(II) biosorption from treated urban effluents by native grapefruit biomass (*Citrus paradisi* L.): The competitive effect of Pb(II), Cu(II) and Ni(II), *Chem. Eng. J.* 191 (2012) 278–287.
- [43] A. Saeed, M.W. Akhtar, M. Iqbal, Affinity relationship of heavy metal biosorption by the husk of *Cicer arietinum* (Chickpea var. black gram) with their atomic weights and structural features, *Fresenius Environ. Bull.* 14 (2005) 219–223.
- [44] J.M. Tobin, D.G. Cooper, R.J. Neufeld, Uptake of metal ions by *Rhizopus arrhizus* biomass, *Appl. Environ. Microbiol.* 47 (1984) 821–824.
- [45] A.R.C. Padeste, H.R. Oswald, The influence of transition metals on the thermal decomposition of calcium carbonate in hydrogen, *Mater. Res. Bull.* 25 (1990) 1299–1350.
- [46] L. Zhirong, A. Uddin, S. Zhanxue, FT-IR and XRD analysis of natural Na-bentonite and Cu(II)-loaded Na-bentonite, *Spectrochim. Acta A Mol. Biomol. Spectrosc.* 79 (2011) 1013–1016.
- [47] W.J. Liu, F.X. Zeng, H. Jiang, X.S. Zhang, Adsorption of lead (Pb) from aqueous solution with *Typha angustifolia* biomass modified by SOCl₂ activated EDTA, *Chem. Eng. J.* 170 (2011) 21–28.