



## Photocatalytic degradation of reactive red 3 andalachlor over uncalcined Fe–TiO<sub>2</sub> synthesized via hydrothermal method

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### ABSTRACT

In this work, Fe<sup>3+</sup> was used to modify TiO<sub>2</sub> to give improved performance under UV and visible light irradiation. The catalysts were prepared via a hydrothermal method without further calcination. Box–Behnken design was used to investigate the effects of hydrothermal temperature, hydrothermal time, and Fe content (wt%) on the photocatalytic performance of TiO<sub>2</sub>. Pollutants such as reactive red 3 (RR3) dye andalachlor were examined. The synthesized catalysts have been characterized by many techniques. Photodegradation of RR3 dye was performed under UV light irradiation whereas photodegradation ofalachlor was performed under both UV and visible light irradiation. In RR3 photodegradation, the effect hydrothermal settings for temperature and time were found significant and the highest removal percentages were 92 and 94% for 15 and 30 min UV irradiation, respectively. Inalachlor photodegradation, the effect of Fe-doping was found significant under both UV and visible light irradiation. The highest removal percentages were 49 and 82% for 15 and 30 min of UV light irradiation, respectively, and 51% for 60 min of visible light irradiation. Only anatase crystallite was found in catalysts with and without Fe. Energy band gaps decreased with increasing Fe contents. The crystallite sizes of catalysts with 0.10 wt% Fe<sup>3+</sup> content decreased with increasing hydrothermal time and temperature, while surface area increased. Energy-dispersive X-ray spectroscopy technique was able to detect nitrogen contents of about 10 wt% and X-ray absorption near edge structure was used to find the oxidation states of Fe<sup>3+</sup> and Fe<sup>3+/4+</sup> in Fe–TiO<sub>2</sub> as well.

*Keywords:* Alachlor; Box–Behnken design; Fe–TiO<sub>2</sub>; Photocatalysis; Dye

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## 1. Introduction

Titanium dioxide is a promising photocatalyst in wastewater treatment. Its excellent properties include photostability, self-cleaning ability, non-toxicity, and low cost [1,2]. It is commonly used in the industry as a commercial photocatalyst and has also been the subject of many researches that focus on the removal of organics in water [1,3]. However, there are a number of limitations to the use of this material in a wider scale than a laboratory setup [1].

The ability to generate electron–hole pairs that facilitate the photocatalytic process can be hindered by high recombination rates [4–6]. Recombination inhibits the movement of the photogenerated electron–hole pairs, rendering them useless and unable to participate in the photocatalytic reactions [7,8]. Light with energy higher than the energy band gap of  $\text{TiO}_2$ , i.e. UV light ( $\lambda = 365 \text{ nm}$ ), should be utilized in order to mobilize the photogenerated electron–hole pairs [2,6,8–13]. Thus, this limits the activity of  $\text{TiO}_2$  to photocatalysis under UV light irradiation, which only makes up a very small portion of solar light [2,8,14].

Metal doping on  $\text{TiO}_2$  has been introduced to address the limitation of its use under UV light irradiation only [2,4,8,15–18]. The addition of  $\text{Fe}^{3+}$  improves the photocatalytic activity of  $\text{TiO}_2$  [17,19–21]. First, it acts as electron traps by capturing the photogenerated electrons and prevents the recombination with the photogenerated holes and thus, decreases the recombination rate [19,22]. It also reduces the energy band gap, resulting in increased activity under light with longer wavelengths, i.e. visible light ( $\lambda > 400 \text{ nm}$ ) [5,19,22–24].

$\text{Fe-TiO}_2$  could remove an array of environmental pollutants from wastewater ranging from dyes to recalcitrant compounds [19,25]. The dark colors of dyes in wastewater have adverse effects since it is toxic to aquatic life, prevents sunlight penetration to the water, and is visible even in low concentrations [26,27]. On the other hand, colorless organic compounds, such as alachlor, also pose a similar threat. The wide usage of alachlor as an herbicide for agricultural crops makes it very easy for it to contaminate water resources [28,29]. It is also considered to be a high health hazard since it has been listed as a carcinogenic compound [28].

It is important to find a photocatalyst that is suitable in systems that do not only involve different light sources, i.e. UV and visible light irradiation, but also pollutants with different physical properties such as RR3 dye, which has a dark color, and alachlor, which is colorless. The application of modified  $\text{TiO}_2$

photocatalysts to such systems extends the understanding of its light-gathering capabilities and the effects of  $\text{Fe}^{3+}$  in its improvement.

Hydrothermal techniques for  $\text{Fe-TiO}_2$  synthesis usually report a single-step heat treatment, a subsequent drying step, and finally, a calcination step at temperatures of at least  $300^\circ\text{C}$ . Shorter hydrothermal time usually requires a higher hydrothermal temperature [20]. Consequently, for a lower hydrothermal temperature, a longer hydrothermal time would also be necessary [22]. Both studies were able to produce photocatalysts that are composed of anatase  $\text{TiO}_2$ . Finding a suitable hydrothermal treatment that will promote anatase  $\text{TiO}_2$  even with the omission of the calcination step will make the synthesis less energy intensive and will also reduce power consumption and costs. In addition, the hydrothermal method produces  $\text{TiO}_2$  catalyst with high crystallinity and controlled particle size [30]. In a previous work, it was found that  $\text{TiO}_2$  prepared via hydrothermal method gave an energy band gap lower than  $3.0 \text{ eV}$  even though it has anatase crystallite phase [30].

In this study,  $\text{Fe-TiO}_2$  photocatalysts were synthesized by hydrothermal method without calcination. Box–Behnken Design (BBD) generated using Minitab 16.0 (Minitab, Inc., Pennsylvania, USA) was used to investigate the effects of hydrothermal temperature and time and Fe content (wt%) on the photocatalytic performance. Removal of reactive red 3 dye was done under UV light irradiation only, whereas alachlor photodegradation was performed under UV and visible light irradiation.

## 2. Materials and methods

### 2.1. Materials

Titanium tetrachloride ( $\text{TiCl}_4$ , 99%) from Merck Schuchardt OHG was used as the titanium dioxide catalyst precursor and 1,000 ppm Iron for atomic absorption standard as the dopant. Pure reactive red 3 (RR3,  $\text{C}_{25}\text{H}_{15}\text{ClN}_7\text{Na}_3\text{O}_{10}\text{S}_3$ ) solid obtained from the textile industry was used to prepare a 1,000-ppm stock solution. Synthetic alachlor PESTANAL analytical standard (99.2%) was dissolved in HPLC grade distilled water from RCI Labscan Limited to prepare a 100-ppm stock solution. Hydrogen peroxide ( $\text{H}_2\text{O}_2$ , 30%) and ammonia solution ( $\text{NH}_4\text{OH}$ , 28%) were purchased from Ajax Finechem Pty Ltd and QRéc, respectively. Isocratic grade acetonitrile ( $\text{CH}_3\text{CN}$ , 99%) and methanol ( $\text{CH}_3\text{OH}$ , 99%) were purchased from Merck and RCI Labscan Limited, respectively.

## 2.2. Catalyst synthesis

The catalyst preparation followed previous works [18,30]. A solution of  $\text{TiCl}_4$  dissolved in 400 mL cold deionized water was stirred for 30 min before the dropwise introduction of  $\text{NH}_4\text{OH}$  (90 mL). A white suspension resulted and this was stirred for another 30 min in an ice bath before it was centrifuged and decanted. Washing of the precipitates was done several times with deionized water until the pH of the washing becomes neutral. The precipitates were dried at  $40^\circ\text{C}$  for 16 h and the obtained solid  $\text{Ti}(\text{OH})_4$  or amorphous  $\text{TiO}_2$  was ground into fine powders manually.

Amorphous  $\text{TiO}_2$  was dissolved in 30 mL  $\text{H}_2\text{O}_2$  and this solution was stirred for 30 min in an ice bath.  $\text{H}_2\text{O}_2$  (90 mL) was introduced dropwise into the solution. For the 0.10% and 0.20 wt% Fe- $\text{TiO}_2$  samples, 0.42 and 0.84 mL 1,000-ppm  $\text{Fe}^{3+}$  solution were added into the solution, respectively. The solution was continuously stirred for 4 h until it became transparent yellow. Thereafter, it was transferred to a Teflon-lined steel autoclave and was subjected to different hydrothermal temperature and time settings. The solution from the autoclave was filtered and dried as follows: (1)  $40^\circ\text{C}$  for 2 h, (2)  $100^\circ\text{C}$  for 4 h, and (3)  $250^\circ\text{C}$  for 4 h.

## 2.3. Catalyst characterizations

X-ray diffraction analysis (XRD Model D8 Discover, Bruker AXS, Germany) was performed on Fe- $\text{TiO}_2$  catalysts to confirm the transformation of  $\text{TiO}_2$  into the crystalline anatase phase. The following conditions were used: Cu  $K\alpha$  radiation at  $\lambda = 0.15406$  nm, 40 kV potential, and 40 mA current. Scanning was done at a step of  $1^\circ \text{step}^{-1}$  from  $2\theta$  of  $20^\circ$  to  $70^\circ$ . Energy-dispersive X-ray spectroscopy (Oxford instrument, EDS7640, UK) was used on the pure  $\text{TiO}_2$  photocatalyst. A UV-vis spectrophotometer (Specord 200 Plus, AnalytikJena, Germany) was used for the diffuse reflectance spectroscopy (UV-DRS) measurements, with  $\text{BaSO}_4$  as the reflectance sample. X-ray absorption near edge structure (XANES) spectra were obtained for the Fe- $\text{TiO}_2$  samples using BL5.2: SUT-NANOTEC-SLRI XAS Beamline of Synchrotron Light Research Institute, Thailand. Brunauer-Emmett-Teller (BET) analysis (NOVA 1200e, Quantachrome, USA) was used to measure the specific surface areas of the photocatalysts.

Analysis of the remaining reactive red 3 dye concentrations was done using a UV-vis spectrophotometer (Specord 200 Plus, AnalytikJena) at 354 nm. On the other hand, analysis of the remainingalachlor concen-

trations was done using high-pressure liquid chromatography (Waters e2695 HPLC, Harlow Scientific, USA) at 197 nm, with a mixture of 40% methanol and 60% acetonitrile as the mobile phase at a flow rate of  $1.0 \text{ mL min}^{-1}$ . Injection volume was 20  $\mu\text{L}$ . The separation was performed by a Hypersil C18 ODS  $4.0 \times 125 \text{ mm } 5 \mu\text{m}$  column.

## 2.4. Catalyst activity measurements

The effects of hydrothermal temperature, hydrothermal time, and Fe content (wt%) during catalyst synthesis on RR3 removal was investigated using BBD (Table 1) created by using Minitab 16 (Minitab, Inc., Pennsylvania, USA). Initial RR3/alachlor concentration was set to 20 ppm, initial solution pH was adjusted to 4 using 1.0 M  $\text{HNO}_3$ , and catalyst loading was set to  $1 \text{ g L}^{-1}$  or 0.05 g per 50 mL. The suspensions were stirred at 500 rpm in the dark for the first 30 min to achieve equilibrium conditions. Afterwards, the suspensions were irradiated with UV light using three 20-W UVA lamps (Philips). The UVA light intensity was  $0.335 \text{ mW cm}^{-2}$ . Five-mL samples were collected after 15 and 30 min of reaction. Each sample was filtered using  $0.45 \mu\text{m}$  nylon filter (Whatman) prior to chemical analysis. Additionally, photodegradation ofalachlor was performed under visible light irradiation from three 22-W fluorescent lamps (Philips) for 60 min using the same amount catalyst and solution volume.

## 3. Results and discussion

The removal percentages of RR3 andalachlor after photocatalysis are shown in Table 2. In UV photocatalysis (30 min), the highest RR3 removal was 94% and the lowest was 76%. The highest and lowestalachlor removal under UV light irradiation (30 min) were 82 and 45%, respectively. On the other hand, under visible light irradiation (60 min), the highest and lowestalachlor removal were 51 and 15%, respectively. Thealachlor removal percentages are lower than RR3

Table 1  
Design of experiments for reactive red 3 dye/alachlor removal using Fe- $\text{TiO}_2$  catalysts

Factors	Symbol	Levels		
		-1	0	+1
Hydrothermal temperature ( $^\circ\text{C}$ )	$X_1$	150	175	200
Hydrothermal time (h)	$X_2$	8	16	24
Fe content (wt%)	$X_2$	0	0.10	0.20

Table 2  
RR3 andalachlor removal under UV and visible light using Fe–TiO<sub>2</sub> photocatalysts

Run	Hydrothermal temperature (°C)	Hydrothermal time (h)	Fe content (wt%)	RR3 removal (%)		Alachlor removal (%)		
				UV		UV		VIS
				15 min	30 min	15 min	30 min	60 min
1	150	8	0.1	89.40	93.44	22.15	48.49	28.24
2	175	16	0.1	70.62	85.95	29.75	49.70	19.00
3	175	16	0.1	76.42	89.88	21.55	47.21	20.39
4	200	8	0.1	82.39	90.44	24.58	44.94	28.97
5	175	16	0.1	83.46	91.30	21.99	48.22	24.98
6	150	24	0.1	73.38	90.02	22.66	46.90	16.85
7	150	16	0.2	89.12	94.10	21.65	46.44	20.25
8	175	8	0.0	71.37	89.19	48.92	75.74	33.98
9	175	8	0.2	91.92	93.37	22.84	45.07	21.28
10	200	16	0.2	77.66	83.81	21.62	48.56	14.91
11	200	16	0.0	66.16	93.51	46.71	82.43	51.02
12	150	16	0.0	85.29	88.33	44.38	70.62	19.79
13	175	24	0.2	75.45	81.11	33.59	48.33	17.64
14	200	24	0.1	70.30	76.31	26.47	52.68	22.86
15	175	24	0.0	79.07	85.70	30.39	55.17	19.40

removal percentages under UV light. This signifies thatalachlor removal does not proceed as easily as color removal. Moreover,alachlor removal under visible light irradiation is significantly lower than RR3 andalachlor removal under UV light irradiation.

The estimated regression coefficients of full quadratic equations were calculated by least-square of error technique and displayed in Table 3 of RR3 andalachlor removal experiments. Then, the mathematical models for RR3 andalachlor removal are given in Eqs. (1)–(3):

$$Y_1 = 89.04 - 2.73X_1 - 4.16X_2 - 0.54X_3 - 2.68X_1X_2 - 3.87X_1X_3 - 2.19X_2X_3 + 0.55X_1^2 - 2.04X_2^2 + 0.34X_3^2 \quad (1)$$

$$Y_2 = 48.38 + 2.02X_1 - 1.40X_2 - 11.95X_3 + 2.33X_1X_2 - 2.42X_1X_3 + 5.96X_2X_3 + 2.91X_1^2 - 3.03X_2^2 + 10.73X_3^2 \quad (2)$$

$$Y_3 = 21.46 + 4.08X_1 - 4.47X_2 - 6.26X_3 + 1.32X_1X_2 - 9.14X_1X_3 + 2.74X_2X_3 + 3.10X_1^2 - 0.32X_2^2 + 1.94X_3^2 \quad (3)$$

where  $Y_1$  is the percentage of RR3 removal under UV light irradiation (30 min);  $Y_2$  and  $Y_3$  are the percentages ofalachlor removal under UV (30 min) and visible light (60 min) irradiation;  $X_1$ ,  $X_2$ , and  $X_3$  are the

coded values of hydrothermal temperature, hydrothermal time, and Fe content, respectively;  $X_1X_2$  is the interaction between hydrothermal temperature and hydrothermal time;  $X_1X_3$  is the interaction between hydrothermal temperature and Fe content;  $X_2X_3$  is the interaction between hydrothermal time and Fe content; and  $X_1^2$ ,  $X_2^2$ , and  $X_3^2$  are the quadratic terms for each of the main factors, respectively.

Table 4 shows the significant results of the ANOVA for the BBD on RR3 andalachlor removal. In RR3 removal under UV light, the response surface methodology (RSM) model generated is significant ( $R^2 = 0.91$ ) and the lack-of-fit error is not significant. In Eq. (1), all of the main factors have negative coefficients indicating that increasing their levels would decrease RR3 removal (Table 3). The coefficients for the interactions also have negative values. The effects of hydrothermal time,  $X_2$ , and  $X_2^2$ , have the largest absolute value of coefficients and thus, the largest influence on the equation (Table 3). At 95% confidence, ANOVA results (Table 4) for RR3 removal under UV light (30 min) determined that the RSM model is also significant ( $R^2 = 0.9299$ ) whereas the lack-of-fit error is not significant according to  $F_{LOF} < F_{critical}$  ( $F_{critical(0.05,2,3)} = 9.55$ ). The main effects of hydrothermal temperature and hydrothermal time are significant on RR3 removal ( $F_{value} > F_{critical}$  ( $F_{critical(0.05,1,5)} = 6.61$ ), while Fe content is not significant.

Alachlor removal under UV light (30 min) results, the main effect of Fe content onalachlor removal

Table 3

Estimated regression coefficients ( $\beta$ ) for RR3 andalachlor removal using Fe–TiO<sub>2</sub> photocatalysts

Parameters	Coefficients	<i>p</i> -value	
(a) Estimated regression coefficients ( $\beta$ ) for RR3 removal under UV light for 30 min			
Constant	89.04	0.000	Significant
<i>A</i> —hydrothermal temperature	−2.73	0.032	Significant
<i>B</i> —hydrothermal time	−4.16	0.006	Significant
<i>C</i> —Fe content	−0.54	0.583	Insignificant
<i>A</i> <sup>2</sup>	0.55	0.702	Insignificant
<i>B</i> <sup>2</sup>	−2.04	0.193	Insignificant
<i>C</i> <sup>2</sup>	0.34	0.811	Insignificant
<i>AB</i>	−2.68	0.096	Insignificant
<i>AC</i>	−3.87	0.032	Significant
<i>BC</i>	−2.19	0.154	Insignificant
(b) Estimated regression coefficients ( $\beta$ ) foralachlor removal under UV light for 30 min			
Constant	48.38	0.000	Significant
<i>A</i> —hydrothermal temperature	2.02	0.332	Insignificant
<i>B</i> —hydrothermal time	−1.40	0.492	Insignificant
<i>C</i> —Fe content	−11.95	0.001	Significant
<i>A</i> <sup>2</sup>	2.91	0.342	Insignificant
<i>B</i> <sup>2</sup>	−3.03	0.324	Insignificant
<i>C</i> <sup>2</sup>	10.73	0.012	Significant
<i>AB</i>	2.33	0.421	Insignificant
<i>AC</i>	−2.42	0.405	Insignificant
<i>BC</i>	5.96	0.075	Insignificant
(c) Estimated regression coefficients ( $\beta$ ) foralachlor removal under visible light for 60 min			
Constant	21.46	0.001	Significant
<i>A</i> —hydrothermal temperature	4.08	0.066	Insignificant
<i>B</i> —hydrothermal time	−4.47	0.051	Significant
<i>C</i> —Fe content	−6.26	0.016	Significant
<i>A</i> <sup>2</sup>	3.10	0.282	Insignificant
<i>B</i> <sup>2</sup>	−0.32	0.905	Insignificant
<i>C</i> <sup>2</sup>	1.94	0.484	Insignificant
<i>AB</i>	1.32	0.615	Insignificant
<i>AC</i>	−9.14	0.014	Significant
<i>BC</i>	2.74	0.318	Insignificant

under UV light can be clearly seen in the relatively large negative coefficient of  $X_3$  (−11.95), as well as in the large coefficient of its quadratic term,  $X_3^2$  (10.73) as shown in Eq. (2). Fe content is significant in negative effect, while hydrothermal temperature and hydrothermal time are insignificant effects and the only hydrothermal temperature effect with a positive coefficient. The effect of hydrothermal temperature and the interaction effects have relatively small coefficients when compared to the coefficients assigned to the effect of Fe content. Although, the lack-of-fit error is significant ( $F_{LOF} = 29.41$ ) according to  $F_{LOF} > F_{Critical}$  ( $F_{critical(0.05,2,3)} = 9.55$ ) at 95% confidence, the quadratic model generated is significant ( $R^2 = 0.93$ ). Thus, the full quadratic equation can be used to predict the experimental results.

The quadratic equation foralachlor removal under visible light (60 min) is significant ( $R^2 = 0.90$ ) and the ANOVA (Table 4) shows that the lack-of-fit error is not significant according to  $F_{LOF} < F_{Critical}$  ( $F_{critical(0.05,2,3)}$ ) at 95% confidence. In Eq. (3), the main effects of hydrothermal time and Fe content as well as the interaction between hydrothermal temperature and Fe content all have negative coefficients. Although hydrothermal temperature effect is insignificant at 95% confidence ( $p$ -value = 0.066), this effect is very close to the value of significant term ( $p$ -value = 0.05). Thus, we can conclude that all variables of main effects show significantly onalachlor removal under visible light at 60 min of reaction time. The interaction between hydrothermal temperature and Fe content has the highest coefficient and was already observed to have a significant effect.

Table 4  
ANOVA for RR3 andalachlor removal using Fe–TiO<sub>2</sub> photocatalysts

Source	df	Sum of squares	Mean square	F-value	p-value	
(a) RR3 removal under UV light for 30 min						
Regression	9	326.244	36.249	5.31	0.040	Significant
A—hydrothermal temperature	1	59.514	59.514	8.72	0.032	Significant
B—hydrothermal time	1	138.611	138.611	20.30	0.006	Significant
C—Fe content	1	2.354	2.354	0.34	0.583	Insignificant
A <sup>2</sup>	1	1.125	1.125	0.16	0.702	Insignificant
B <sup>2</sup>	1	15.410	15.410	2.26	0.193	Insignificant
C <sup>2</sup>	1	0.432	0.432	0.06	0.811	Insignificant
AB	1	28.676	28.676	4.20	0.096	Insignificant
AC	1	59.830	59.830	8.76	0.032	Significant
BC	1	19.228	19.228	2.82	0.154	Insignificant
Lack-of-fit	3	18.774	6.258	0.81	0.592	Insignificant
(b) Alachlor removal under UV light for 30 min						
Regression	9	1,878.20	208.69	7.36	0.020	Significant
A—hydrothermal temperature	1	32.64	32.64	1.15	0.322	Insignificant
B—hydrothermal time	1	15.57	15.57	0.55	0.492	Insignificant
C—Fe content	1	1,141.54	1,141.54	40.28	0.001	Significant
A <sup>2</sup>	1	31.17	31.17	1.10	0.342	Insignificant
B <sup>2</sup>	1	33.89	33.89	1.20	0.324	Insignificant
C <sup>2</sup>	1	425.22	425.22	15.01	0.012	Significant
AB	1	21.76	21.76	0.77	0.421	Insignificant
AC	1	23.47	23.47	0.83	0.405	Insignificant
BC	1	141.97	141.97	5.01	0.075	Insignificant
Lack-of-fit	3	138.55	46.18	29.41	0.033	Significant
(c) Alachlor removal under visible light for 60 min						
Regression	9	1,025.56	1,025.56	4.68	0.052	Significant
A—hydrothermal temperature	1	133.09	133.09	5.47	0.066	Insignificant
B—hydrothermal time	1	159.49	159.49	6.56	0.051	Significant
C—Fe content	1	313.88	313.877	12.90	0.016	Significant
A <sup>2</sup>	1	35.58	35.58	1.45	0.282	Insignificant
B <sup>2</sup>	1	0.383	0.383	0.02	0.905	Insignificant
C <sup>2</sup>	1	425.22	425.22	15.01	0.012	Significant
AB	1	6.97	6.97	0.29	0.615	Insignificant
AC	1	334.34	334.34	13.17	0.014	Significant
BC	1	29.92	29.92	1.23	0.318	Insignificant
Lack-of-fit	3	102.03	34.011	3.47	0.232	Not significant

Both of the other interactions are positive but have smaller coefficients and were not found to be significant inalachlor removal under visible light.

Furthermore, optimization of the parameters were determined using BBD. The optimum conditions for RR3 removal under UV light irradiation were 150°C, 8 h, and 0.20 wt% Fe. Based on Eq. (1), low hydrothermal temperature and hydrothermal time settings are already known to be favored in this model and Fe content has a very small negative effect. On the other hand, the optimum conditions foralachlor removal are the same for UV and visible light irradiation, which are 200°C, 8 h, and 0 wt% Fe.

The effects of the main factors on RR3 andalachlor removal are shown in Fig. 1. In RR3 removal under UV light (Fig. 1(a)), all of the main factors have negative effects. The effects of hydrothermal temperature and hydrothermal time are significant and increasing these hydrothermal settings decreases RR3 removal under UV light. The effect of Fe content is not significant since the mean RR3 removal percentages were at a very small range for the three different amounts of Fe added.

The meanalachlor removal under UV light irradiation is lower than the mean RR3 removal. The meanalachlor removal under visible light irradiation is

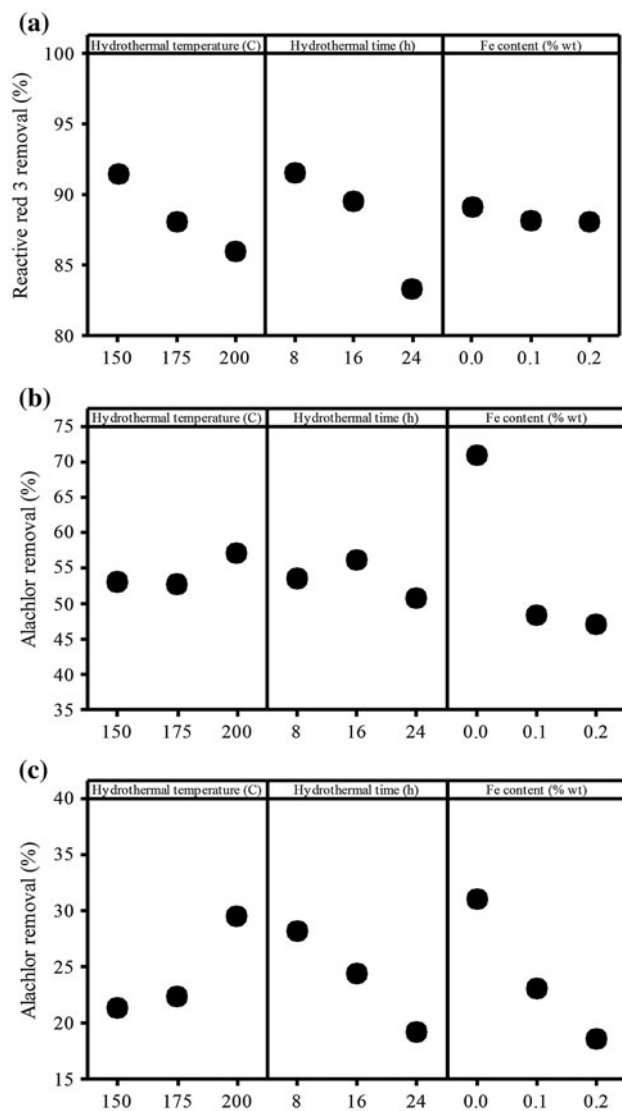


Fig. 1. Main effects for (a) RR3 removal under UV light andalachlor removal under, (b) UV light, and (c) visible light irradiation (initial RR3/Alachlor concentration: 20 ppm, pH 4.0 and catalyst loading  $1 \text{ g L}^{-1}$ ).

much lower than that under UV light irradiation. The main effects plots foralachlor removal under UV and visible light (Fig. 1(b) and (c)) show trends that are similar to each other but contrary to RR3 removal (Fig. 1(a)). The only significant effect inalachlor removal is the Fe content, in which the samples without Fe-doping gave the highest meanalachlor removal under UV and visible light irradiation, as also exhibited in Eqs. (2) and (3). Varying the hydrothermal temperature and time did not notably increase or decrease

alachlor removal whether under UV light or visible light irradiation.

In RR3 removal, only the interaction between the hydrothermal temperature and Fe content is significant. High RR3 removal was observed when the hydrothermal temperature was decreased and the Fe content is increased. Apart from this, the mean removal percentages almost do not vary greatly within the range of values in each interaction effect investigated. Fig. 2(a)–(c) show the contour plots for this interaction. The results of these two plots show that the highest RR3 removal can be observed when the Fe content is 0.20 wt% and the hydrothermal temperature used was 150°C. This affirms the importance of Fe doping that although the main effect of Fe content is insignificant, doping with 0.20 wt% does not reduce the removal efficiency.

From ANOVA (Table 4), none of the interaction effects are significant inalachlor removal under UV light irradiation (at 95% confidence). Following the obtained optimum conditions, fixing the Fe content to 0 wt%, the highestalachlor removal is observed when the hydrothermal temperature is 200°C and when the hydrothermal time is 8 h.

Similar to RR3 removal in UV and visible light, the interaction between hydrothermal temperature and Fe content is significant inalachlor removal under visible light. From Fig. 2(b) and (c), the highestalachlor removal was achieved when the hydrothermal temperature is at 200°C and the Fe content is at 0 wt% which is the exact opposite of the preferred interaction in RR3 removal.

These findings are supported by the results of the characterization techniques. The XRD patterns of Fe–TiO<sub>2</sub> photocatalysts are shown in Fig. 3, comparing the effects of hydrothermal temperature, hydrothermal time, and Fe content. The characteristic peaks of anatase TiO<sub>2</sub> at the  $2\theta$  positions of 25°, 38°, 48°, 55°, 56°, and 63° are found in all samples. This confirms that anatase TiO<sub>2</sub> has been produced via the hydrothermal treatment without calcination. Anatase TiO<sub>2</sub> is the component of the catalyst that is responsible for its photocatalytic activity. No Fe-containing peaks have been detected since the doping was done in small amounts [16]. Fe-doping also has no effect on the degree of crystallinity since there is no change in the sharpness of the main peaks of anatase for the samples with 0% and 0.20 wt% Fe.

The crystallite sizes of the photocatalysts were calculated using Scherrer's equation based on the XRD patterns. For catalysts synthesized at hydrothermal time of 8 h and 0 wt% Fe, an increase in the hydrothermal temperature from 150 to 200°C resulted in an increase (21%) in crystallite size from 10.53 nm

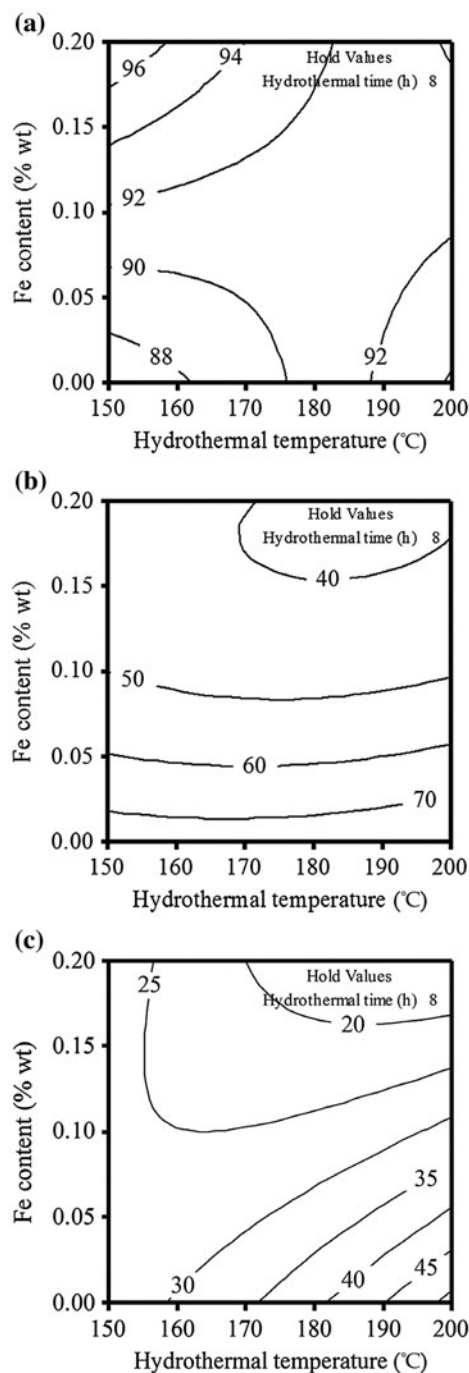


Fig. 2. Contour plots for the interaction hydrothermal temperature and Fe content on RR3 dye and alachlor removal at 8 h of hydrothermal time (initial RR3/Alachlor concentration: 20 ppm, pH 4.0 and catalyst loading  $1 \text{ g L}^{-1}$ ).

to 12.74 nm, which then translates to an increase in particle size. The increase in crystallite size brought about by the increase in hydrothermal temperature enhanced RR3 and alachlor removal. At hydrothermal

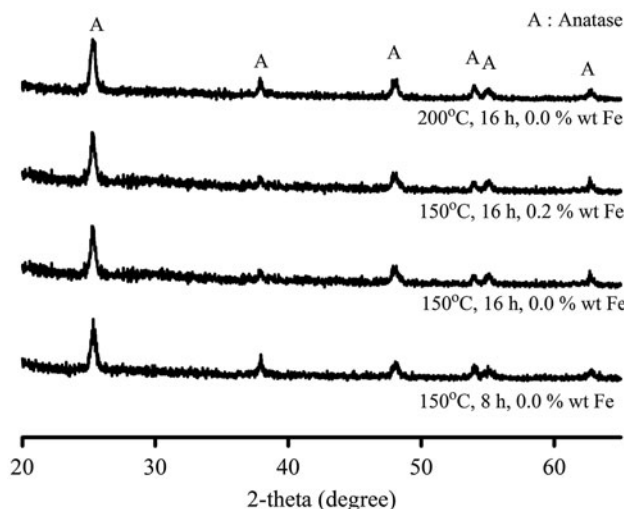


Fig. 3. XRD patterns of Fe-TiO<sub>2</sub> photocatalysts. This samples show only anatase crystallite phase.

time of 8 h and 0 wt% Fe, increasing the hydrothermal temperature from 150 to 200°C increased RR3 removal (UV light) from 88 to 94%; alachlor removal (UV light) from 71 to 82%; and alachlor (visible light) from 20 to 51%.

The crystallite size of TiO<sub>2</sub> is directly related to its particle size. BET surface area is known to be indirectly proportional to crystallite size [31]. For samples with 0.1 wt% Fe at hydrothermal time of 8 h, increasing the hydrothermal temperature from 150 to 200°C increased the BET surface area from 67.26 to 74.62  $\text{m}^2 \text{g}^{-1}$ . Thus, this also translates to a decrease in crystallite size. In UV photocatalysis, increasing the hydrothermal temperature from 150 to 200°C decreased RR3 removal from 93 to 90% and alachlor removal from 48 to 45%. Alachlor removal under visible light irradiation did not significantly change from 28 to 29%.

Increasing the hydrothermal time from 8 to 16 h resulted in a decrease (15%) in crystallite size from 12.15 to 10.53 nm for catalysts synthesized at a hydrothermal temperature of 150°C and with 0 wt% Fe. On the other hand, at the hydrothermal temperature of 150°C and Fe content of 0.1 wt% Fe, increasing the hydrothermal time from 8 to 24 h increased the BET surface area from 67.26 to 87.87  $\text{m}^2 \text{g}^{-1}$ , which also corresponds to a decrease in crystallite size. In UV photocatalysis, RR3 removal decreased from 93 to 90% while alachlor removal decreased from 48 to 47%. Alachlor removal under visible light irradiation also decreased from 28 to 17%.

A decrease in crystallite size that corresponds to the increase in BET surface area brought about by



increasing the hydrothermal temperature from 150 to 200 °C and the hydrothermal time from 8 to 24 h is observed in samples containing 0.1 wt% Fe. The atomic size of Fe ( $r = 0.64 \text{ \AA}$ ) is very similar to that of Ti ( $r = 0.68 \text{ \AA}$ ) [32]. Thus, its insertion into the crystal lattice of  $\text{TiO}_2$  did not cause any major alterations in the structure that will decrease the crystallinity. The slightly smaller atomic size of Fe may have caused a slight decrease in the effective crystallite size of the Fe– $\text{TiO}_2$  photocatalysts. The insertion of  $\text{Fe}^{3+}$  into the  $\text{Ti}^{4+}$  structure translates into defects which affected the crystallite growth [32].

In order to confirm the state of Fe-doping, XANES was used to determine the valence states in the photocatalysts as shown in Table 5. For different Fe– $\text{TiO}_2$  photocatalysts containing 0.20 wt% Fe, the different hydrothermal temperature and time settings resulted in a mixture of  $\text{Fe}^{3+}$  and  $\text{Fe}^{3+/4+}$  species. An increase in hydrothermal time from 8 to 16 h resulted in a major shift of the valence state from  $\text{Fe}^{3+}$  to a combination of  $\text{Fe}^{3+/4+}$ .  $\text{Fe}^{4+}$  is stable in the lattice of anatase  $\text{TiO}_2$ , which indicates that it can substitute the Ti atom easily. On the other hand, increasing the hydrothermal temperature from 150 to 175 °C only resulted in a slight decrease in the amount of  $\text{Fe}^{3+}$  species. In general, the majority of the measurements also denoted that there are no species in the  $\text{Fe}^{2+}$  state. The XANES results showing that the majority of the Fe species has a +3 valence state is further supported by the energy band gap measurements from the UV-DRS characterization. Kubelka-Munk theory was used to obtain the absorption spectra and energy band gap measurements. Pure  $\text{TiO}_2$  photocatalysts obtained in this study registered an energy band gap of 2.78 eV. Fe– $\text{TiO}_2$  doped with 0.10 wt% Fe also exhibited an energy band gap of 2.72 eV. This means that the doping amount was too small to significantly cause a change in the absorption properties of pure  $\text{TiO}_2$  synthesized by the same method. However, the addition of 0.20 wt% Fe decreased this value to 2.60 eV. This shift can only be attributed to the presence of  $\text{Fe}^{3+}$ , which was confirmed by the XANES measurements. Additionally, the measured energy band gaps for the synthesized

Fe– $\text{TiO}_2$  photocatalysts with 0.00, 0.10, and 0.20 wt% Fe in this study are about 2.78, 2.72, and 2.60, respectively, and significantly lower than the reported value of 3.20 eV for  $\text{TiO}_2$  in most studies. Although the decrease in energy band gap is expected for the Fe-doped  $\text{TiO}_2$  as ascribed to the red shift phenomenon [16,30], the measured energy band gap for the undoped  $\text{TiO}_2$  is still low enough to ensure its activity even in visible light photocatalysis. From a previous work [30], pure  $\text{TiO}_2$  prepared by same technique has shown the energy band gap lower than 3.00 eV. The energy-dispersive X-ray results of the pure  $\text{TiO}_2$  photocatalyst have Ti, O, and N as the main elements at about 51.19, 38.78, and 10.03 wt%, respectively. According to another research [33], the preparation of amorphous  $\text{TiO}_2$  in alkaline conditions by precipitation using  $\text{NH}_3\text{OH}$  resulted with N as an impurity in the amorphous  $\text{TiO}_2$ . It is also well known that N is one of the non-metal dopants that decrease the energy band of  $\text{TiO}_2$  [34,35]. Thus, it can be concluded that nitrogen doping is one of the major causes of the red shift of the energy band gap.

From the characterization techniques, it was confirmed that the  $\text{Fe}^{3+}$  and N present in the photocatalysts decreased the energy band gap and thus, increased the absorption in visible light. However, alachlor removal under both UV and visible light irradiation favored  $\text{TiO}_2$  than Fe-doped  $\text{TiO}_2$ . In this case, the decreased activity may be due to the behavior of  $\text{Fe}^{3+}$  as traps for the photogenerated electron–hole pairs. Instead of discretely trapping the electrons and the holes, the traps themselves may have become the recombination centers [18]. This was not observed in the experiments in RR3 color removal under UV light irradiation, wherein the optimum condition for Fe content is 0.20 wt% Fe. Dye sensitization also occurs under UV light irradiation in which the dye molecules of RR3 are able to supply excess electrons to the system that enhances the photocatalytic activity [18]. Another reason for the higher activity of Fe– $\text{TiO}_2$  with 0.20 wt% Fe in RR3 removal under UV light irradiation is the basis of RR3 removal percentages is only the decolorization as measured by spectrophotometry.

Table 5  
XANES measurements of the valence states of Fe in Fe– $\text{TiO}_2$  photocatalysts

Catalyst		Valence state	
Hydrothermal temperature (°C)	Hydrothermal time (h)	$\text{Fe}^{3+}$	$\text{Fe}^{3+/4+}$
150	8	75.3	24.7
150	16	8.6	91.4
175	8	66.8	33.2

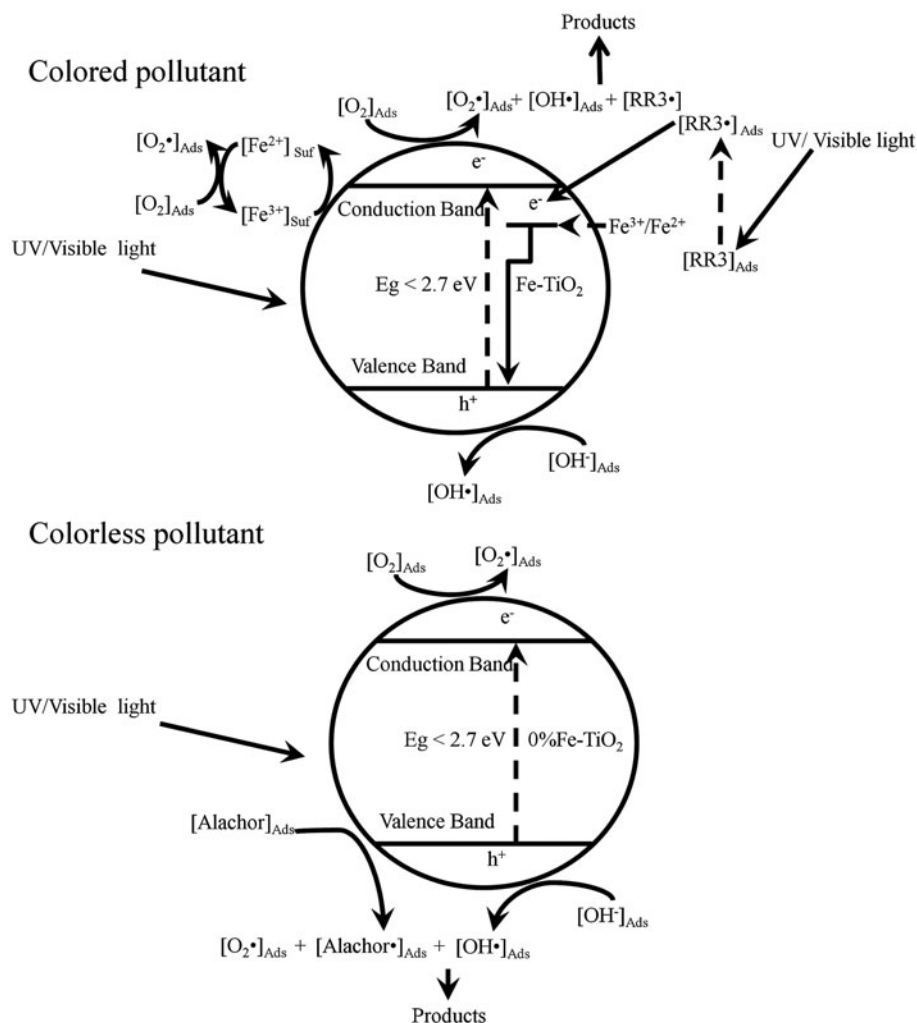


Fig. 4. Mechanisms of RR3 and alachlor degradation over Fe–TiO<sub>2</sub> photocatalysts under UV–vis light irradiation.

RR3 is also an organic molecule like alachlor. Alachlor degradation was reported in terms of the remaining amounts in solution as measured by the HPLC. The breakdown of the organic molecule of RR3 was not taken into account and thus decolorization gave higher removal rates than the alachlor removal. Therefore, the enhancement of TiO<sub>2</sub> by Fe doping was only observed in reactive red 3 dye removal under UV photocatalysis. Such effect was not significantly detected in the alachlor removal experiments under both UV and visible light irradiation. Even so, the undoped TiO<sub>2</sub> photocatalysts are already active under visible light irradiation and can remove up to 51.02% alachlor from the solution after 60 min. Regardless of the Fe-doping, the energy band gap of the pure TiO<sub>2</sub> is already lower than the reported value in literature of 3.20 eV, which explains its activity in both UV and visible light regions.

The mechanisms for the photodegradation of RR3 and alachlor under UV light irradiation can be explained in different mechanisms, depending on the amount of Fe doped on TiO<sub>2</sub>. The electrons in the TiO<sub>2</sub> valence band can be excited by light energy and move to conduction band. The mechanisms of RR3 photodegradation include four pathways, as shown in Fig. 4. Path 1 shows electrons form RR3• radicals, excited by light irradiation to RR3, which moved to Fe<sup>3+</sup>. Similar to a photosensitization process, the electrons moved to the valence band of TiO<sub>2</sub> to react with the holes to decrease the electron–hole pair recombination of TiO<sub>2</sub> according to castro and coworkers providing this mechanism in their work [19]. Path 2 shows OH<sup>−</sup> on the surface of TiO<sub>2</sub> reacting with the holes and forming hydroxyl radicals (•OH). The •OH radical then reacted with adsorbed RR3 to degrade it to smaller molecules as explained in the authors's previous

works [16]. Path 3 shows electrons in the conduction band reacting with the surface-adsorbed  $O_2$  molecules to yield  $O_2^-$  radicals. Consequently, the  $O_2^-$  radicals reacted with adsorbed RR3 to break its molecules. Path 4 shows the  $Fe^{3+}$  on the surface of  $TiO_2$  being excited (photosensitization) and bringing about efficient charge transfer in the composite samples. The  $Fe^{3+}$  particles could also act as electron traps as explained in our previous work [16]. These could reduce electron recombination in the catalyst matrix by becoming  $Fe^{2+}$  species. Since  $Fe^{2+}$  is unstable, it would rapidly transfer an electron into the  $O_2$  molecules to yield more  $O_2^-$  radicals. Therefore, the photocatalytic activity of  $TiO_2$  doped with Fe could be improved greatly for RR3 dye, which is a colored pollutant in agreement with many researches [9,15,19,36]. On the other hand, the mechanisms of alachlor photodegradation included only two pathways that are the same with that of RR3 in paths 2 and 3, as shown in Fig. 4. The colorless pollutant photodegradation under UV light irradiation cannot be enhanced efficiently by Fe-doping in  $TiO_2$  as was also reported by other researchers [19,37].

#### 4. Conclusions

Fe- $TiO_2$  catalysts were synthesized via hydrothermal method without calcination. Photocatalytic degradation of reactive red 3 dye was carried out under UV light irradiation whereas alachlor photodegradation was carried out under UV and visible light irradiation. Under UV light irradiation, the highest removal percentages for reactive red 3 dye were 92 and 94% for 15 and 30 min, respectively. In UV photocatalysis of RR3 dye for 30 min, the significant main effects are the hydrothermal temperature and time and the interaction between hydrothermal temperature and Fe content. The obtained optimum conditions are 150 °C, 8 h, and 0.20 wt% Fe. Photodegradation of alachlor under UV light irradiation for 15 and 30 min gave removal percentages of 49 and 82%, respectively. Visible light photocatalysis for 60 min removed up to 51% of alachlor in the solution. Only Fe content is the significant main effect in both experiments, wherein alachlor removal is highest when Fe content is 0. Under UV and visible light photocatalysis, the optimum conditions are 200 °C, 8 h, and 0.00 wt% Fe.

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