



## Effects of nitrate on the UV photolysis of H<sub>2</sub>O<sub>2</sub> for 2,4-dichlorophenol degradation in treated effluents

K.B. Ko<sup>a\*</sup>, J.Y. Lee<sup>a</sup>, Y.H. Yoon<sup>a</sup>, T.H. Moon<sup>a</sup>, Y.H. Ahn<sup>a</sup>, C.G. Park<sup>a</sup>, K.S. Min<sup>b</sup>, J.H. Park<sup>a</sup>

<sup>a</sup>School of Civil and Environmental Engineering, Yonsei University, 134 Shinchondong, Seoul, 120-749, Korea

Tel. +82 2 2123 2892; Fax: +82 2 364 5300; email: kbko@yonsei.ac.kr

<sup>b</sup>Department of Environmental Engineering, Kyungpook National University, 1370 Sanguykdong, Daegu, 702-701, Korea

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### ABSTRACT

The major objective of this study was to delineate the effect of nitrate on the UV oxidation of 2,4-DCP by conducting a bench-scale operation at various reaction times, and initial concentrations of H<sub>2</sub>O<sub>2</sub> and NO<sub>3</sub><sup>-</sup>. 2,4-DCP (20±5 µg/L) was oxidized in very limited amounts through direct UV photolysis, without additional oxidation by hydroxyl radicals. However, it was completely oxidized with an initial H<sub>2</sub>O<sub>2</sub> concentration of 20 mg/L at a reaction time of 1.0 min under the operating conditions described below. The practical reaction time for 80% oxidation turned out to be 2.0 min (with a high UV dose) with an initial H<sub>2</sub>O<sub>2</sub> concentration of 10 mg/L. Nitrate enhanced the 2,4-DCP oxidation by the hydroxyl radicals produced from nitrate photolysis with the relatively low initial H<sub>2</sub>O<sub>2</sub> concentrations of 0.0 to 5 mg/L, but hindered the oxidation, when an initial H<sub>2</sub>O<sub>2</sub> concentration in the reactor was less than or around about 10 mg/L. The adverse effect of nitrate on the 2,4-DCP oxidation was not observed with a relatively high initial H<sub>2</sub>O<sub>2</sub> concentration of 20 mg/L at the reaction times of 1.0 to 2.0 min. The scavenging effect of nitrate on the 2,4-DCP oxidation was generally limited with the concentration ranges tested in this study.

**Keywords:** 2,4-dichlorophenol; UV oxidation; Nitrate; Nitrite; UV/H<sub>2</sub>O<sub>2</sub> process

### 1. Introduction

The UV oxidation process is being increasingly used to oxidize complex organic constituents in the treated effluents from domestic wastewater treatment plants, for water reuse. The UV oxidation process typically involves the generation and use of hydroxyl radicals, one of the most active oxidants known. Hydroxyl radicals, unlike other oxidants, are capable of oxidizing almost all the reduced materials present in treated effluents, without restriction to specific classes or groups of compounds [1]. The typical concentrations of NO<sub>3</sub><sup>-</sup>-N range from 3 to

5 mg/L in the biologically well-treated effluents. However, the nitrate ion, NO<sub>3</sub><sup>-</sup>, is a well-known strong absorber of UV light in the case of wavelengths generally below 250 nm [2,3]. NO<sub>2</sub><sup>-</sup> from NO<sub>3</sub><sup>-</sup> photolysis may hinder the degradative oxidation reactions of organic chemicals enhanced by hydroxyl radicals. Low-pressure, high-intensity UV lamps, manufactured in a mercury-indium amalgam, are continuously being developed. Studies should be conducted to investigate the adverse effects of nitrate on the UV oxidation of 2,4-dichlorophenol (2,4-DCP) using these new and efficient monochromatic lamps.

It is known that nitrate photolysis has three distinct mechanisms, which result in the formation of nitrite

\*Corresponding author.

( $\text{NO}_2^-$ ), peroxyxynitrite ( $\text{ONO}_2^-$ ), and nitrogen dioxide radical ( $\bullet\text{NO}_2$ ), respectively. One of these mechanisms is the direct route to  $\text{NO}_2^-$  formation from  $\text{NO}_3^-$  photolysis, with a low quantum yield [3,4]. A significant production of  $\text{NO}_2^-$  can be expected via the two other reactions which produce the intermediates  $\text{ONO}_2^-$  and  $\bullet\text{NO}_2$ , which in turn eventually undergo thermal reactions to form  $\text{NO}_2^-$  as a stable product [3,5]. The formation of hydroxyl radicals ( $\bullet\text{OH}$ ) can be also expected, together with one of the intermediates,  $\bullet\text{NO}_2$ , from nitrate photolysis. As  $\text{NO}_2^-$  accumulates, it can react with  $\bullet\text{OH}$ , and acts as an  $\bullet\text{OH}$  scavenger.

The mechanisms involving  $\text{H}_2\text{O}_2$  photolysis were also critically reviewed [6]. Hydrogen peroxide ( $\text{H}_2\text{O}_2$ ) also influences  $\text{NO}_2^-$  production. Since  $\text{H}_2\text{O}_2$  photolysis provides another source of hydroxyl radicals, it might be expected to decrease  $\text{NO}_2^-$  production.  $\text{H}_2\text{O}_2$ , however, appears to act in part as a scavenger of hydroxyl radicals. Peroxyxynitrite ions and their conjugate acid, peroxyxynitrous acid ( $\text{ONO}_2\text{H}$ ), are strong oxidants. Hydroxyl radicals are also produced from the decomposition of peroxyxynitrous acid. Nitrite and oxygen can be formed from the reaction between peroxyxynitrous acid and hydrogen peroxide [5,7,8]. The literature review conducted on the reactions related with the UV photolysis of hydrogen peroxide in the presence of nitrate revealed that both nitrate and hydrogen peroxide appear to act either as an  $\bullet\text{OH}$  producer or, at some time, as an  $\bullet\text{OH}$  scavenger, in an aqueous solution.

The UV photolysis or UV oxidation (i.e., photolysis of hydrogen peroxide in the  $\text{H}_2\text{O}_2/\text{UV}$  process) has recently been increasingly applied to the oxidation of trace organic chemicals found in water and treated water. These processes were studied for the removal of atrazine, trichloroethylene (TCE), methyl tertiary butyl ether (MTBE), 1,4-dioxane, pesticides, taste- and odor-causing compounds such as MIB and geosmin, N-nitrosodimethylamine (NDMA), and a variety of pharmaceuticals [1,9–15]. There was only one study, though, in which the effects of nitrate in an aqueous solution were systematically determined for the  $\text{H}_2\text{O}_2/\text{UV}$  process [16]. In their study, the UV oxidation for EDTA degradation was studied with wavelengths of 222 and 254 nm in  $\text{NO}_3^-$  solutions, in the presence and absence of  $\text{H}_2\text{O}_2$ . The effects of the  $\text{NO}_3^-$  concentrations 0, 10, 20, 50, and 100 mg/L were investigated where the  $\text{NO}_3^-$  concentration range studied was quite different from that in this study. Nitrate was reported to have caused a significant “inner filter” effect by reducing the absorption of UV by  $\text{H}_2\text{O}_2$ .

Studies have been conducted on the UV oxidation of 2,4-DCP dissolved in aqueous solutions [17–19]. However, no studies were conducted for the effect of nitrate on the UV oxidation of 2,4-DCP, especially dissolved in around or less than 20  $\mu\text{g}/\text{L}$ . The major objective of this study was

to delineate the effects of nitrate on the UV oxidation of 2,4-DCP by conducting a bench-scale operation at various reaction times, and initial concentrations of  $\text{H}_2\text{O}_2$  and  $\text{NO}_3^-$ -N. The identification of the intermediates from 2,4-DCP oxidation was not within the scope of this study.

## 2. Materials and methods

All the experiments were carried out in an 8.4 L jacketed brown-glass reactor equipped with a 3.6 L stainless-steel reaction chamber. The UV lamp in the chamber (Trojan Logic™ LF18), with a nominal power of 67 W, emitted radiation at 254 nm. The inner surfaces of all the tubes were made of Teflon, and all headspaces inside the reactors and tubes were completely eliminated during the experiments [20]. All the experiments were performed in batch mode, and the pHs in the reactors were not controlled.

The influent solution (12 L) to be poured into the reactor was prepared by dissolving 15 mL of the 2,4-DCP (99%, Sigma) stock solution (0.016 g 2,4-DCP/1 L methanol) and 0.362 g  $\text{NaNO}_3$  (98%, Shinyo) in 11 L of double-distilled water. The mixture was carefully poured in the reactor, and was circulated with the use of an installed peristaltic pump for 3 min, to completely mix the solution. Aliquots (342.83  $\mu\text{g}/\text{L}$ ) of  $\text{H}_2\text{O}_2$  (35%, Showa) were then injected into the mixture, and the reactor was filled with additional double-distilled water in order to avoid any headspace inside it (for an  $\text{H}_2\text{O}_2$  concentration of 10 mg/L as an example). This influent solution was completely mixed again with the use of the recirculation pump for the first min, without any UV irradiation, and the UV lamp in the chamber was then turned on to initiate oxidation reaction. Samples (40 mL) were regularly collected according to the pre-determined schedule, and were analyzed for 2,4-DCP using the solid phase micro-extraction process [21]. The concentrations of 2,4-DCP were measured by using GC/MS (Varian Saturn 2000 Ver. 6.41) equipped with a PTE-5, 30 m  $\times$  0.25 mm ID, 0.25  $\mu\text{m}$  film column. The flow rate of the carrier gas (helium) was set 40 cm/s at 40 °C. The injector temperature was 280 °C. The oven temperature was initially set to 40 °C and kept up to 260 °C at 12 °C/min [22].

## 3. Results and discussion

As shown in Fig. 1(a), 2,4-DCP was rapidly degraded for the first 0.5 min of UV exposure, and was completely oxidized at a reaction time of 1 min with nitrate addition and without it. It is noted that this complete degradation was observed with a relatively high initial  $\text{H}_2\text{O}_2$  concentration of 20 mg/L in the reactor. The adverse effect of  $\text{NO}_3^-$  on 2,4-DCP degradation could not clearly be

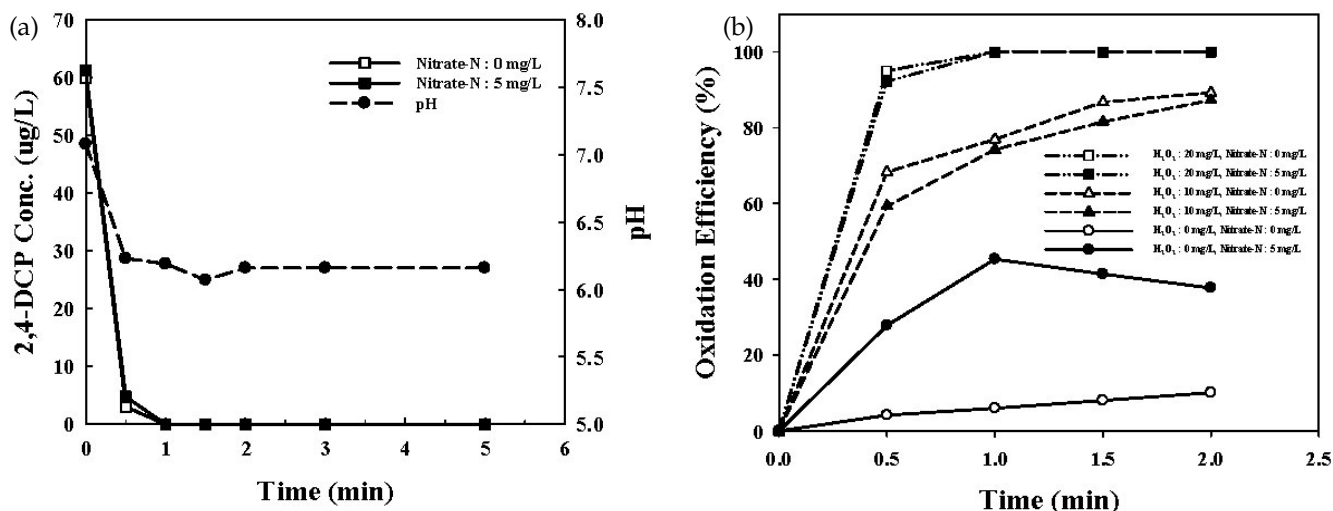
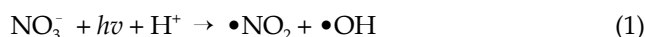


Fig. 1. (a) Profiles of 2,4-DCP concentration and pH (in the absence of nitrate) as functions of reaction time with respect to different initial conc. of NO<sub>3</sub><sup>-</sup>-N; initial conc. of 2,4-DCP: 64 µg/L, initial conc. of H<sub>2</sub>O<sub>2</sub>: 20 mg/L. (b) Profiles of oxidation efficiencies (%) of 2,4-DCP as functions of reaction time with respect to different initial conc. of H<sub>2</sub>O<sub>2</sub> and NO<sub>3</sub><sup>-</sup>-N; initial conc. of 2,4-DCP: 20±5 µg/L.

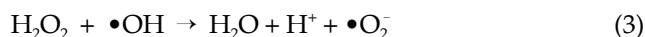
shown under this operating conditions. The pH slightly decreased and ranged from 7.08 to 6.16 in the absence of nitrate. The overall pattern of pH decrease in the presence of nitrate showed trends very similar to that in the absence of it [not shown in Fig. 1(a)]. The pH ranged from 6.41 to 6.07 with the initial NO<sub>3</sub><sup>-</sup>-N concentration of 5 mg/L. Fig. 1(b) shows the profiles of oxidation efficiencies (%) of 2,4-DCP as functions of reaction time with respect to different initial concentrations of H<sub>2</sub>O<sub>2</sub> and NO<sub>3</sub><sup>-</sup> at an initial 2,4-DCP concentration of 20 ± 5 µg/L. The removal of 2,4-DCP was generally rapid for the first 1 min of UV oxidation and gradually increased after that. It also shows that 2,4-DCP was degraded by UV irradiation in the reactor without adding H<sub>2</sub>O<sub>2</sub> and NO<sub>3</sub><sup>-</sup>. The removal efficiencies in the absence of H<sub>2</sub>O<sub>2</sub> and NO<sub>3</sub><sup>-</sup> were only about 6% at a 1 min reaction time and about 10% at a 2 min reaction time. This indicates that 2,4-DCP can be oxidized in very limited amounts through direct UV photolysis, without additional oxidation by hydroxyl radicals

It is quite interesting to compare the oxidation in the two reactors, into which H<sub>2</sub>O<sub>2</sub> was not supplied. NO<sub>3</sub><sup>-</sup>, however, was added into the one reactor as an initial NO<sub>3</sub><sup>-</sup>-N concentration of 5 mg/L, and no NO<sub>3</sub><sup>-</sup> was added into the other reactor [Fig. 1(b)]. The oxidation efficiencies in the reactor where NO<sub>3</sub><sup>-</sup> was present were higher than those in the reactor where NO<sub>3</sub><sup>-</sup> was absent, possibly due to the oxidation of 2,4-DCP by hydroxyl radicals. NO<sub>3</sub><sup>-</sup> can be attributed to the OH radical production from the NO<sub>3</sub><sup>-</sup> absorption of UV [8], even when no H<sub>2</sub>O<sub>2</sub> dissolved in the solution was present in the reactors. The results indicate that NO<sub>3</sub><sup>-</sup> clearly has enhanced the 2,4-DCP oxidation

through the following nitrate photolysis [2,3,9]:



The adverse effect of nitrate on the oxidation of 2,4-DCP was clearly shown when the oxidation efficiencies in one reactor where nitrate was added were compared with those in the reactor where nitrate was not added. The initial H<sub>2</sub>O<sub>2</sub> concentration was 10 mg/L for both reactors [Fig. 1(b)]. The differences in oxidation efficiencies caused by NO<sub>3</sub><sup>-</sup> in the reactor were relatively small, and ranged only about 2 to 9%. This might be because the photolysis of NO<sub>3</sub><sup>-</sup> produced NO<sub>2</sub><sup>-</sup> ions which were accumulated during the reaction, as mentioned above [2,9]. The observed oxidation efficiencies consequently decreased due to OH radical scavenging by photochemically generated NO<sub>2</sub><sup>-</sup>, as shown in the following chemical reactions [5]. NO<sub>3</sub><sup>-</sup> was also reported to have caused a significant “inner filter” effect by reducing the absorption of UV by H<sub>2</sub>O<sub>2</sub>, which resulted in a significant reduction in the efficiency of UV/H<sub>2</sub>O<sub>2</sub> system [2]:



The differences in the oxidation efficiencies caused by NO<sub>3</sub><sup>-</sup> were a little larger in the reactor at the initial H<sub>2</sub>O<sub>2</sub> concentration of 10 mg/L than those at the initial H<sub>2</sub>O<sub>2</sub> concentration of 20 mg/L, as the NO<sub>3</sub><sup>-</sup> photolysis and scavenging hydroxyl radicals by nitrite ions were rather limited at this high H<sub>2</sub>O<sub>2</sub> concentration. The adverse effect

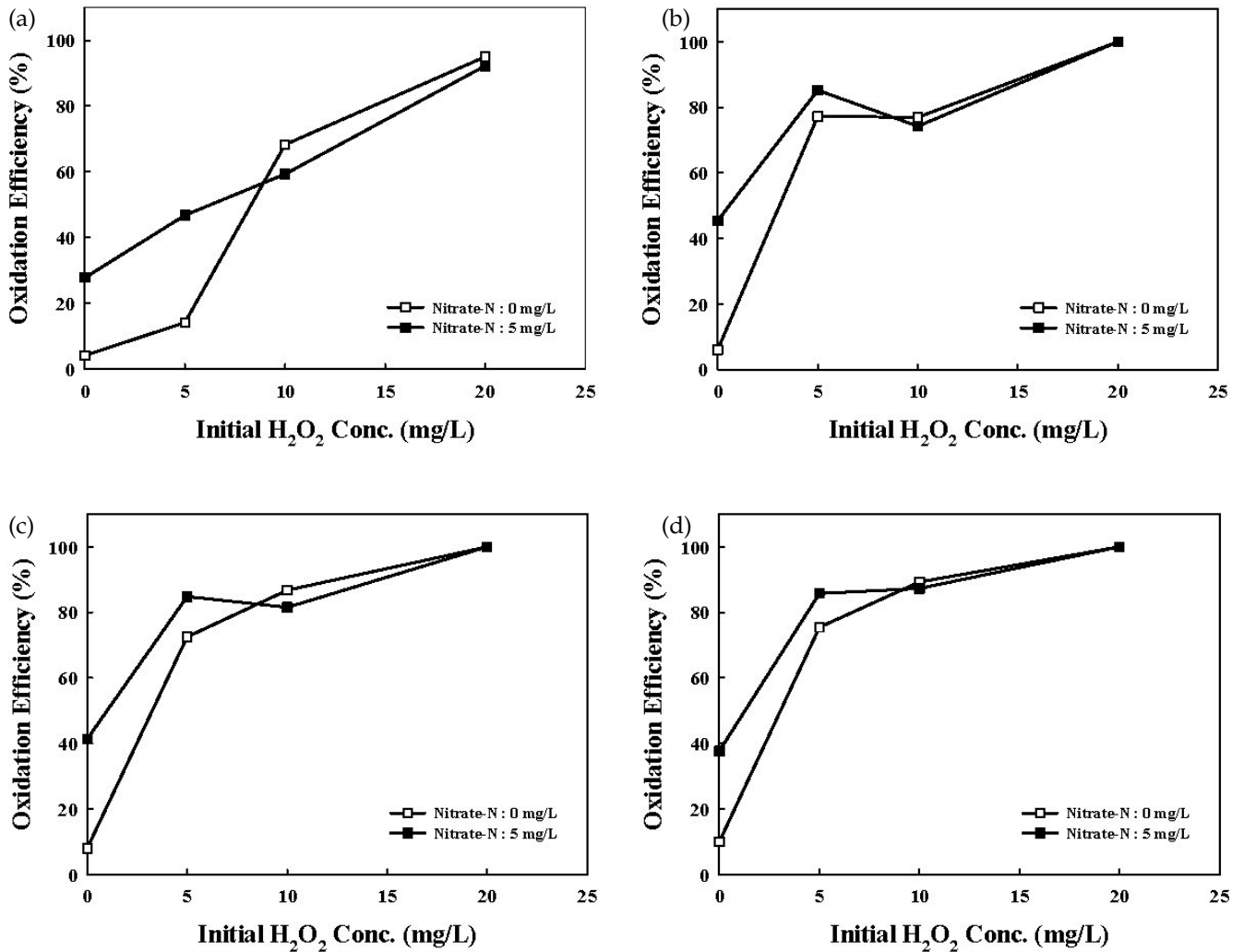


Fig. 2. Oxidation efficiencies (%) of 2,4-DCP as functions of initial conc. of H<sub>2</sub>O<sub>2</sub> with respect to the different initial conc. of NO<sub>3</sub><sup>-</sup>-N at the reaction times of (a) 0.5 min, (b) 1.0 min, (c) 1.5 min, and (d) 2.0 min. Initial conc. of 2,4-DCP: 20±5 µg/L.

was clearly reduced at the short reaction time of 0.5 min, and disappeared at the long reaction times of 1.0, 1.5 and 2.0 min with the initial H<sub>2</sub>O<sub>2</sub> concentration of 20 mg/L. The results indicate that 2,4-DCP can be completely oxidized with an initial H<sub>2</sub>O<sub>2</sub> concentration of 20 mg/L at a reaction time of 1.0 min under the operating conditions described above. It is noted that the 0.5, 1.0, 1.5 and 2.0 min of UV exposure accounted for 238, 477, 715 and 954 mJ/cm<sup>2</sup> as an UV dose, respectively, considering the reaction times and UV intensities applied under the operating conditions described above.

The effects of the reaction times on the 2,4-DCP degradation are shown in Fig. 2. The oxidation of 2,4-DCP was not limited by nitrate with the initial H<sub>2</sub>O<sub>2</sub> concentrations of 0.0 and 5 mg/L at any reaction time, and was rather enhanced by nitrate in the reactors. The 2,4-DCP oxidation was hindered in very limited amounts with the initial H<sub>2</sub>O<sub>2</sub> concentrations of 10 mg/L at all

reaction times, but was not hindered with the initial H<sub>2</sub>O<sub>2</sub> concentrations of 20 mg/L at the relatively long reaction times of 1.0, 1.5 and 2.0 min, except at the short reaction time of 0.5 min. It is interesting that the oxidation efficiencies with the initial H<sub>2</sub>O<sub>2</sub> concentrations of 5 mg/L was rather higher than those with the initial H<sub>2</sub>O<sub>2</sub> concentrations of 10 mg/L at the reaction time of 1 min. The results show that the practical reaction time for the 80% oxidation turned out to be 2.0 min with an initial H<sub>2</sub>O<sub>2</sub> concentration of 10 mg/L. However, when a reaction time of 1 min is considered for 2,4-DCP oxidation, the desirable initial H<sub>2</sub>O<sub>2</sub> concentration can be 5 mg/L rather than 10 mg/L in the reactor for high removal efficiency.

Fig. 3 shows that the UV photolysis of H<sub>2</sub>O<sub>2</sub> was the most effective method for 2,4-DCP degradation among the three options considered for this study, as the scavenging effect of nitrate ion on the 2,4-DCP oxidation was rather limited with the concentration ranges tested in this study.

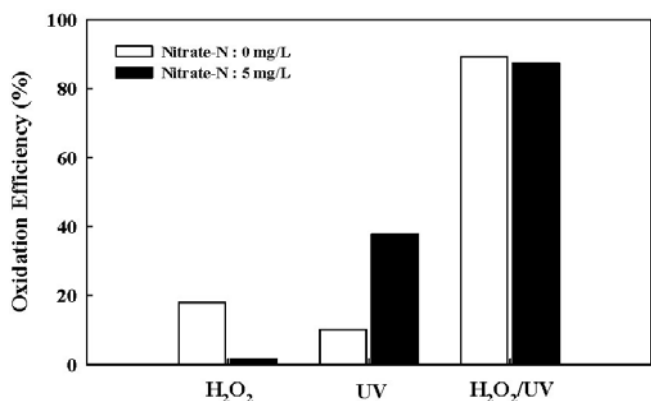


Fig. 3. Profile of removal efficiencies (%) of 2,4-DCP with respect to the different initial concentration of  $\text{NO}_3^-$ -N with the initial  $\text{H}_2\text{O}_2$  concentration of 10 mg/L and at the reaction time of 2 min;  $\text{H}_2\text{O}_2$ :  $\text{H}_2\text{O}_2$  addition without UV irradiation, UV: UV irradiation without  $\text{H}_2\text{O}_2$  addition, and  $\text{H}_2\text{O}_2$ /UV: UV oxidation; initial concentration of 2,4-DCP:  $20 \pm 5$   $\mu\text{g/L}$ .

It is noted that 18% oxidation of 2,4-DCP, initiated by  $\text{H}_2\text{O}_2$  alone in the solution, was observed without any UV irradiation under the operating conditions. The reason for this relatively high oxidation is, so far, unknown, even if hydrogen peroxide itself is one of the strong oxidants. This might be possible because  $\text{H}_3\text{O}^+$ , produced from the reaction of  $\text{H}_2\text{O}_2$  with  $\text{H}_2\text{O}$ , caused the additional 2,4-DCP oxidation. The oxidation efficiencies in the reactor where  $\text{NO}_3^-$  was present were higher than those in the reactor where  $\text{NO}_3^-$  was absent, possibly due to the oxidation of 2,4-DCP by hydroxyl radicals.  $\text{NO}_3^-$  could be attributed to the OH radical production from the  $\text{NO}_3^-$  absorption of UV, even when no dissolved  $\text{H}_2\text{O}_2$  in the solution was present in the reactors, previously discussed above.

#### 4. Conclusions

It was found that 2,4-DCP ( $20 \pm 5$   $\mu\text{g/L}$ ) was oxidized in very limited amounts through the direct UV photolysis, without additional oxidation by hydroxyl radicals. However, it was completely oxidized with an initial  $\text{H}_2\text{O}_2$  concentration of 20 mg/L at a reaction time of 1.0 min under the operating conditions described above. The practical reaction time for the 80% oxidation turned out to be 2.0 min (with a high UV dose) with an initial  $\text{H}_2\text{O}_2$  concentration of 10 mg/L. Nitrate enhanced the 2,4-DCP oxidation by the hydroxyl radicals produced from nitrate photolysis with the relatively low initial  $\text{H}_2\text{O}_2$  concentration of 0.0 to 5 mg/L, but hindered the UV oxidation when the initial  $\text{H}_2\text{O}_2$  concentration in the reactor was less than or around about 10 mg/L. The 2,4-DCP oxidation was not clearly hindered by nitrate with a relatively high initial  $\text{H}_2\text{O}_2$  concentration of 20 mg/L at the long reaction

times of 1.0 to 2.0 min. The scavenging effect of nitrate on the 2,4-DCP oxidation was generally limited with the concentration ranges tested in this study. It is noted that about 18% oxidation of 2,4-DCP, initiated by  $\text{H}_2\text{O}_2$  alone in the solution, was observed without any UV irradiation under the operating conditions. The reason for this relatively high oxidation should be further investigated, even if hydrogen peroxide itself is one of the strong oxidants. This may be possibly because  $\text{H}_3\text{O}^+$ , produced from the reaction of  $\text{H}_2\text{O}_2$  with  $\text{H}_2\text{O}$ , resulted in the additional 2,4-DCP oxidation.

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