

The adsorption of Reactive Black 5 by nanowire-synthesized nano-manganese dioxide and nano-manganese oxyhydroxide in a natural nanoclay substrate: an adsorption kinetics and isotherm study

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ABSTRACT

The compounds nano-manganese oxyhydroxide (γ -MnOOH) and nano-manganese dioxide (β -MnO₂) and their composites with montmorillonite (γ -MnOOH/M and β -MnO₂/M) were used for the first time to adsorb and remove the residual Reactive Black 5 (RB5) dye from textile industrial wastewater. The synthesis of γ -MnOOH and β -MnO₂ through the hydrothermal method resulted in the nanowire morphology of these compounds. Two new composites were synthesized by the interaction of these compounds with natural nanoclay montmorillonite. These compounds were able to penetrate montmorillonite nanolayers and intercalate them. The synthesized compounds and composites were characterized using Fourier-transform infrared spectroscopy, X-ray diffraction and scanning electron microscopy. The capacity of the compounds and composites to adsorb the RB5 was investigated in an artificial industrial wastewater. Both compounds and their composites were able to adsorb the dye and the results indicated the dependence of the adsorption capacity on different parameters, including pH, contact time, adsorbent dosage, and dye concentration. As expected, the composites showed a higher dye removal efficiency than the compounds, and the most sufficient dye adsorption (70%) was detected in the composite β -MnO₂/M for a dye concentration of 500 mg L⁻¹. The reusability of β -MnO₂ was also demonstrated for an efficient adsorption. The adsorption kinetics of compounds and composites followed the pseudo-second-order kinetic and the rate constants (k_2) of the compounds were higher than those of the composites. The adsorption isotherms of γ -MnOOH and β -MnO₂ corresponded to the Langmuir and Freundlich isotherms, respectively, and the adsorption isotherms of their composites followed the Langmuir isotherm. This study shows that nano-manganese compounds and their composites are efficient adsorbents for the removal of RB5 dye from industrial wastewater.

Keywords: Manganese oxyhydroxide; Manganese dioxide; Montmorillonite; Adsorption; Dye removal

1. Introduction

Different industries, such as the textile, plastic, wool, paper, cotton, food, carpet, pharmaceutical, cosmetic and silk industries, use dyes on a large scale for several applications. The residual dye in industrial wastewater has a negative impact on ecosystems [1]. Researchers have therefore sought

to establish efficient procedures to remove the colored pollutants from wastewater to decrease its negative environmental effects. The textile industry has an extensive need for different dyes and is the main permanent consumer of color products [2] and thereby the main producer of colored wastewater.

Given their solubility, structure, and chemical properties, dyes are classified into different groups, such as reactive, direct, vat, basic, and acid dyes [1,3–6]. About 76% of the

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dyes discharged by the textile industries belong to the reactive (36%), acid (25%), and direct (15%) groups [7]. Due to the bright color, good solubility, and simple operation of reactive dyes, they are the most-used dye group in the textile industry. Dye removal from wastewater can be carried out by various methods such as, adsorption [8], coagulation and flocculation [9], electrocoagulation [10,11], biological methods [4,12], advanced oxidation procedures [13,14], membrane filtration [15], and reverse osmosis [16]. In practical and economic aspects, the adsorption technique has proven to be a simple and cost-effective operation for treating a high volume of wastewater [17]. Different kinds of adsorbents are used for the adsorption technique, including agricultural waste [3,18,19], industrial waste products [20,21], natural inorganic materials (bentonite) [22], sepiolite [23], vermiculite [24], gypsum [25], kaolin [26,27], zeolite [28], perlite [29], feldspar [30], activated carbon in different forms [31,32], carbon nanotube [33], alginate [34], activated sludge [35], and chemical synthetic materials [36,37].

As synthetic materials, different manganese oxides, including MnO, MnO₂, and Mn₃O₄, are often used as adsorbent [38], molecular sieve [39], and catalyst [40,41]. Among the existing manganese oxides, manganese dioxide is the most widely used with its high surface area and diverse crystal structures [42–45]. The phases, sizes, and morphologies of manganese dioxide play an important role in its properties and applications [46–48]. The reported morphologies include nanotube [49], nanorod [44], nanowire [50], flower-like [51], and nanospindle [52] and phases such as “ α ” [36], “ γ ” [37], and “ ϵ ” [47].

A simple and low-cost production, efficient dye adsorption, possibility of regeneration, safe disposal without environmental damage, and potential use as a natural-based material (montmorillonite) make manganese compounds and their composites attractive candidates for the present study of dye adsorption. Considering these positive practical and economic aspects, the present research used manganese compounds (γ -MnOOH and β -MnO₂) and their montmorillonite composites (γ -MnOOH/M and β -MnO₂/M) for the first time to remove Reactive Black 5 (RB5) dye from textile industry wastewater.

2. Experimental materials and methods

2.1. Materials and instruments

KMnO₄, C₂H₅OH, AgNO₃, HCl, and cetyltrimethylammoniumbromide (CTAB) were supplied by Merck and used without further purification. Montmorillonite (CEC = 100 meq 100 g⁻¹) was purchased from Jilin Liufangzi Bentonite Science and Technology, China. Commercial anionic Reactive Black 5 (RB5) dye (Fig. 1) with color index number 20505 (molecular weight 991.82 g mol⁻¹, molar absorptivity (ϵ) 0.0344 L mg⁻¹, and maximum wavelength (λ_{\max}) 597 nm) was supplied from Tianjin Level Chemical Company, China.

Fourier transform infrared spectra (FTIR) of the samples were recorded by the Broker, Tensor 27 spectrometer, using KBr (Mid-Infrared, 4,000–400 cm⁻¹) pellets. The phase composition and structure of samples were defined by the X-ray powder diffractometer, Philips, PW 1800 (Cu K α radiation, $\lambda = 1.54060 \text{ \AA}$).

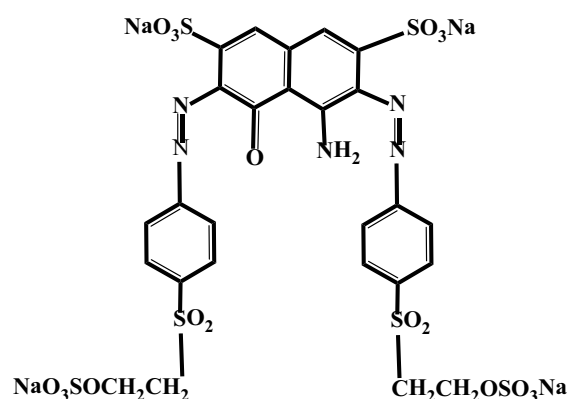


Fig. 1. Structure of RB5.

The size and surface morphologies of synthesized adsorbents were determined using the scanning electron microscopy (SEM), Philips, XL 30.

The concentration of RB5 dye was measured by ultraviolet visible spectrophotometer, Biocary, Varian 100.

2.2. Method

The nano-manganese oxyhydroxide (γ -MnOOH), nano-manganese dioxide (β -MnO₂) compounds and the nano-manganese oxyhydroxide/montmorillonite (γ -MnOOH/M) and nano-manganese dioxide/montmorillonite (β -MnO₂/M) composites were synthesized and characterized.

2.2.1. Synthesis of γ -MnOOH and β -MnO₂ compounds

The γ -MnOOH compound was synthesized using reported hydrothermal method [53] that was modified in our laboratory. KMnO₄ (1.5 g, 9.5×10^{-3} mol) was solved in 65 mL CTAB solution (1 mM), then 4 mL (0.06 mol) absolute ethanol was added and the solution was stirred at room temperature until it was precipitated and became colorless (about 45 min). This mixture was transferred to a stainless steel autoclave, which was placed in the oven at 116°C for 24 h. Mixture was cooled at room temperature and filtered. The brown precipitate (MnOOH) was washed with water and dried at 80°C for 2 h.

The MnO₂ compound was synthesized by calcination of MnOOH, at 300°C for 3 h.

2.2.2. Preparation of γ -MnOOH/M and β -MnO₂/M composites

Montmorillonite was added to 10% HCl (1:100, w/v) and the mixture was stirred for 1 h at room temperature. The mixture was filtered and the filtrate (Montmorillonite) was washed with distilled water. The washed filtrate was mixed with the appropriate compound (γ -MnOOH, β -MnO₂) (2:1 w/w) and stirred (300 rpm) for 3 h at room temperature. The mixture was filtered and the filtrate (γ -MnOOH/M, β -MnO₂/M) was washed and dried in oven at 70°C for 2 h.

2.2.3. Dye removal

Dye adsorption on the synthesized compounds and composites was studied at different conditions of pH, contact time, dye concentration and adsorbent dosage.

Dye solutions imitating textile industrial wastewater were prepared at different concentrations of dye (20, 30, 40, 50, 100, 200, 300, 500, 700, and 900 mg L⁻¹). The concentrations (mg L⁻¹ deionized water) of the chemical compounds contained in the solution imitating textile industrial wastewater were as follows: sucrose (C₁₂H₂₂O₁₁, 600 mg L⁻¹), starch ((C₆H₁₀O₅)_n, 1,000 mg L⁻¹), sodium lauryl sulphate (NaCl₁₂H₂₅SO₄, 100 mg L⁻¹), acetic acid (CH₃COOH, 200 mg L⁻¹), sodium chloride (NaCl, 3,000 mg L⁻¹), sodium carbonate (Na₂CO₃, 500 mg L⁻¹), sodium hydroxide (NaOH, 175 mg L⁻¹), sulfuric acid (H₂SO₄, 300 mg L⁻¹) [54].

Mixtures (10 mL) of the adsorbents (at different dosages) and dye solutions (for each concentration) were prepared with different pH values (phosphate and acetate buffer solutions). These mixtures were stirred (at 120 rpm in room temperature) for defined contact times and were then immediately centrifuged. The adsorption of the supernatant (residual dye) was measured by UV–Vis spectrophotometer. The experiment was performed in triplicate.

3. Results and discussion

The synthesis of compounds and their composites were analyzed by structural and morphological characterization using FTIR spectra, X-ray diffraction (XRD) patterns and SEM images. The dye adsorption process was characterized based on defined adsorption kinetics and isotherm.

3.1. Structural and morphological characterization

The synthesis of γ -MnOOH by the reduction of KMnO₄ (Mn⁷⁺ to Mn³⁺) and the synthesis of β -MnO₂ by the oxidation of γ -MnOOH (Mn³⁺ to Mn⁴⁺) were demonstrated by structural and morphological characterization using different methods. A structural analysis was used to characterize the production of composites by the intercalation of the compounds into nanolayers.

3.1.1. FTIR spectroscopy

The absorption bands above 3,400 cm⁻¹ detected in γ -MnOOH, β -MnO₂ and their composites are attributed to the O–H stretching bands. The O–H stretching band in β -MnO₂ is caused by captured water molecules. The observed absorption bands, including 596 and 490 cm⁻¹ in γ -MnOOH, 519 cm⁻¹ in β -MnO₂, 594 and 522 cm⁻¹ in γ -MnOOH/M and 527 cm⁻¹ in β -MnO₂/M indicate the stretching of Mn–O bond in these products [51,55].

The broad band at 1,036–1,039 cm⁻¹ detected in the composites confirms the stretching of Si–O bond in montmorillonite. The detected absorption bands, including 522 and 452 cm⁻¹ in γ -MnOOH/M and 527 and 465 cm⁻¹ in β -MnO₂/M are related to the Si–O–Si bending in montmorillonite [56]. Some absorption bands of γ -MnOOH, β -MnO₂ and montmorillonite overlap in their composites.

3.1.2. X-Ray diffraction

The XRD patterns of γ -MnOOH, β -MnO₂, montmorillonite, γ -MnOOH/M and β -MnO₂/M are shown in Fig. 2. The pattern of γ -MnOOH confirms the γ -phase

(nine peaks with miller indices (111), (020), (002), (121), (012), (113), (131), (202), and (222), JCPDS NO: 00-041-1379, Fig. 2(a)) [42]. The pattern of β -MnO₂ confirms the β -phase (six peaks with miller indices (110), (101), (111), (211), (220), and (002), JCPDS NO: 00-024-0735, Fig. 2(b)) [57,58]. The patterns of γ -MnOOH and β -MnO₂ are not changed in the composites and their crystalline structures remain stable.

The pattern of montmorillonite shows a peak at $2\theta = 6.76$ ($d = 1.305$ nm, Fig. 2(c)), which is changed similarly in both composites as a result of the intercalation of montmorillonite [59] by γ -MnOOH and β -MnO₂. This peak is changed to $2\theta = 6.28$ ($d = 1.405$ nm) in γ -MnOOH/M composite (Fig. 2(d)) and to $2\theta = 6.29$ ($d = 1.401$ nm) in β -MnO₂/M composite (Fig. 2(e)).

3.1.3. Scanning electron microscopy

SEM images of γ -MnOOH (Fig. 3(a)) and β -MnO₂ (Fig. 3(b)) indicate the similar nanowire morphologies (diameter ~ 36 nm, length ~ 1,000 nm) for both compounds. As shown in Fig. 3(c) and (d), the nanolayer morphology of montmorillonite is not changed by the intercalation of the compounds into the montmorillonite.

3.2. Dye adsorption process

The adsorption of RB5 by γ -MnOOH, β -MnO₂, γ -MnOOH/M, and β -MnO₂/M was investigated under different pH values, contact times, amounts of adsorbent and dye concentrations for optimizing the dye removal conditions. Dye adsorption on β -MnO₂, γ -MnOOH/M, and β -MnO₂/M is based on electrostatic interactions, and dye adsorption on γ -MnOOH is caused by the hydrogen bonds formed between γ -MnOOH (oxygen atoms and OH groups) and the dye molecules. The dye concentration (c), calculated by UV–Vis spectrophotometry [60], was used to define the adsorption kinetics and isotherms.

3.2.1. pH

pH is an important parameter in the adsorption process that affects the adsorbent capacity, dye solubility, and surface of the adsorbent [19]. Dye adsorption was therefore investigated at different pH values, including 4, 7, and 10 (Fig. 4). The highest adsorption capacity for γ -MnOOH was observed at the pH of 10, which increased the hydrogen bonds between the dye molecules and the compound. Through the hydrogen bondings, the OH⁻ ions that are connected to the positive hydrogens on the surface of γ -MnOOH (Fig. 5) attach to the negatively-charged RB5 dye molecules [2]. β -MnO₂, β -MnO₂/M, and γ -MnOOH/M showed the highest adsorption capacity at the lowest pH value, resulting in an increase of the electrostatic attraction between the dye molecules and the compound/composites. Through the electrostatic attractions, the H⁺ ions act as a bridge between the negatively-charged surfaces of β -MnO₂ (Fig. 5) and the nanolayers of montmorillonite and the anionic dye molecules.

3.2.2. Contact time

The contact time between the adsorbate and the adsorbent is a significant parameter in the adsorption process. At the

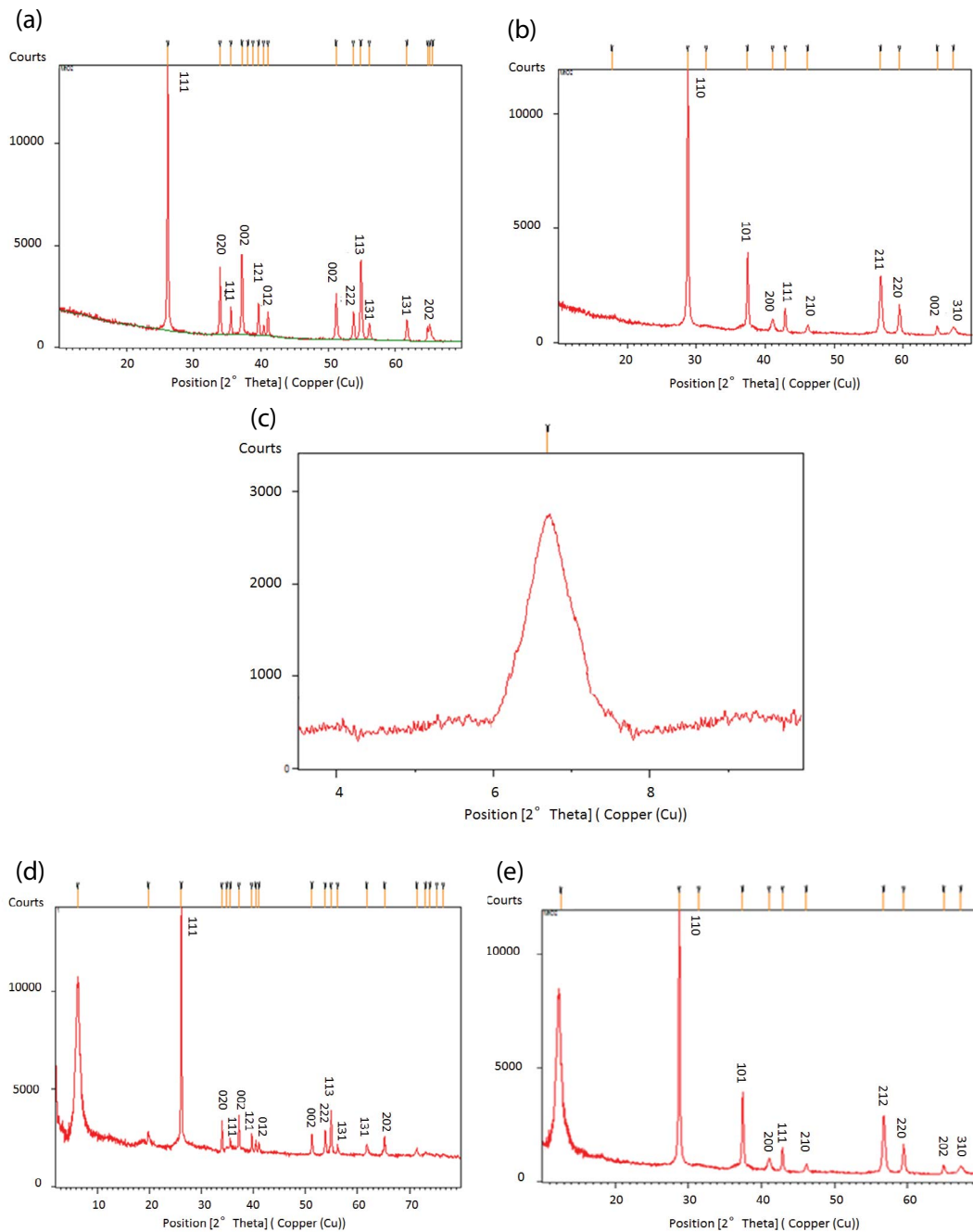


Fig. 2. XRD patterns of, (a) γ -MnOOH, (b) β -MnO₂, (c) montmorillonite, (d) γ -MnOOH/M, and (e) β -MnO₂/M.

optimized pH value, maximum adsorption was achieved after 45 min for both compounds, where γ -MnOOH showed the higher adsorption. For γ -MnOOH/M and β -MnO₂/M, the maximum adsorption was reached after 90 and 120 min, respectively, and β -MnO₂/M showed the higher adsorption. Considering the montmorillonite nanolayer structure, the composites needed a longer contact time to reach the maximum adsorption (Fig. 6).

3.2.3. Adsorbent dosage

The adsorption capacity was analyzed at the optimized pH and contact time under different adsorbent dosages.

The maximum adsorption of the compounds was observed at 1 g L⁻¹ and γ -MnOOH had the higher adsorption. The composites showed a maximum adsorption at 2 g L⁻¹ and the adsorption of β -MnO₂/M was higher. γ -MnOOH showed the highest adsorption with a dosage of 1 g L⁻¹ (Fig. 7).

3.2.4. Dye concentration

The adsorption capacity was investigated by different dye concentrations (20–900 mg L⁻¹) at optimized pH, contact time and adsorbent dosage conditions. At low dye concentrations (20–40 mg L⁻¹), γ -MnOOH showed the highest adsorption

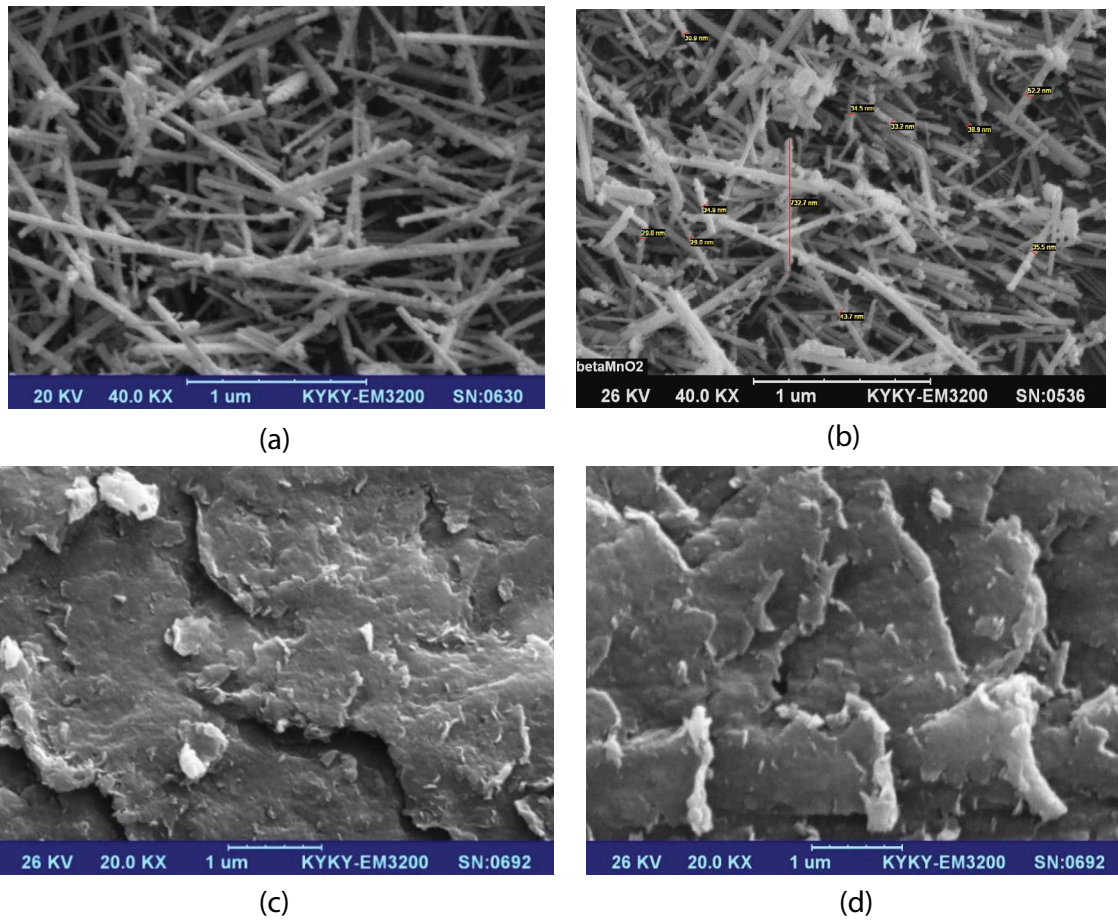


Fig. 3. SEM patterns of, (a) γ -MnOOH, (b) β -MnO₂ (~36 and 1,000 nm, diameter and length), (c) montmorillonite, and (d) γ -MnOOH/M.

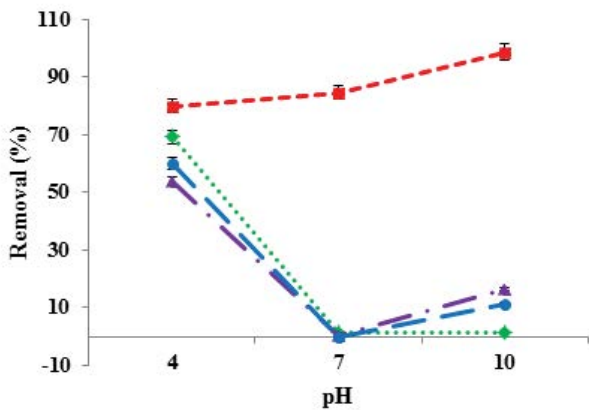


Fig. 4. Effect of pH on RB5 adsorption (Adsorbent = 1 g L⁻¹, Time = 45 min, [dye] = 30 mg L⁻¹) γ -MnOOH (■, SD = ± 2.70%), β -MnO₂ (◆, SD = ± 3.30%) γ -MnOOH/M (▲, SD = ± 3.10%), β -MnO₂/M (●, SD = ± 3.60%).

(~100%), which could be related to the hydroxyl groups on the surface of γ -MnOOH, which increase the hydrogen bonds. At high dye concentrations, the most efficient dye removal was 70% for β -MnO₂/M (500 mg L⁻¹), followed by 60% for γ -MnOOH/M (300 mg L⁻¹), 67% for γ -MnOOH (100 mg L⁻¹)

and 63% for β -MnO₂ (200 mg L⁻¹). The β -MnO₂/M composite showed the most significant dye adsorption of 70% with a concentration of 500 mg L⁻¹ (Fig. 8).

Table 1 presents a summary of the results obtained for adsorption at different conditions. As shown, the β -MnO₂/M composite is the most efficient adsorbent.

3.3. Reusability

There generation and reusability of adsorbents has economic relevance. Washing or heating are two main procedures used to remove dyes and regenerate adsorbents [63,64]. Adsorbents are regenerated without any chemical changes and can be released without any negative environmental impact. Due to cost issues, the washing technique was used for regenerating the adsorbent β -MnO₂. A mixture of adsorbent (β -MnO₂, 0.01 g) and dye (50 mg L⁻¹, pH = 4) was prepared, stirred for 45 min and then centrifuged. The filtrate (β -MnO₂ + dye) was washed (in 3 mL of water) and centrifuged to remove the dye and regenerate the adsorbent. The filtrate (regenerated β -MnO₂) was used again for dye adsorption under the same conditions. This process was repeated seven times. The adsorption capacity of 72%, reached in the first adsorption cycle, was reduced to 60% in the seventh cycle. This small reduction in adsorption

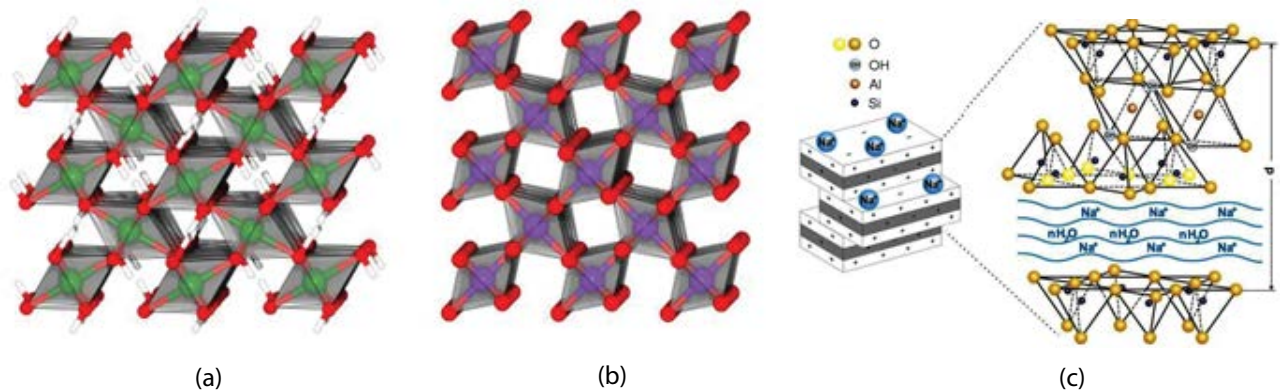


Fig. 5. Scheme of the structures of (a) γ -MnOOH [61], (b) β -MnO₂ [61], and (c) montmorillonite [62].

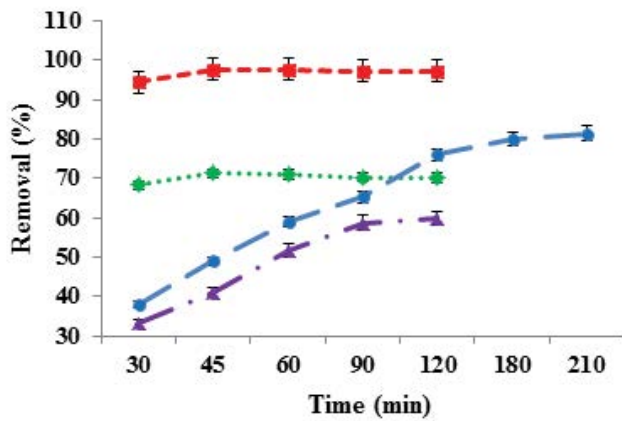


Fig. 6. Effect of contact time on RB5 adsorption (Adsorbent = 1 g L⁻¹, [dye] = 30 mg L⁻¹), γ -MnOOH (■, SD = ± 2.80%) pH = 10, β -MnO₂ (◆, SD = ± 1.70%) pH = 4, γ -MnOOH/M (▲, SD = ± 3.10%) pH = 4, β -MnO₂/M (●, SD = ± 2.20%) pH = 4.

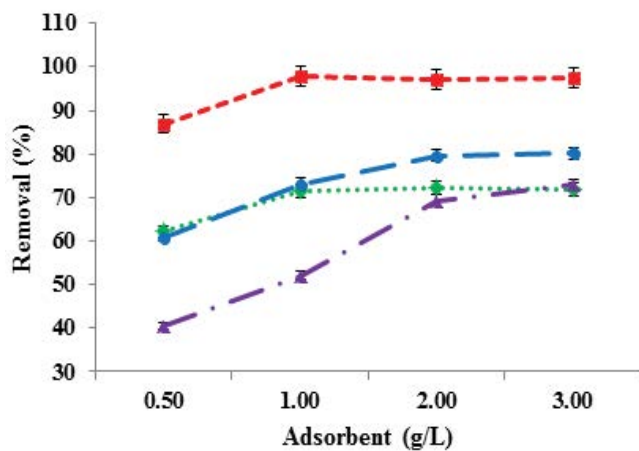


Fig. 7. Effect of adsorbent dosage on RB5 adsorption, [dye] = 30 mg L⁻¹, γ -MnOOH (■, SD = ± 2.35%) pH = 10, Time = 45 min, β -MnO₂ (◆, SD = ± 2.20%) pH = 4, Time = 45 min, γ -MnOOH/M (▲, SD = ± 1.90%) pH = 4, Time = 90 min, β -MnO₂/M (●, SD = ± 1.70%) pH = 4, Time = 120 min.

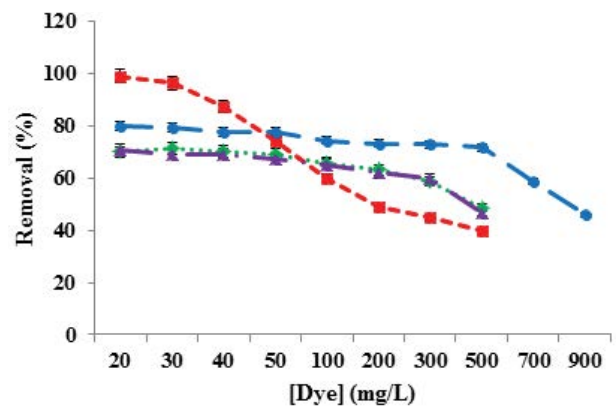


Fig. 8. Effect of initial dye concentration on RB5 adsorption γ -MnOOH (■, SD = ± 2.75%) Adsorbent = 1 g L⁻¹, pH = 10, Time = 45 min, β -MnO₂ (◆, SD = ± 3.20%) Adsorbent = 1 g L⁻¹, pH = 4, Time = 45 min, γ -MnOOH/M (▲, SD = ± 2.98%) Adsorbent = 2 g L⁻¹, pH = 4, Time = 90 min, β -MnO₂/M (●, SD = ± 2.15%) Adsorbent = 2 g L⁻¹, pH = 4, Time = 120 min.

Table 1

Best condition on removal of RB5 by γ -MnOOH, β -MnO₂, γ -MnOOH/M, β -MnO₂/M, and M

Sample	pH	Time (min)	Adsorbent (g L ⁻¹)	[Dye] (mg L ⁻¹)	R(%)
γ -MnOOH	10	45	1	100	67.51
β -MnO ₂	4	45	1	200	63.14
γ -MnOOH/M	4	90	2	300	59.79
β -MnO ₂ /M	4	120	2	500	71.72
M	4	90	2	100	< 20

capacity demonstrates the efficiency of regenerating and reusing β -MnO₂ (Fig. 9).

3.4. Adsorption kinetics and isotherms

3.4.1. Kinetics study

Adsorption kinetics study was performed for the compounds γ -MnOOH and β -MnO₂ and the composites

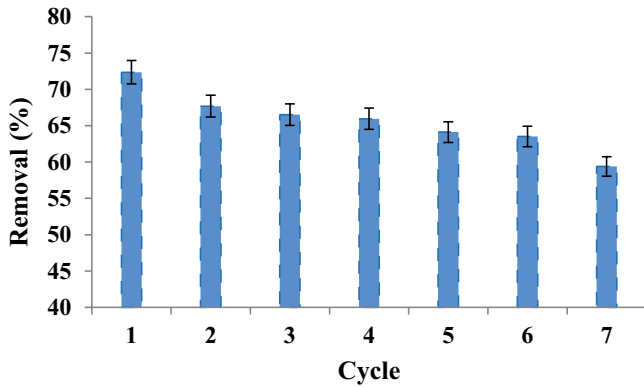
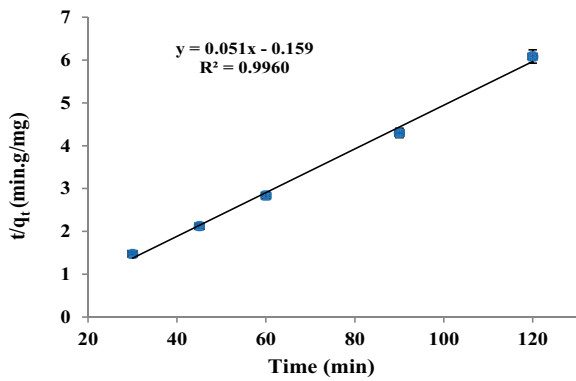


Fig. 9. Reusability of $\beta\text{-MnO}_2$ on RB5 adsorption, Adsorbent = 1 g L⁻¹, pH = 4, Time = 45 min, [dye] = 50 mg L⁻¹ (SD = ± 2.25%).

$\gamma\text{-MnOOH/M}$ and $\beta\text{-MnO}_2\text{/M}$ at a dye concentration of 30 mg L⁻¹. The pseudo-first-order kinetic model (Lagergren, 1898, Eq. (1)) [65] as well as the pseudo-second-order kinetic model (Ho and McKay, 1998, Eq. (2)) [55,65] were applied to define the adsorption kinetics.

$$\log(q_{\text{eq}} - q_t) = \log q_{\text{eq}} - \left(\frac{k_1}{2.303}\right)t \quad (1)$$



(a)

$$\frac{t}{q_t} = \frac{1}{(k_2 q_{\text{eq}}^2)} + \left(\frac{1}{q_{\text{eq}}}\right)t \quad (2)$$

As demonstrated in Fig. 10, the adsorption kinetics of all the compounds and composites followed the pseudo-second-order kinetic model. The kinetic parameters, i.e. k_2 (rate constant) and q_{eq} were higher in the compounds than in the composites, and $\gamma\text{-MnOOH}$ showed the highest values (Table 2).

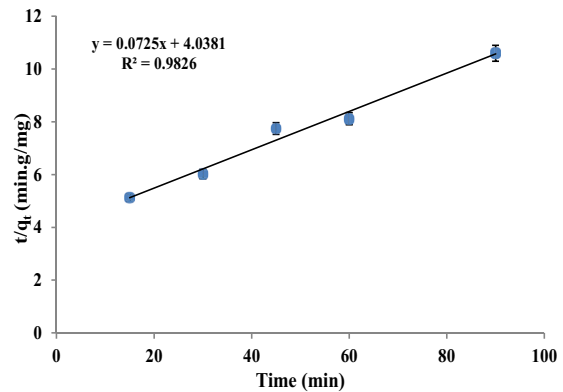
3.4.2. Isotherm study

The most-used adsorption isotherms, i.e. Freundlich (Eqs. (3) and (4)) and Langmuir (Eqs. (5)–(7)) [66,67], were applied to determine the adsorption isotherm for the compounds and the composites by different dye concentrations (20–900 mg L⁻¹) at optimized conditions.

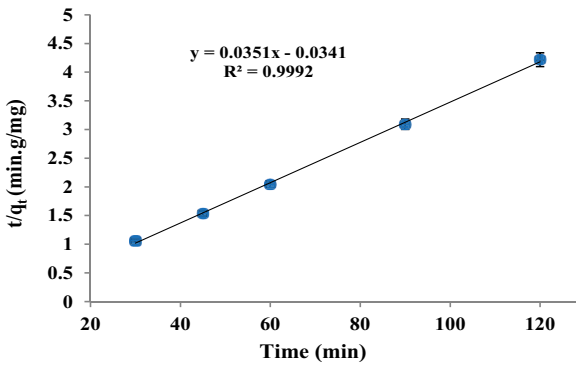
$$q_e = K_f C_e^{1/n} \quad (3)$$

$$\log q_e = \log K_f + \frac{1}{n} \log C_e \quad (4)$$

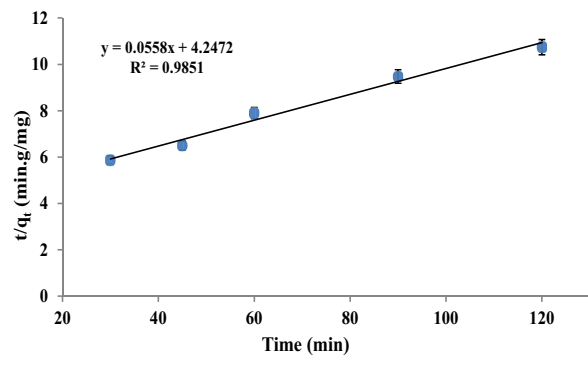
$$q_e = \frac{(q_m b C_e)}{(1 + b C_e)} \quad (5)$$



(c)



(b)



(d)

Fig. 10. Pseudo-second-order kinetic model of RB5, (a) $\gamma\text{-MnOOH}$ (1 g L⁻¹, pH = 10, [dye] = 30 mg L⁻¹, SD = ± 2.85%), (b) $\beta\text{-MnO}_2$ (1 g L⁻¹, pH = 4, [dye] = 30 mg L⁻¹, SD = ± 2.54%), (c) $\gamma\text{-MnOOH/M}$ (2 g L⁻¹, pH = 4, [dye] = 30 mg L⁻¹, SD = ± 2.85%), and (d) $\beta\text{-MnO}_2\text{/M}$ (2 g L⁻¹, pH = 4, [dye] = 30 mg L⁻¹, SD = ± 3.05%).

Table 2
Results of the kinetics calculations of γ -MnOOH and β -MnO₂

Adsorbent	Conc. (mg L ⁻¹)	Pseudo-first-order kinetic			Pseudo-second-order kinetic		
		q_{eq} (mg g ⁻¹)	k_1 (1 min ⁻¹)	R^2	q_{qe} (mg g ⁻¹)	k_2 (g mg ⁻¹ min)	R^2
γ -MnOOH	30	29.509	15.660	0.924	28.490	3.612	0.999
β -MnO ₂	30	24.888	15.660	0.910	19.608	1.635	0.996
γ -MnOOH/M	30	17.386	0.0490	0.945	13.793	0.0013	0.983
β -MnO ₂ /M	30	118.17	0.0108	0.974	17.921	0.0007	0.985

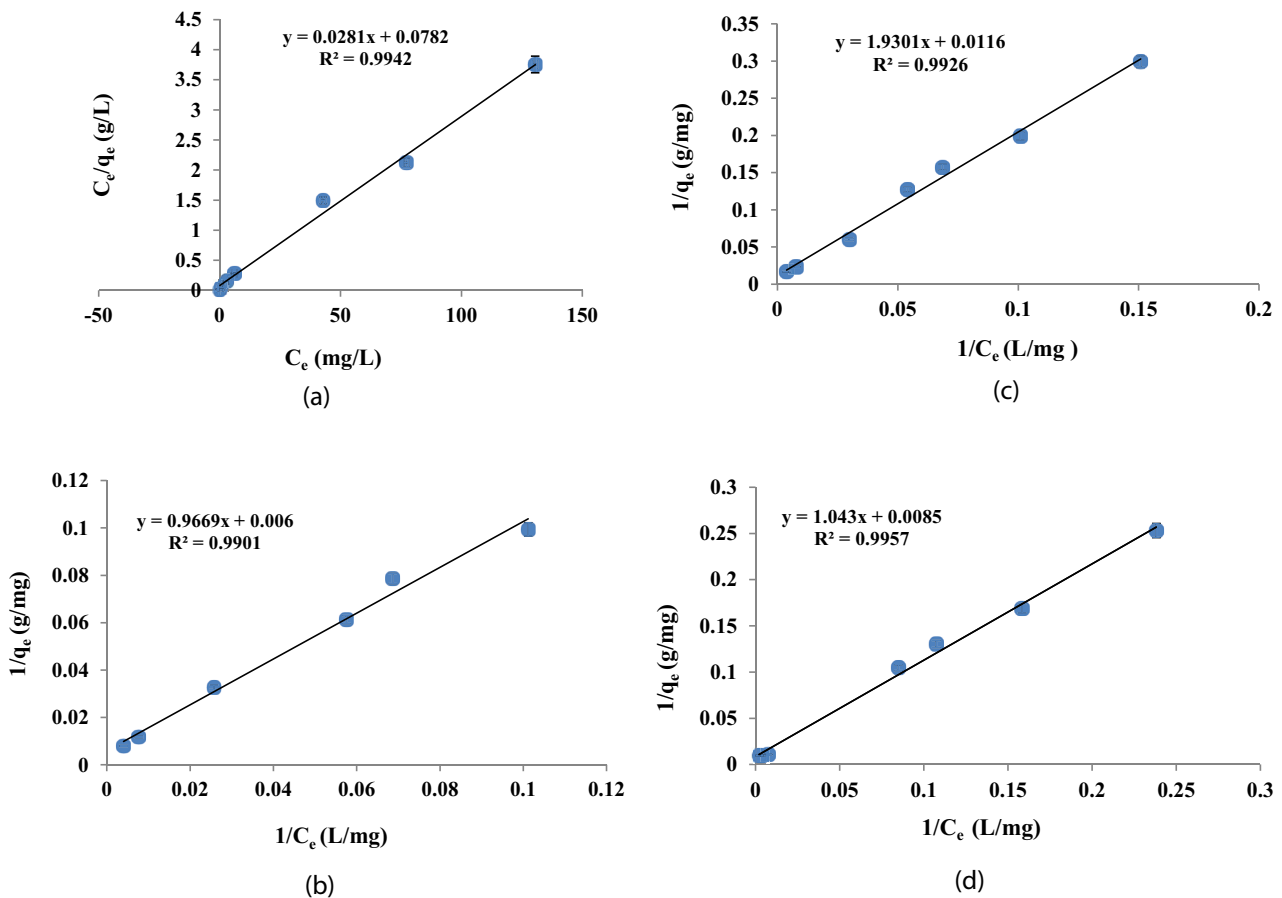


Fig. 11. Langmuir adsorption isotherms of RB5, (a) γ -MnOOH (Adsorbent = 1 g L⁻¹, pH = 10, Time = 45) (SD = \pm 2.85%), (b) β -MnO₂ (Adsorbent = 1 g L⁻¹, pH = 4, Time = 45) (SD = \pm 3.40%), (c) γ -MnOOH/M (Adsorbent = 2 g L⁻¹, pH = 4, Time = 90) (SD = \pm 3.15%), and (d) β -MnO₂/M (Adsorbent = 2 g L⁻¹, pH = 4, Time = 120) (SD = \pm 2.45%).

$$\frac{C}{q_e} = \frac{C_{eq}}{q_m} + \frac{1}{(q_m b)} \quad (6)$$

$$\frac{1}{q_e} = \frac{1}{q_m} + \frac{1}{(q_m b C_e)} \quad (7)$$

The correlation coefficients (R^2) of Freundlich and Langmuir isotherms were set for all the compounds and

composites. With the set R^2 , γ -MnOOH and both composites follow the Langmuir isotherm, and β -MnO₂ follows the Freundlich isotherm (Figs. 11 and 12, Table 3). Since the value of all R^2 s were high and close to each other, the isotherm parameters, including Freundlich isotherm constant (K_f (mg^{1-1/n} L^{1/n} g⁻¹), adsorption intensity (n), Langmuir isotherm constant (b (L mg⁻¹)) and maximum monolayer capacity (q_m (mg g⁻¹)) were determined. The isotherm parameters were similar for all the adsorbents, except for γ -MnOOH.

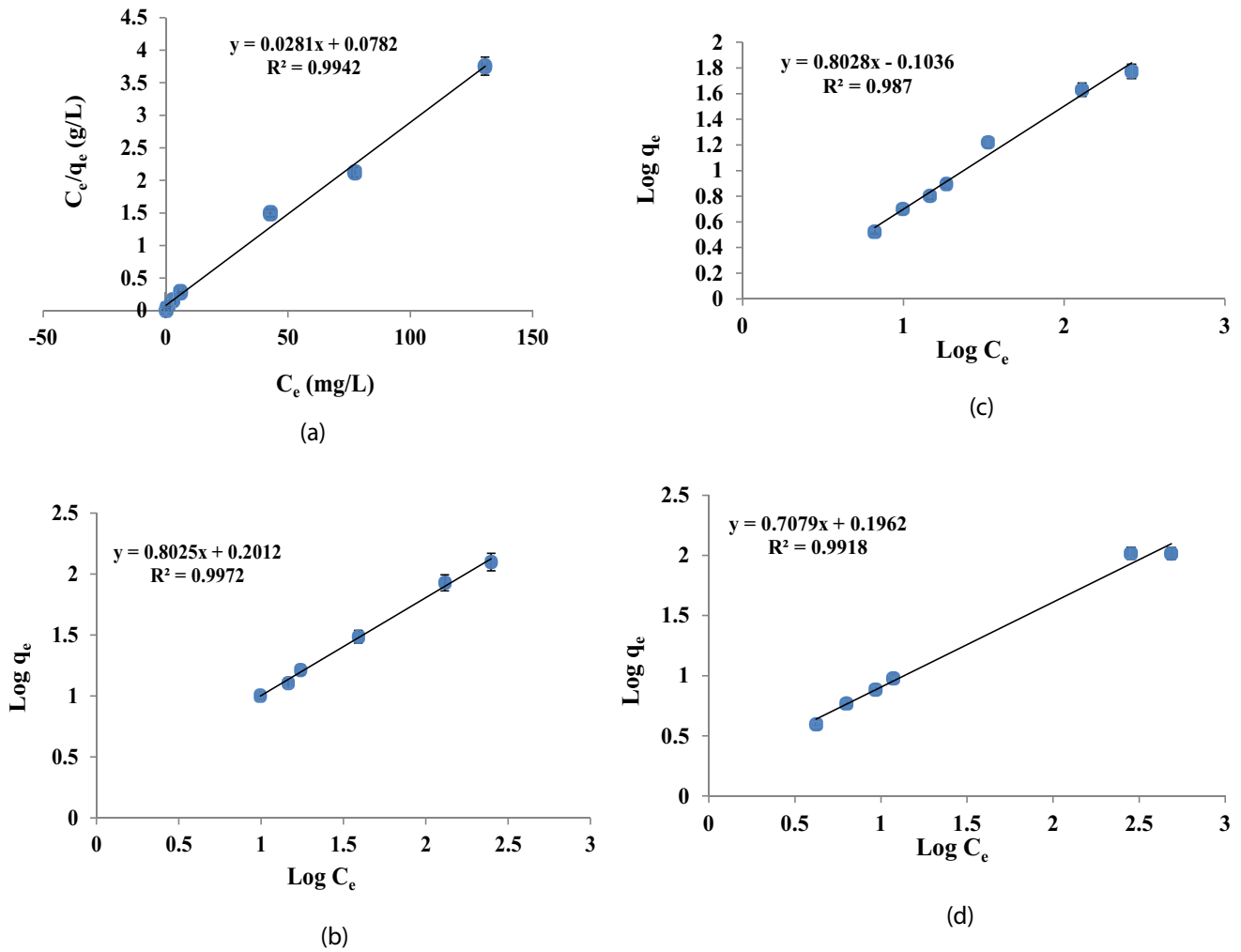


Fig. 12. Freundlich adsorption isotherms of RB5, (a) γ -MnOOH (Adsorbent = 1 g L⁻¹, pH = 10, Time = 45) (SD = ± 2.85%), (b) β -MnO₂ (Adsorbent = 1 g L⁻¹, pH = 4, Time = 45) (SD = ± 3.40%), (c) γ -MnOOH/M (Adsorbent = 2 g L⁻¹, pH = 4, Time = 90) (SD = ± 3.15%), and (d) β -MnO₂/M (Adsorbent = 2 g L⁻¹, pH = 4, Time = 120) (SD = ± 2.45%).

Table 3
Results of the isotherms calculations at optimum condition

Isotherm	Isotherm parameters	Adsorbent			
		γ -MnOOH	β -MnO ₂	γ -MnOOH/M	β -MnO ₂ /M
Langmuir	b (L mg ⁻¹)	0.3593	0.0062	0.0046	0.0081
	q_m (mg g ⁻¹)	35.5872	166.6666	109.8901	117.6470
	R^2	0.9942	0.9901	0.9926	0.9957
	R_L (min)*	0.1221	0.3283	0.9157	0.8605
	R_L (max)*	0.0137	0.2439	0.3030	0.1206
Freundlich	K_f (mg ^{1-1/n} L ^{1/n} g ⁻¹)	14.9830	1.5892	1.2694	1.5711
	n	5.2465	1.2461	1.2456	1.4126
	R^2	0.9855	0.9972	0.9870	0.9918

Min (minimum) & max (maximum) concentrations of dye

Table 4
Adsorption capacities of different adsorbents for the RB5 adsorption (Langmuir adsorption isotherm)

Adsorbents	q_{\max} (mg g ⁻¹)	References
Chitosan flakes	480	[68]
Chitosan beads	400	[68]
Eucalyptusbark/magnetite composite	370.7	[69]
Cetyltrimethylammonium bromide-coated magnetite	312.5	[70]
β -MnO ₂	166.66	This study
Ionic liquid grafted-magnetic nanoparticles	161.29	[71]
Chitosan-intercalated montmorillonite	138.89	[4]
Chitin	130	[68]
β -MnO ₂ /Montmorillonite(β -MnO ₂ /M)	117.65	This study
γ -MnOOH/Montmorillonite (γ -MnOOH/M)	109.89	This study
Surfactant-modified activated carbon	100	[72]
Powdered activated carbon	58.823	[73]
Banana peel powder	49.2	[63]
Silica–alumina oxide	47.10	[74]
γ -MnOOH	35.58	This study
Chitosan 10B	34.197	[75]
Bentonite clay	34.01	[22]
ZnO–Fe ₃ O ₄	22.1	[76]
Activated carbon from walnut wood	19.34	[77]
Surfactant-Modified zeolite	12.929	[78]
Cu–Cu ₂ O-based char	6.06	[79]
F ₃ O ₄ -based char	2.88	[79]

The equilibrium parameter of the Langmuir isotherm (R_L) was calculated for γ -MnOOH, β -MnO₂, γ -MnOOH/M, and β -MnO₂/M at respective minimum and maximum dye concentrations [64]. As expected, the values of all the R_L s were less than 1, and γ -MnOOH showed the lowest value (Table 3).

Since most of the adsorbents used in this study follow the Langmuir isotherm, Table 4 presents an overview of the q_m values of these and other reported adsorbents (natural minerals, synthetic compounds and vegetable/fruit waste).

In addition to the q_m parameter, further factors, such as dye adsorption conditions, availability and production of adsorbent, should be considered for selecting the most efficient adsorbent.

4. Conclusion

In the course of this study, the manganese compounds γ -MnOOH and β -MnO₂, with similar nanowire morphologies, were synthesized. These compounds intercalated the nanolayers of montmorillonite and produced their respective composites, i.e. γ -MnOOH/M and β -MnO₂/M. Both compounds and composites were able to adsorb RB5 in dye solutions imitating textile industrial wastewater. At similar conditions, the highest adsorption was observed at pH = 4 for β -MnO₂ and both composites. Meanwhile, γ -MnOOH showed the best adsorption at pH = 10. At optimized pH values, the composites needed a longer contact time for an efficient adsorption. At optimized pH values and contact times, the compounds showed the lowest adsorbent dosage for the most efficient

adsorption. At optimized pH values, contact times and adsorbent dosages, the highest adsorption was detected in a low dye concentration for γ -MnOOH and in a high dye concentration for β -MnO₂/M. The most adequate dye adsorption (70%) was detected for the composite β -MnO₂/M by a dye concentration of 500 mg L⁻¹. The regeneration experiment showed that β -MnO₂ is a reusable adsorbent with a high adsorption capacity.

The adsorption kinetics of compounds and composites thus follow the pseudo-second-order kinetic model. The k_2 and q_{eq} of compounds were higher than those of the composites, and γ -MnOOH showed the highest value.

The results obtained for the adsorption isotherms showed that γ -MnOOH and the composites follow the Langmuir isotherm and β -MnO₂ follows the Freundlich isotherm.

All the adsorbents, except for γ -MnOOH, showed similar values for the Freundlich and Langmuir isotherm parameters K_f , n , b , and q_m .

Based on the present finding, manganese compounds (γ -MnOOH and β -MnO₂) and their composites (γ -MnOOH/M and β -MnO₂/M) have proven to be suitable adsorbents for removing different concentrations of RB5 dye from textile industrial wastewater. Their relatively low cost, simple production steps, and possibility of reuse make these materials good candidates for use as efficient dye adsorbents for the treatment of industrial wastewater.

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