

Synthesis and characterization of Dawson heteropolyanion $[H_3Fe][\alpha_2P_2MoW_{17}O_{62}]$: application on dye degradation

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ABSTRACT

An heteropolyanion compound consisting of saturated Dawson anions and trivalent iron cations, $\alpha_2H_3FeP_2W_{17}MoO_{62}$ has been synthesized and characterized by various spectroscopic methods, IR, UV-Vis, ³¹P NMR and ESI-MS. The catalytic performances of heteropolyanion were tested for degradation of aqueous Malachite Green dye under Fenton process. The degradation reaction was monitored by UV-visible and IR spectroscopy. The effects of different reaction parameters such as the initial pH of the medium, the initial hydrogen peroxide concentration, the catalyst mass, the initial MG concentration and the reaction temperature on the oxidative degradation of malachite green has been investigated. The optimal reacting conditions were found to be pH = 3, initial hydrogen peroxide was 0.31 M, and the catalyst mass was 0.03 g, for initial MG concentration of 20 mg.L⁻¹ at 30°C. After optimizing operating parameters, the dye was demineralized after 7 h of reaction.

Keywords: Heteropolyanion; Synthesis; Characterization; Catalysis; dye; Degradation; Wastewater treatment

1. Introduction

Environmental pollutants, such as synthetic dyes, have been a threat to our society. These substances are recalcitrant molecules, toxic to microorganisms and are liable to affect the hormonal system without inducing direct toxicological risks on human beings and wildlife. Due to their good solubility, synthetic dyes are common water pollutants and are frequently found in industrial wastewater [1,2]. Particularly triphenylmethane dyes, Malachite green (MG), or C.I. Basic green 4, is a cationic dye used in different domains. Malachite green has been extensively used in textile industry for dyeing wool and silk, paper, and in leather industry [3–7]. Besides its industrial uses, has widely been used to prevent fungal infections in fish farms [8]. If discharged malachite green directly into streams, it will affect the aquatic lives and cause detrimental effects on the liver, gill, kidney, intestine, gonads and pituitary gonadotropic cell of casualty.

Advanced oxidation processes are an alternative promising compared to the traditional treatment processes of effluent. Removal of colour and recalcitrant organic content of textile effluent can be achieved with the high efficiencies. Costs

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of AOPs are another point of view. But, Fenton process seems to be viable choice for textile wastewater treatment [9,10]. Fenton reaction has attracted attention because of its simplicity, rapidity and highly efficiency in organic contaminant removal. If the concentrations of reactants are not limiting, the organic compounds can be completely mineralized. The classical Fenton reaction is based on the activation of hydrogen peroxide (H_2O_2) by aqueous ferrous iron (Fe(II)) under acidic conditions to from hydroxyl radicals, \cdot OH. Several studies have reported that other cations such as Fe³⁺, Cu²⁺, Mn²⁺, Co²⁺ can also mediate the Fenton reaction, these reactions are referred to as the "Fenton-like processes" [11,12].

Heteropolyanions (HPAs) are metal-oxo clusters, are stable and easily modified by incorporation of transition metal ions. This family of clusters has been widely applied in various fields, including catalysis [13–15] and electrocatalysis [16,17]. The heteropolyanions obtained with P constitute a rich family. Two main types of heteropolyanions are known, the type of Keggin $[PW_{12}O_{40}]^3$ and type of Dawson $[P_2W_{18}O_{62}]^{6-}$ (Fig. 1).

The ability to modify the redox and chemical properties of heteropolyanions by replacing and or introducing one or more elements renders them particularly interesting in catalysis.

In this work we report the synthesis, characterization and catalytic properties of a new heteropolyanion complex formed by introducing Fe (III) ion into the saturated 17-tungsto-1-molybdo-2-phosphate mixed heteropolyanion $[P_2MoW_{17}O_{62}]^6$.

The addition of ferric ions at the acid form was made by analogy to the compounds [(M (H₂O) ₄) x] [H_{6-2x}P₂W_{18-n}MoO₆₂] (M = Cu^{II}, Co^{II}, Ni^{II}) [18] and leads to the compound [H₃FeP₂MoW₁₇O₆₂], which is characterized by IR, UV, ³¹P NIMR.

The catalytic oxidation of malachite green in aqueous solution, in the presence of Dawson heteropolyanion $[H_6P_2W_{18}O_{62}]$, has been studied by photocatalytic process [19]. In this work, we have investigated the oxidation of malachite



Fig. 1. Structure of Dawson.

green by $[H_3FeP_2MoW_{17}O_{62}]$ Dawson heteropolyanion with Fenton catalytic process as well as the influence of operating parameters on the decolorization such as oxidant dosages; initial dye concentration, pH of solution, catalyst mass and temperature were determined to find optimum conditions for complete decolorization and total oxidation of dye solution.

2. Materials and methods

2.1. Synthesis of precursor heteropolyanions

The heteropolyanions $K_6P_2W_{18}O_{62}$, $\alpha_2K_{10}P_2W_{17}O_{61}$ and $\alpha_2 K_6P_2W_{17}MoO_{62}$ were synthesized according to the published procedures [20,21]. The structure and purity of $\alpha_2 K_6P_2W_{17}MoO_{62}$ were confirmed by infrared, ³¹P NMR and ESI mass spectroscopy. The acid form of mixed salt $\alpha_2K_6P_2$. $W_{17}MoO_{62}$ was prepared by extraction with ether.

2.2. Synthesis of $H_3FeP_2W_{17}MoO_{62}$ (HPAFe)

A 0.178 g (1.1 mmole) of FeCl₃ was dissolved in 20 mL of water at room temperature after stirring, 5 g (1.1 mmole) of $H_6P_2W_{17}MOO_{62}$.14H₂O was then added. The mixture was stirred for 10 min. Dark yellow crystals were obtained after 4 d by slow evaporation with yield 76%. UV-Visible: shoulder between 198 and 282 nm for [HPAFe] = 6.82×10^{-5} M.

2.3. Characterization of heteropolyanions

BET surface area measurement was performed at liquid nitrogen temperature using a Micrometrics ASAP 2020 apparatus. The sample was degassed at T = 80°C for 4 h.

The IR spectra were recorded on KBr pellets using a spectrophotometer shimadzu FTIR-8400s. The UV-visible spectra were recorded on spectrophotometer Jenway 6300 UV/visible in a quartz cell. ³¹P NMR spectra were recorded on Bruker 400 MHz Ascend. The ³¹P NMR shifts were measured for 10^{-3} M solution of heteropolyanions in D₂O solution and were referenced to 85% H₃PO₄. The ESI mass spectra were recorded in negative mode on microtof-Q II 10027 Bruker electro spray ionization mass spectrometer. The capillary high voltage was set to +3,000 V. The end voltage was set to -500 V.

2.4. Oxidation of malachite green (MG) dye

The dye, malachite green oxalate salt of chemical formula $C_{52}H_{56}N_4O_{12'}$ was purchased from Sigma-Aldrich without any purification. The structure of this dye is shown in Fig. 2 [22].



Fig. 2. Chemical structure of malachite green.

The oxidation of the dye with hydrogen peroxide (H_2O_2 , 30%) in the presence of heteropolyanion was performed as follows: A given quantity of heteropolyanion was added to 100 mL of malachite green solution (5 mg/L). After vigorous stirring in a thermostatic batch (25°C), the pH of the solution is adjusted with H_2SO_4 (0.1N) or NaOH (0.1N) before addition of the oxidant H_2O_2 . The concentrations of malachite green in solution were analysed with different time intervals.

The malachite green concentrations were analysed at the maximum wavelength (λ_{max} = 619 nm) with UV-Vis spectrophotometer. Hydrogen peroxide concentrations were determined using the iodometric method.

The degradation efficiency of malachite green was defined as follows:

$$E(\%) = [(C_i - C_i)/C_i] \times 100$$

where C_i (mg/L) is the initial concentration of malachite green, and C_f (mg/L) is the final dye concentration at reaction time *t* (min).

3. Results and discussion

3.1. Synthesis and characterization

The heteropolyanion $\alpha_2 K_6 P_2 W_{17} MoO_{62}$.nH₂O and the corresponding acid form were prepared as described in the literature [23]. $\alpha_2 K_6 P_2 W_{17} MoO_{62}$ heteropolyanion is saturated mixed specie derived from the Dawson structure; it was obtained by substitution of an apical tungsten with a molybdenum. The corresponding acid form is obtained by extraction with ether under acidic conditions. The addition of ferric ions at the acidic form of saturated 17-tungsto-1-molybdo-2-phosphate mixed heteropolyanion $[P_2 MoW_{17}O_{62}]^{6-}$ with 1/1 stoechiometric amounts led to the substitution of three protons. The compound obtained $\alpha_2 H_3 FeP_2 W_{17} MoO_{62}$.nH₂O was characterized with various spectroscopic methods.

The specific surface area of compound is $4.7105 \text{ m}^2/\text{g}$. The UV-Vis spectrum (Fig. 3) was recorded in aqueous solutions. The W (VI) and Mo(VI) ions have a d⁰ electronic



Fig. 3. U.V. spectrum of $[H_3Fe][\alpha_2P_2MoW_{17}O_{62}]$.

configuration. The spectrum of the compound show a band between 200 and 280 nm assigned to the π -d electronic transition in M-O terminal [24]. The wide band observed at 300 nm is assigned to electronic transitions in binding M-Ob-M (M = W, Mo) [24]. Gap energy Eg was determined from the UV-visible spectrum [25]. Plot of $(\epsilon h \upsilon)^2$ against h υ is shown in inset of Fig. 3. The extrapolated value of hn at $\epsilon = 0$ (ϵ is the absorption coefficient) gave an absorption edge energy at Eg = 3.5 eV.

The IR spectra of synthesized heteropolyanions have all characteristic bands of Dawson structure (Table 1) [26,27]. The IR spectrum of compound $\alpha_2H_3FeP_2W_{17}MoO_{62}$ shows a band at 1,092 cm⁻¹ attributed to the asymmetric vibration of the P-Oa bond. The bands located at 960, 914 and 783 cm⁻¹ assigned, respectively to asymmetric vibrations of M-O terminal groups and inter- and intra-M-O-M (M = W, Mo).

The phosphorus NMR spectroscopy is particularly suitable for checking the purity of heteropolyanions. ³¹P NMR spectrum of $\alpha_2 K_6 P_2 W_{17} MoO_{62}$ shows two peaks located at –12.23 and –13 ppm (Fig. 4(a)), indicating the two in equivalence phosphorus in this structure. These values are comparable to those observed by [20]. $\alpha_2 H_3 FeP_2 W_{17} MoO_{62}$ is a product with a single peak on the ³¹P NMR spectrum located –13.208 ppm (Fig. 4(b)). The second phosphorus resonance, near the ferric ion affected by its paramagnetism is radically shifted and broadened. This shift and broadening is enough important to make the corresponding signal unobserved [28,29].

The ESI mass spectrum of $\alpha_2 H_3 \text{FeP}_2 W_{17} \text{MoO}_{62}$ (Fig. 5) displays a base peak centered at m/z = 1,064.71 and another peak at m/z = 1,419.26. These peaks characterized by $\Delta(\text{m/z}) = 1/4$ and $\Delta(\text{m/z}) = 1/3$ were attributed to $(H_2 P_2 W_{17} \text{MoO}_{62})^-$ and $(H_3 P_2 W_{17} \text{MoO}_{62})^{-3}$, respectively.

3.2. Oxidation of malachite green (MG)

3.2.1. Effect of operating conditions on the degradation of malachite green

Several operating conditions affected the degradation of malachite green with H_2O_2/HPA system such as pH, concentration of malachite green, catalyst mass, reaction temperature and hydrogen peroxide concentration were investigated.

3.2.1.1. Effect of initial pH

The solution pH is one of the most important factors that control the degradation of malachite green. The effect of initial pH on the degradation of malachite green by hydrogen peroxide using $\alpha_2 H_3 FeP_2 W_{17} MoO_{62}$ as catalyst was determined at the initial dye solution of 5 mg/L, catalyst mass 0.01 g, initial hydrogen peroxide concentration of 0.08 M, and temperature of 25°C. Degradation experiments were performed at different pH values of 2.0, 3.0, 4.0, 6.0, 8.0 and 10.0 to evaluate the MG degradation efficiency of the catalytic oxidation process.

The effect of initial pH on the removal rate of the dissolved dye in the batch Fenton is shown in Fig. 6. The oxidation reaction of malachite green is quite important in acidic media (pH 2, 3, 4, 6) and particularly, faster at pH 3 with maximum degradation efficiency (78.48%) after 120 min.

Table 1I.R. bandes of heteropolyanions

Compound	I.R. bands (cm ⁻¹) v _{as} (P-O _a)	$v_{as}(W-O_d)$	$v_{as}(W-O_{b}-W)$	$v_{as}(W-O_{c}-W)$
$\alpha_2 P_2 W_{17} O_{61}$	1,086	959	914, 893	800
$\alpha_2 P_2 W_{17} MoO_{62}$	1,088	960	914	775
$\alpha_2 H_3 FeP_2 W_{17} MoO_{62}$	1,092	960	914	783



Fig.4. ³¹P NMR spectrum of heteropolyanions: $\alpha_2 K_6 P_2 W_{17} MoO_{62}$ (a), $\alpha_2 H_3 FeP_2 W_{17} MoO_{62}$ (b).

Further increase in the pH value from 6 to 10, the degradation efficiency decrease from 68.22% to 48.06%. This was due to that the number of hydroxyl radicals available for degradation of dye reduced when the pH value was greater than six, because, H_2O_2 was unstable in high alkaline solution, and partly decomposed to H_2O and O_2 [30]. Thus, the catalytic activity of HPA was apparently decreased when the solution pH was 10. The rate of degradation of the dye depends on the pH of the medium and the best pH for this reaction was obtained at 3.

3.2.1.2. Effect of $\alpha_2 H_3 FeP_2 W_{17} MoO_{62}$ mass

Catalyst mass can have a significant impact on the dye degradation. To evaluate the influence of $\alpha_2 H_3 FeP_2 W_{17} MoO_{62}$ mass on the degradation, a set of experiments were carried



Fig. 5. ESI Mass spectrum of $\alpha_2 H_3 FeP_2 W_{17} MoO_{62}$.



Fig. 6. Effect of initial pH on the degradation of malachite green during Fenton oxidation catalysed by α_2 H₃FeP₂W₁₇MoO₆₂ (Conditions: V_R =100 mL, [MG]₀ = 5 mg/L, m_{cat} = 0.01 g, *T* = 25°C, [H₂O₂] = 0.08 M).

out by varying the mass from 0 to 0.08 g at optimal pH value (pH = 3), the results are presented in Fig. 7.

The reaction of degradation without catalyst (m = 0 g) was produced with a low efficiency (13.70%) after 90 min, but a notable increase of efficiency (13.70% to 67.08%) was observed when the catalyst mass was increased from 0 to 0.005 g. The presence of α_2 H₃FeP₂W₁₇MoO₆₂ as catalyst significantly increased the degradation rate of malachite green. The presence of catalyst iron-substituted may increase oxidation activity by hydrogen peroxide which favors the formation of hydroxyl radical. The efficiency of degradation is substantially



Fig. 7. Effect of catalyst mass on the degradation of malachite green during Fenton oxidation catalysed by α_2 H₃FeP₂W₁₇MoO₆₂ (Conditions: V_R = 100 mL, [MG]₀ = 5 mg/L; pH = 3, T = 25°C, [H₂O₅] = 0.08 M).

similar from 0.01 to 0.03 g. However, the degradation efficiency increased less when catalyst mass addition was higher than 0.03 g. The highest efficiency (E = 79.80%) of dye degradation was observed for 0.03 g catalyst mass after 90 min.

3.2.1.3. Effect of initial concentration of hydrogen peroxide

The concentration of H_2O_2 is an important factor in the oxidation reaction by Fenton process. The effect of initial concentration of hydrogen peroxide on malachite green degradation was investigated at optimal parameters of pH and catalyst mass in the range of 0.032 to 0.40 M and the results are shown in Fig. 8.

As expected, the increase in initial [H₂O₂] accelerated the dye decolorization at the beginning of the reaction. The decoloration efficiency increased from 63.99% to 81.21% as a consequence of increasing H₂O₂ dosage from 0.032 to 0.31 M. this can be explained by the effect of ·OH radicals produced additionally. The addition of H₂O₂ is known to increase the rate of dye degradation by allowing an enhancement in the yield of formation of hydroxyl radical. On increasing concentration of hydrogen peroxide from 0.31 to 0.40 M, there is no significant variation in the color removal and the degradation efficiency was not significantly changed (81.21%-82.44%). This observation can be explained by deficiency of OH radicals in the reaction medium. Similar observations have been reported in other studies [31,32], the H₂O₂ became an extractor of hydroxyl radicals at high concentrations. Thus, increasing concentration of H₂O₂ does not increase the degradation efficiency. For this purpose, an intermediate concentration of 0.31 M in H₂O₂ is chosen for optimum concentration because more H2O2 cannot improve the degradation rate much more.

3.2.1.4. Effect of temperature

The increase in temperature accelerated the dye degradation at the beginning of the reaction (Fig. 9). It was observed that the degradation efficiency of malachite green increased



Fig. 8. Effect of initial H_2O_2 concentration on the degradation of malachite green during Fenton oxidation catalysed by $\alpha_2H_3FeP_2W_{17}MoO_{62}$ (Conditions: V_R =100mL, [MG]₀=5mg/L;pH=3, m_{crt} = 0.03 g, *T* = 25°C).



Fig. 9. Effect of temperature on the degradation of malachite green during Fenton oxidation catalysed by α_2 H₃FeP₂W₁₇MoO₆₂ (Conditions: V_R = 100 mL, [MG]₀ = 5 mg/L; pH = 3, m_{cat} = 0.03 g, [H₂O₅] = 0.31M).

from 70.17% to 78.71% as a consequence of increasing the temperature from 30°C to 50°C within the first 30 min of oxidation process. This is because higher temperature increased the reaction rate between hydrogen peroxide and catalyst, thus increasing the rate of generation of oxidizing species such as OH radicals [22]. After a reaction time of 50 min, the increase in the degradation efficiencies of MG (79.97, 78.34 and 78.71) is only marginal on increasing the temperature (30, 40 and 50). Therefore, the temperature 30°C is selected for further study.

3.2.1.5. Effect of initial malachite green concentration

The effect of initial malachite green concentration on the oxidation reaction at the optimized operating parameters (pH, catalyst mass, $[H_2O_2]$ and temperature) was studied by varying its concentration in the range of 3–50 mg/L (Fig. 10).



Fig. 10. Effect of initial dye concentration on the degradation of malachite green during Fenton oxidation catalysed by $\alpha_2 H_3 \text{FeP}_2 W_{17} \text{MoO}_{62}$ (Conditions: $V_R = 100 \text{ mL}$, pH = 3, $m_{cat} = 0.03 \text{ g}$, [H₂O₃] = 0.31M, $T = 30^{\circ}$ C).

The efficiency of catalytic degradation increased with increasing initial concentration of malachite green from 3 to 20 mg/L (73.66%–93.45%) after 120 min. This phenomenon was due to the effectiveness of hydroxyl radicals produced by the used catalytic system. But a notable decrease (93.45%–90.99%) could be found when the initial concentration was increased from 20 to 50 mg/L. This is probably due to the weakness of available hydrogen peroxide quantities and the degradation of malachite green slowed down significantly. Therefore, the best initial malachite green concentration 20 mg/L.

3.3. Products of malachite green identified by UV-Visible and IR analysis

3.3.1. UV-Visible analysis

UV-Visible spectral analysis of malachite green before degradation and after 80 min of decolorization reaction is presented in Fig. 11. The spectrum showed the disappearance of bands located at 629 and 425 nm relative to the electronic transitions in the C = C and C = N bonds, respectively [32]. Therefore, the conjugated system has been interrupted by breakdown of C = C and C = N bonds. TLC check, with different eluent (CHCl₃ CH₂Cl₂) confirmed the occurrence of two species of significantly different polarities.

The spectrum presented in Fig. 11, also showed the appearance of three bands between 300 and 200 nm. This interval is specific to electronic transitions π - π * and n- π * in unsaturated molecules and the carbonyl derivatives [33].

3.3.2. IR analysis

To identify species produced by the degradation of the malachite green, an IR spectrum was performed (Fig. 12) in the dichloromethane. The spectrum of malachite green after 120 min of oxidation revealed the appearance of two bands at 1,010 and 1,090 cm⁻¹ which can be attributed to the vibrations of C-O bonds of the alcohol function [34] and a band



Fig. 11. U.V. spectra of Malachite green before and after 2 h of MG oxidation.



Fig. 12. I.R spectrum of malachite green before (A) and after 2 h (B) of MG oxidation.

at 1,200 cm⁻¹ is attributed to stretching vibration of the C-N bond. Two bands located at 1,419 and 1,650 cm⁻¹ are related to the N-Ph and C = O bonds, respectively [34]. Several bands appeared in the range of 2,000–2,900 cm⁻¹ are attributed to vibrations of aromatic C-H bonds in the benzophenone [34]. The bands located at 3,500 and 3,690 cm⁻¹ are related to the vibrations of OH alcohols bonds.

From spectroscopic UV-visible and IR data, Fig. 13 show the products obtained after 2 h of green malachite oxidation.

The IR spectrum of the MG after 4 h of oxidation was very different from that recorded at 2 h of reaction, which revealed the progress of the oxidation reaction.

The IR spectrum of the malachite green after 4 h of oxidation presented bands located at 865.98, 894.91 and 938.27 cm⁻¹ relating to the vibration of angular deformation of the C-H bonds of the aromatic rings and the stretching vibrations are present at 3,055.03 cm⁻¹. The bands observed at 1,014.49 and 1,097.49 cm⁻¹ are attributed to C-O bonds of carboxylic acids. Two bands located at 1,369.37 and 1,398.30 cm⁻¹ are related to the vibration of N-C bonds of CH₃-N fragment. The band at 1,411.80 cm⁻¹ corresponds to the vibration of the N-Ph bond.

The C = O group of the carboxylic acid was present in these bands located at 1,751.24 and 1,757.03 cm⁻¹. The bands



Fig. 13. Products of 2 h of MG oxidation.



Fig. 14. Effect of the catalyst nature on the degradation of malachite green during Fenton oxidation catalysed by $\alpha_2 H_3 FeP_2 W_{17} MoO_{62'}$ FeSO₄/ Fe(NO₃)₂, FeCl₃ (Conditions: $V_R = 100$ mL, [MG]₀ = 5 mg/L; pH = 3, [Cat] = 0.1 mol/L, [H₂O₂] = 0.31 M, T = 30°C).

located at 2,964.39 and 2,985.60 cm⁻¹ are attributed to C-H bonds of CH₃-group. The C = C bonds of the aromatic rings are present in the spectrum by their bands of low intensity located at 1,560 and 1,600 cm⁻¹. The OH group of the carbox-ylic acid was present in the bands at 2,600 and 2,700 cm⁻¹.

After 6 h of oxidation reaction, the IR spectrum showed no bands related to aromatic rings, and there were only bands of very low intensity relating to C-O and C = O groups of the carboxylic acid and a band located at 2,918.10 cm⁻¹ was characteristic to C-H asymmetric vibration in alkyl group. Oxidation of MG was complete after 7 h of reaction where the IR spectrum in dichloromethane presented only bands thereof.

At the end of this study, we have compared the catalytic performance of the iron-substituted $\alpha_2 H_3 \text{FeP}_2 W_{17} \text{MoO}_{62}$ (HPAFe) catalyst with three different iron catalysts used in Fenton process (FeSO₄/ FeCl₃/ Fe (NO₃)₃). The results are shown in following Fig. 14.

The results showed that, the efficiency of catalytic degradation varied significantly with the nature of the catalyst. The yields obtained with different catalysts are ($E_{\rm HPAFe}$ = 82.32%; $E_{\rm FeSo_4}$ = 72.94%; $E_{\rm FeCl_3}$ = 55.16%; $E_{\rm Fe(NO_{3})_3}$ = 72.36%). The degradation of malachite green by hydrogen peroxide in the presence of heteropolyanion Dawson HPAFe was better than the other catalysts.

3.4. Catalytic mechanism of $H_3FeP_2W_{17}MoO_{62}$

It was reported that the presence of H_2O_2 ; with molybdates MoO_4^{2-} [35] or heteroppolyanions [36] lead to the formation of molybdenum (Mo) peroxo complex, $MoO_2(O_2)_2^{2-}$ or peroxo-HPA, which are a strong oxidants and can oxidize the organic compounds by the direct oxygen transfer or by the singlet oxygen (1O₂) generated from the peroxo-complex:

$$P_2 W_{17} MoO_{62}^{6-} + 2H_2 O_2 \rightarrow P_2 W_{17} MoO_{62} (O_2)_2^{6-} + 2H_2 O$$
(1)

$$P_2 W_{17} MoO_{62} (O_2)_2^{6-} \rightarrow P_2 W_{17} MoO_{62}^{6-} + 1O_2$$
(2)

$$1O_2 + Dye \rightarrow oxidized \text{ products}$$
 (3)

On the other hand, the Fe^{3+}/H_2O_2 system suggest the reduction of Fe^{3+} to Fe^{2+} . The formed Fe^{2+} then reacts with H_2O_2 to generate.OH radicals which are ready to degrade the organic compounds:

$$Fe^{3+} + H_2O_2 \rightarrow Fe^{2+} + OOH + H^+$$
(4)

$$Fe^{2+} + H_2O_2 \rightarrow \equiv Fe^{3+} + OH + OH^-$$
(5)

$$\cdot OH + Dye \rightarrow oxidized products$$
 (6)

4. Conclusions

This study mainly reports the synthesis and spectroscopic characterization of a Dawson heteropolyanion $\alpha_2H_3FeP_2W_{17}MoO_{62}$ and its use in one of the advanced oxidation process, process Fenton (H_2O_2/HPA) for degrading a pollutant, green malachite.

The degradation study of the dye was performed with the optimization of some reaction parameters; initial pH of solution, mass of catalyst, concentration of the oxidant, temperature and dye concentration in order to achieve demineralization. The catalytic activity results showed that the optimum conditions for the maximum catalytic.

Degradation of malachite green was obtained at initial solution pH of 3, a catalyst mass of 0.03 g, an initial hydrogen peroxide concentration of 0.31 mol/L, at temperature of 30° C and initial malachite green concentration of 20 mg/L. UV–Vis spectra showed the disappearance of C = C and C = N bonds after 80 min and IR spectra showed the destruction of aromatics rings after 6 h of reaction and the demineralization of dye was achieved after 7 h.

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